

# Modulating Ru-Co bond lengths in Ru<sub>1</sub>Co single-atom alloys through crystal phase engineering for electrocatalytic nitrate-to-ammonia conversion

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Single atom alloys (SAAs) with maximum atomic efficiency and uniform active sites show great promise for heterogeneous catalytic applications. Meanwhile, crystal phase engineering has garnered significant interest due to tailored atomic arrangements and coordination environments. However, the crystal phase engineering of SAAs remains challenging owing to high surface energy and complex phase transition dynamics. Herein, Ru<sub>1</sub>Co SAAs with tunable crystal phases (hexagonal-close-packed (hcp), face-centered-cubic (fcc), and hcp/fcc structure) are successfully synthesized via controlled phase transitions. These SAAs exhibit distinct crystal phase-dependent performance towards nitrate reduction reaction (NO<sub>3</sub>RR), where hcp-Ru<sub>1</sub>Co outperforms its counterparts with a NH<sub>3</sub> Faradaic efficiency of 96.78% at 0 V vs. reversible hydrogen electrode and long-term stability exceeding 1200 h. Mechanistic investigations reveal that the hcp configurations enables shorter Ru-Co distances, stronger interatomic interactions, and more positive surface potential compared to hcp/fcc-Ru<sub>1</sub>Co and fcc-Ru<sub>1</sub>Co, which enhances the NO<sub>3</sub><sup>-</sup> adsorption, reduces the free energy barrier, and suppresses competitive hydrogen evolution.

Noble metal-based nanomaterials have attracted considerable attention in electrocatalysis due to their unique catalytic properties<sup>1,2</sup>. Theoretically, modulating the crystal structure can tailor the coordination geometry and electronic configuration of active sites, thereby affecting the adsorption/desorption behavior of reactants and intermediates, which ultimately regulates catalytic performance<sup>3,4</sup>. However, the inherent characteristics of metallic bonds (their unsaturated and non-directional nature) tend to drive metal catalysts toward

conventional crystal structures<sup>5,6</sup>. For instance, Ru typically forms a hexagonal-close-packed (hcp) structure while Pt adopts a face-centered-cubic (fcc) arrangement. This structural persistence presents significant challenges in both controlling crystal phase modifications and establishing clear structure–property relationships in metallic catalytic systems.

To minimize noble metal usage while enhancing catalytic performance, the atomic dispersion of noble metal atoms within a host

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metal matrix to form single-atom-alloys (SAAs) has emerged as an effective strategy<sup>7–9</sup>. SAAs can realize the maximum utilization of metal atoms, uniform active sites, peculiar geometric and electronic structures, which collectively contribute to superior catalytic properties<sup>10–13</sup>. The well-defined active centers in SAAs further facilitate fundamental investigations of structure–activity relationships and catalytic mechanisms. Nevertheless, constructing SAAs with tailored crystal structures remains challenging due to the high surface energy of isolated metal atoms and the lack of effective synthetic methods for precise crystal phase control at the nanoscale. Notably, successful demonstrations of crystal phase engineering in SAAs have not yet been reported.

Herein, we successfully synthesize Ru<sub>1</sub>Co SAAs with distinct crystal phases (i.e., hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, and fcc-Ru<sub>1</sub>Co) through a solvothermal method followed by thermal annealing. These obtained Ru<sub>1</sub>Co SAAs are employed as electrocatalysts for nitrate reduction reaction (NO<sub>3</sub>RR) to ammonia (NH<sub>3</sub>). Remarkably, hcp-Ru<sub>1</sub>Co demonstrates competitive performance with a NH<sub>3</sub> Faradaic efficiency (FE<sub>NH<sub>3</sub></sub>) of 96.78% at 0 V vs. reversible hydrogen electrode (RHE). The energy consumption (EC) and NH<sub>3</sub> production cost for hcp-Ru<sub>1</sub>Co are calculated as 19.04 kWh kg<sup>−1</sup> and 0.57 \$<sub>USD</sub> kg<sup>−1</sup>, respectively. Additionally, hcp-Ru<sub>1</sub>Co maintains operational stability for over 1200 h. Combined experimental and theoretical analyses reveal that hcp-Ru<sub>1</sub>Co possesses reduced Ru–Co distances, enhanced Ru–Co interatomic interactions, and more positive surface potential compared to hcp/fcc-Ru<sub>1</sub>Co and fcc-Ru<sub>1</sub>Co, collectively promoting NO<sub>3</sub><sup>−</sup> adsorption, lowering the free energy barrier, and suppressing hydrogen evolution reaction (HER). A prototype Zn–NO<sub>3</sub><sup>−</sup> battery employing hcp-Ru<sub>1</sub>Co as the cathode catalyst demonstrates high electrochemical performance.

## Results

### Synthesis and structural characterizations

The Ru<sub>1</sub>Co SAAs with different crystal phases are successfully synthesized via a solvothermal method followed by thermal annealing (see the “Methods” section for experimental details and Fig. 1a for schematic illustration). Specifically, CoCl<sub>2</sub>·6H<sub>2</sub>O and RuCl<sub>3</sub>·xH<sub>2</sub>O precursors are dissolved in 1,4-butanediol and heated at 230 °C for 20 min. Subsequent annealing at 300, 500, and 700 °C for 30 min yields hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, and fcc-Ru<sub>1</sub>Co, respectively.

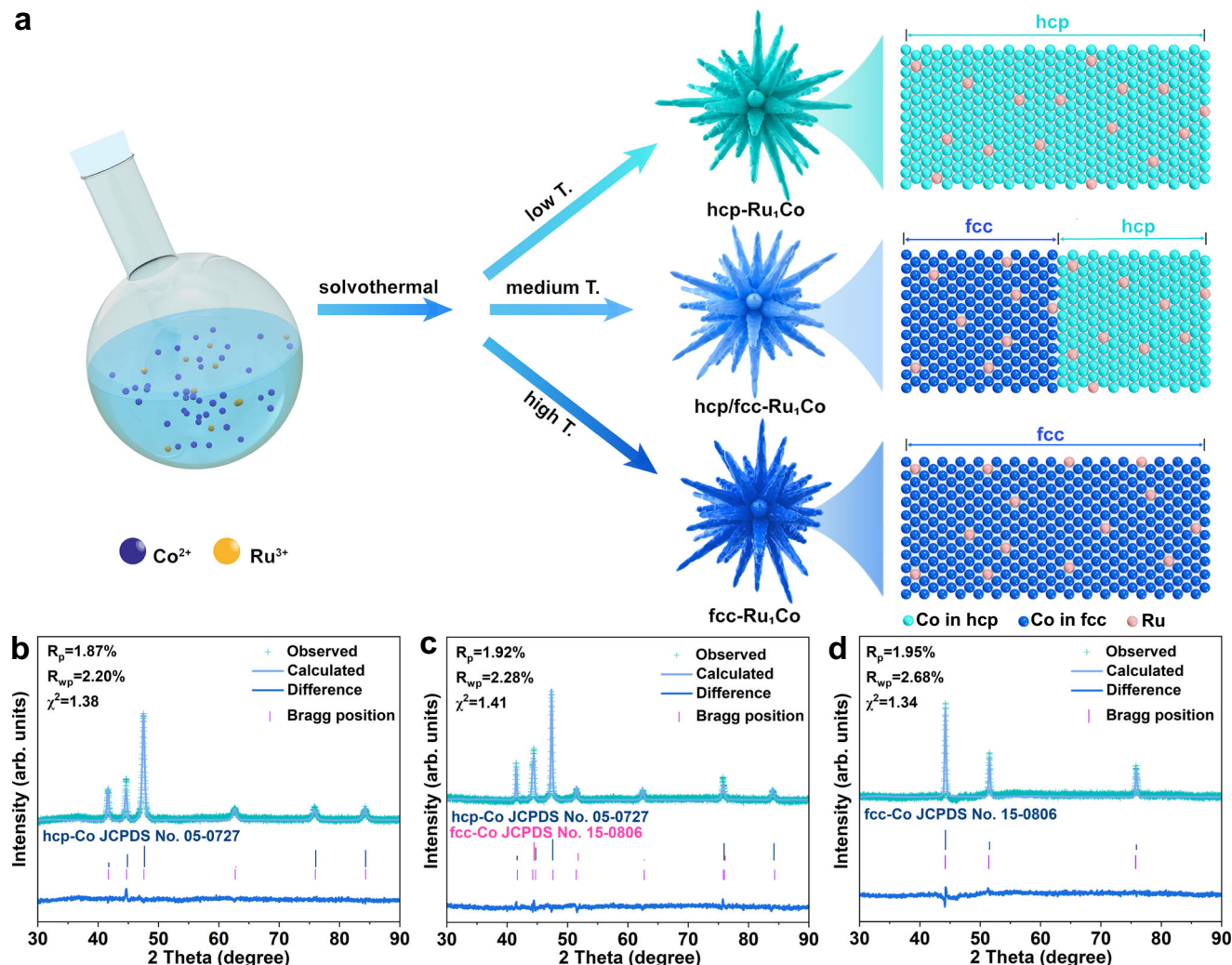
The crystal phases of synthesized samples are characterized by X-ray diffraction (XRD). As shown in Fig. 1b, d, the diffraction peaks of hcp-Ru<sub>1</sub>Co match well with those of hcp-Co (JCPDS No. 05-0727), while fcc-Ru<sub>1</sub>Co exhibits the diffraction peaks well indexed to fcc-Co (JCPDS No. 15-0806). Notably, the diffraction peaks of both hcp-Ru<sub>1</sub>Co and fcc-Ru<sub>1</sub>Co exhibit slightly negative shifts compared to those of hcp-Co and fcc-Co, indicating the successful incorporation of Ru with a large atomic radius into the Co matrix. The XRD pattern of hcp/fcc-Ru<sub>1</sub>Co shows the coexistence of diffraction peaks from both phases (Fig. 1c), verifying the successful synthesis of hcp/fcc-Ru<sub>1</sub>Co. Rietveld refinement profiles demonstrate high phase purity in all Ru<sub>1</sub>Co SAAs. Inductively coupled plasma-optical emission spectroscopy (ICP-OES) analysis confirms consistent Co/Ru atomic ratios of 99.25/0.75 in all Ru<sub>1</sub>Co SAAs (Supplementary Table 1).

The morphology of hcp-Ru<sub>1</sub>Co is investigated through transmission electron microscopy (TEM) and high-angle annular dark-field scanning TEM (HAADF-STEM), which reveals a homogeneous nano-urchin structure (Fig. 2a, Supplementary Figs. 1 and 2). Atomic-scale characterization via aberration-corrected HAADF-STEM (AC-HAADF-STEM) utilizes Z-contrast imaging, where Ru atoms (Z = 44) exhibit brighter atomic-scale contrast compared to Co (Z = 27). As shown in Fig. 2b, isolated Ru atoms are observed without detectable clusters or nanoparticles, confirming the atomic dispersion of Ru in the Co matrix. Three-dimensional (3D) surface plots converted from the cyan square in Fig. 2b are analyzed. High-intensity spots represent Ru atoms, while low-intensity spots correspond to Co atoms. The isolated Ru spots in

Fig. 2c provide additional evidence of Ru atomic dispersion. The atomic arrangement of hcp-Ru<sub>1</sub>Co is further revealed by high-resolution AC-HAADF-STEM (Fig. 2d). An enlarged view from the cyan square in Fig. 2d shows the atomic columns along the [110] zone axis (Fig. 2e), closely matching the simulated atomic model of hcp-Co (Fig. 2g). The corresponding fast Fourier transform (FFT) pattern (Fig. 2f) aligns with the simulated electron diffraction pattern of hcp-Co (Fig. 2h). Interplanar spacings measured from the intensity profiles (converted from orange rectangles in Fig. 2d) are 0.21 and 0.19 nm, corresponding to the (110) and (111) planes of hcp-Ru<sub>1</sub>Co, respectively (Fig. 2i, j). Notably, the presence of isolated peaks with relatively high intensity further confirms the atomic dispersion of Ru. HAADF-STEM image and corresponding elemental mappings demonstrate the uniform distribution of Ru and Co in the nano-urchin structure (Fig. 2k–n). Energy-dispersive X-ray spectroscopy (EDS) reveals the Ru/Co atomic ratio of 99.24/0.76 (Supplementary Fig. 3), consistent with ICP-OES results.

The structural characteristics of fcc-Ru<sub>1</sub>Co are systematically investigated. TEM image confirms the preserved nano-urchin morphology (Fig. 3a and Supplementary Fig. 4). Atomic dispersion of Ru in the Co matrix is verified by HAADF-STEM (Fig. 3b) and 3D surface plot analysis (Fig. 3c). An enlarged AC-HAADF-STEM image (Fig. 3e) from the purple square in Fig. 3d shows the atomic columns along the [110] zone axis, matching the simulated atomic model of fcc-Co (Fig. 3g). The corresponding FFT pattern (Fig. 3f) aligns with the simulated diffraction pattern of fcc-Co (Fig. 3h). Interplanar spacing measurements yield 0.21 nm, corresponding to the (111) plane of fcc-Ru<sub>1</sub>Co, with isolated Ru peaks confirming atomic dispersion (Fig. 3i, j). For hcp/fcc-Ru<sub>1</sub>Co, TEM image reveals the conserved nano-urchin structure (Fig. 3k and Supplementary Fig. 5). HAADF-STEM image (Fig. 3l) and 3D surface plots (Fig. 3m) confirm the atomic dispersion of Ru. High-resolution AC-HAADF-STEM image reveals two types of atomic arrangements with distinct heterophase boundary (Fig. 3n). FFT patterns (Fig. 3o and p) from the selected purple and cyan squares in Fig. 3n, align with the simulated diffraction patterns of fcc-Co along the [110] zone axis (Fig. 3q) and hcp-Co along the [111] zone axis (Fig. 3r), respectively. FFT pattern (Supplementary Fig. 6b) from the boundary region (orange square) in Supplementary Fig. 6a, reveals the overlapped electron diffraction dots along the [110] zone axis of fcc-Co ([110]<sub>fcc</sub>) and the [111] zone axis of hcp-Co ([111]<sub>hcp</sub>) (Supplementary Fig. 6c). The intensity profiles from the orange rectangles in Fig. 3n reveal the interplanar spacings of 0.21 and 0.20 nm, assigned to the (111) plane of fcc-Ru<sub>1</sub>Co and (011) plane of hcp-Ru<sub>1</sub>Co, respectively (Fig. 3s, t). The existence of the isolated maximum peaks further confirms Ru atomic dispersion.

The electronic structure and coordination environment of Ru<sub>1</sub>Co SAAs with different crystal phases are investigated by X-ray photoelectron spectroscopy (XPS) and X-ray absorption spectroscopy (XAS). XPS analysis confirms that metallic Co and Ru are dominant in all Ru<sub>1</sub>Co SAAs (Supplementary Fig. 7). The Ru 3p XPS spectrum of hcp-Ru<sub>1</sub>Co exhibits peaks at 461.38 and 483.56 eV, assigned to 3p<sub>3/2</sub> and 3p<sub>1/2</sub> of Ru<sup>0</sup>, respectively<sup>14</sup>. A positive shift in the binding energy of Ru<sup>0</sup> 3p<sub>3/2</sub> peak is observed for hcp/fcc-Ru<sub>1</sub>Co (461.79 eV) and fcc-Ru<sub>1</sub>Co (462.01 eV) compared to hcp-Ru<sub>1</sub>Co (461.38 eV), suggesting reduced electron density on Ru in hcp-Ru<sub>1</sub>Co. The observed oxides are attributed to the easy oxidation characters of Co and Ru in air, in accordance with previous reports<sup>15,16</sup>. Figure 4a displays the normalized Co K-edge X-ray absorption near edge structure (XANES) spectra of Ru<sub>1</sub>Co SAAs and references (i.e., Co foil and Co<sub>3</sub>O<sub>4</sub>). The absorption edges of all Ru<sub>1</sub>Co SAAs are close to Co foil but with slight shifts towards higher energy, indicating the metallic characteristics of Co with reduced electron density. This is attributed to the lower electronegativity of Co (1.9) compared to Ru (2.2), resulting in electron transfer from Co to Ru<sup>17</sup>. This directional electron transfer is further corroborated by the decreased valence state of Ru in hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, and



**Fig. 1 | Scheme and XRD characterization.** **a** Scheme for the formation of  $\text{Ru}_1\text{Co}$  SAAs with different crystal phases. **b–d** The Rietveld refinement of XRD patterns of hcp- $\text{Ru}_1\text{Co}$  (**b**), hcp/fcc- $\text{Ru}_1\text{Co}$  (**c**), and fcc- $\text{Ru}_1\text{Co}$  (**d**). Source data for this figure are provided as a Source Data file.

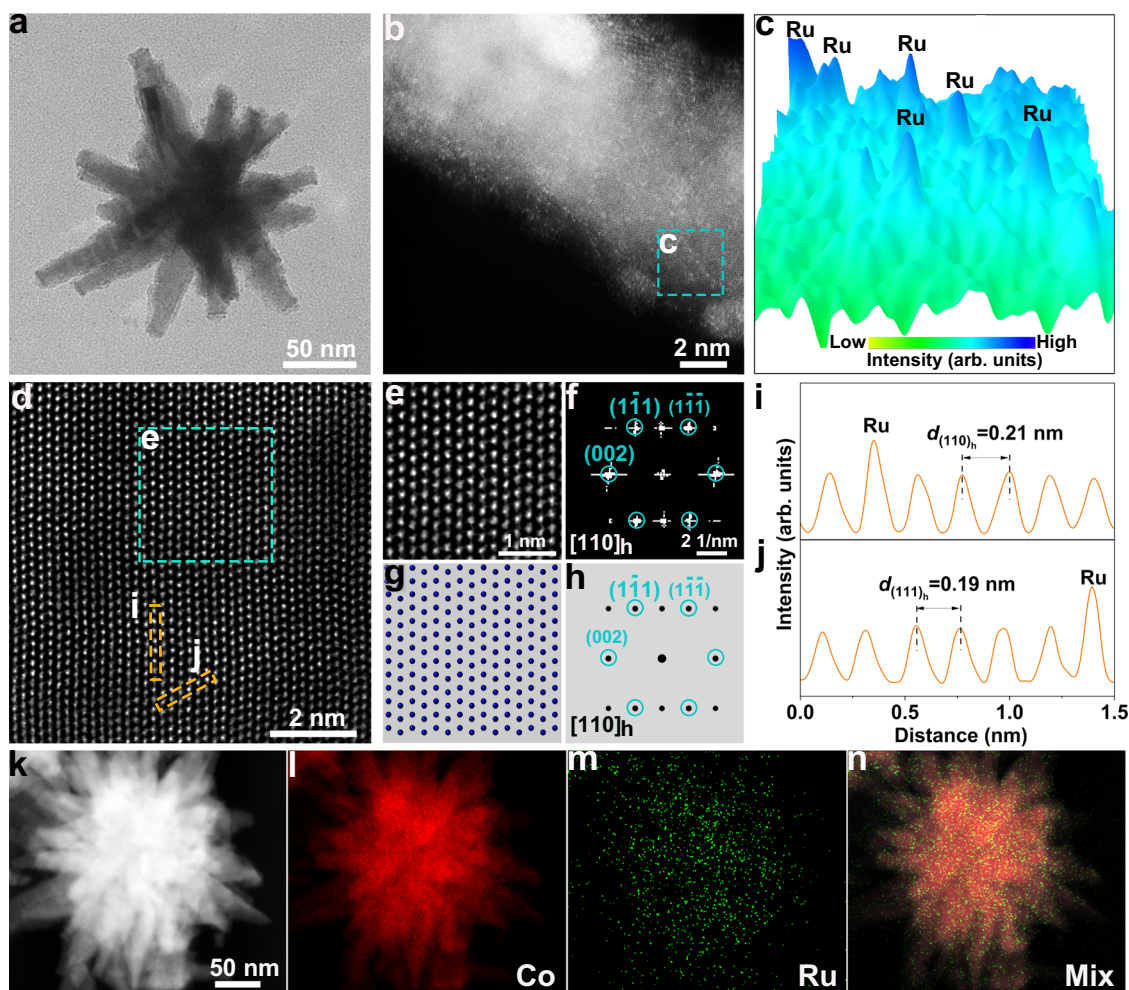
fcc- $\text{Ru}_1\text{Co}$  relative to Ru foil, as revealed in the normalized Ru K-edge XANES spectra (Fig. 4c). Notably, the Co K-edge adsorption of hcp- $\text{Ru}_1\text{Co}$  positively shifts compared to fcc- $\text{Ru}_1\text{Co}$  and hcp/fcc- $\text{Ru}_1\text{Co}$  (inset of Fig. 4a), with the opposite trend observed for the Ru K-edge adsorption (inset of Fig. 4c), suggesting a stronger electronic interaction between Co and Ru in hcp- $\text{Ru}_1\text{Co}$ .

Extended X-ray absorption fine structure (EXAFS) spectroscopy is performed to probe the local atomic configurations. The Co K-edge Fourier transformed EXAFS (FT-EXAFS) spectra of  $\text{Ru}_1\text{Co}$  SAAs display a prominent peak at 2.17 Å, matching the characteristic Co–Co bond observed in Co foil (Fig. 4b). This consistent peak position results from the low Ru content and the predominant Co–Co bond in  $\text{Ru}_1\text{Co}$  SAAs. The Ru K-edge FT-EXAFS spectrum of Ru foil shows a peak at 2.35 Å, corresponding to the Ru–Ru metallic bond (Fig. 4d). In contrast, hcp- $\text{Ru}_1\text{Co}$ , hcp/fcc- $\text{Ru}_1\text{Co}$ , and fcc- $\text{Ru}_1\text{Co}$  exhibit the prominent peaks at 2.10, 2.13, and 2.17 Å, respectively. The significant differences in peak positions between Ru foil and  $\text{Ru}_1\text{Co}$  SAAs suggest that the prominent peak of  $\text{Ru}_1\text{Co}$  SAAs is not contributed by Ru–Ru metallic bond, but Ru–Co metallic bond. The absence of Ru–Ru bond further confirms the atomic dispersion of Ru in  $\text{Ru}_1\text{Co}$  SAAs. Notably, the Ru–Co bond length in hcp- $\text{Ru}_1\text{Co}$  is shorter than that in fcc- $\text{Ru}_1\text{Co}$  and hcp/fcc- $\text{Ru}_1\text{Co}$ , suggesting enhanced interatomic interactions between Ru and Co in hcp- $\text{Ru}_1\text{Co}$ , consistent with the XANES results.

The least-squares EXAFS fitting curves and fitting parameters are provided in Supplementary Figs. 8–17 and Tables 2 and 3. The Co K-edge EXAFS oscillation functions reveal minor variations in both oscillation frequencies and amplitudes for hcp- $\text{Ru}_1\text{Co}$ , hcp/fcc- $\text{Ru}_1\text{Co}$ , and fcc- $\text{Ru}_1\text{Co}$ , indicating similar coordination environment for Co species (Supplementary Fig. 18). In contrast, the Ru K-edge EXAFS oscillation functions of  $\text{Ru}_1\text{Co}$  SAAs exhibit significant differences, reflecting substantial variations induced by crystal phase differences (Fig. 4e). The Co K-edge wavelet-transformed EXAFS (WT-EXAFS) contour plot of Co foil shows a local maximum at  $k = 7.21 \text{ \AA}^{-1}$  and  $R = 2.17 \text{ \AA}$ , similar to that of hcp- $\text{Ru}_1\text{Co}$  ( $k = 7.25 \text{ \AA}^{-1}$ ,  $R = 2.17 \text{ \AA}$ ), hcp/fcc- $\text{Ru}_1\text{Co}$  ( $k = 7.42 \text{ \AA}^{-1}$ ,  $R = 2.17 \text{ \AA}$ ), and fcc- $\text{Ru}_1\text{Co}$  ( $k = 7.59 \text{ \AA}^{-1}$ ,  $R = 2.17 \text{ \AA}$ ) (Supplementary Fig. 19). However, the Ru K-edge WT-EXAFS contour plot reveals that hcp- $\text{Ru}_1\text{Co}$  exhibits a local maximum at  $k = 7.69 \text{ \AA}^{-1}$  and  $R = 2.10 \text{ \AA}$ , which is significantly different from Ru foil ( $k = 9.52 \text{ \AA}^{-1}$ ,  $R = 2.35 \text{ \AA}$ ) and assigned to Ru–Co bond (Fig. 4f, i). Additionally, the lower  $R$  value in hcp- $\text{Ru}_1\text{Co}$  (2.10 Å) in comparison with hcp/fcc- $\text{Ru}_1\text{Co}$  (2.13 Å) and fcc- $\text{Ru}_1\text{Co}$  (2.17 Å) further confirms the shorter Ru–Co bond in hcp- $\text{Ru}_1\text{Co}$  (Fig. 4g, h). These results collectively confirm that hcp- $\text{Ru}_1\text{Co}$  possesses a shorter Ru–Co bond and thus stronger interatomic interaction compared to hcp/fcc- $\text{Ru}_1\text{Co}$  and fcc- $\text{Ru}_1\text{Co}$ .

To further confirm the atomic dispersion of Ru in  $\text{Ru}_1\text{Co}$  SAAs with different crystal phases, in situ CO diffuse reflectance infrared Fourier transform spectroscopy (CO-DRIFTS) is performed (Fig. 4j and





**Fig. 2 | Characterization of hcp-Ru<sub>1</sub>Co.** **a** TEM image of hcp-Ru<sub>1</sub>Co. **b** HAADF-STEM image of hcp-Ru<sub>1</sub>Co. **c** 3D surface plots converted from the cyan square in (b). **d** High-resolution AC-HAADF-STEM image of hcp-Ru<sub>1</sub>Co. **e** Enlarged AC-HAADF-STEM image taken from the cyan square in (d). **f** The corresponding FFT pattern. **g** and **h** The simulated atomic model (**g**) and the electron diffraction pattern (**h**) of

hcp-Co viewed along the [110] zone axis. **i** and **j** Intensity profiles from the orange rectangles in (d). **k–n** HAADF-STEM image (**k**) and corresponding elemental mappings (**l–n**) of hcp-Ru<sub>1</sub>Co. Source data for this figure are provided as a Source Data file.

Supplementary Fig. 20). Following CO adsorption at room temperature, two broad peaks at 2170 and 2121 cm<sup>-1</sup> are observed, corresponding to the mononuclear (Ru<sup>δ+</sup>(CO)) and tricarbonyl species adsorbed on single Ru atom (Ru<sup>δ+</sup>(CO)<sub>3</sub>), respectively<sup>18–20</sup>. The absence of peaks below 2000 cm<sup>-1</sup>, which is the fingerprint of bridge-bonded CO, confirms the absence of Ru clusters or nanoparticles<sup>21,22</sup>.

### Electrocatalytic NO<sub>3</sub>RR performance

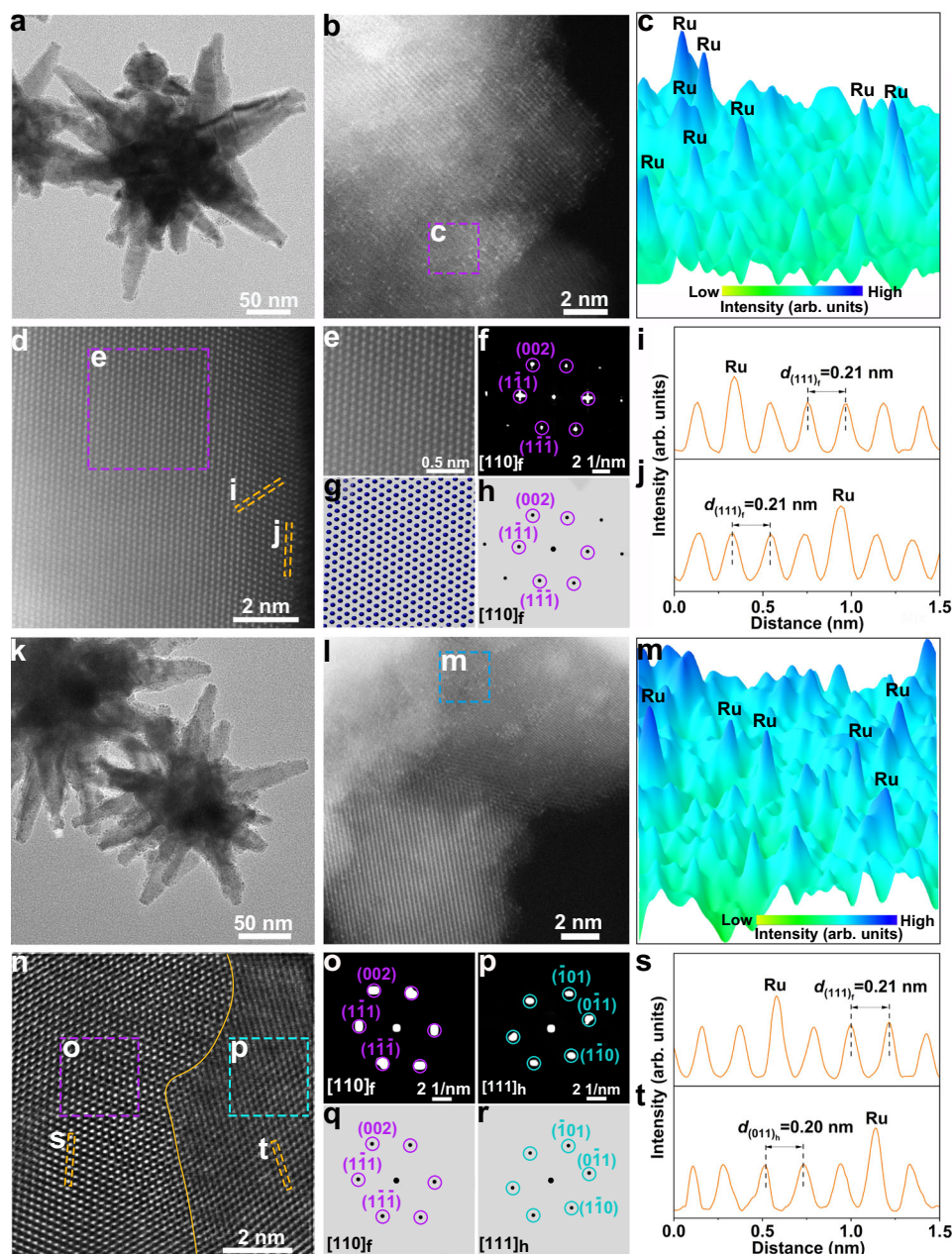
The electrocatalytic NO<sub>3</sub>RR performance is evaluated using an H-type cell. Ru<sub>1</sub>Co SAAs supported on Ni foam (NF) serve as the working electrode, with Ag/AgCl (saturated KCl) and Pt wire as the reference and counter electrodes, respectively. The electrolyte contains 0.5 M Na<sub>2</sub>SO<sub>4</sub> and 0.1 M NaOH with 200 ppm NO<sub>3</sub><sup>-</sup>-N. All potentials are referenced to the RHE scale. Figure 5a displays the linear sweep voltammetry (LSV) curves of Ru<sub>1</sub>Co SAAs in electrolyte with/without 200 ppm NO<sub>3</sub><sup>-</sup>-N. Apparently, upon the addition of NO<sub>3</sub><sup>-</sup>, significant enhancement in current density is observed, indicating the occurrence of NO<sub>3</sub>RR. Notably, hcp-Ru<sub>1</sub>Co demonstrates the highest current density in the presence of NO<sub>3</sub><sup>-</sup> and the lowest current density in the absence of NO<sub>3</sub><sup>-</sup>, indicating superior NO<sub>3</sub>RR activity and suppressed hydrogen evolution reaction (HER) (Supplementary Fig. 21).

The NO<sub>3</sub>RR performance of Ru<sub>1</sub>Co SAAs is systematically investigated through chronoamperometric tests at different potentials. The

concentrations of NO<sub>3</sub><sup>-</sup>-N and NH<sub>4</sub><sup>+</sup>-N are quantified by colorimetric methods via UV-Vis spectrophotometer (Supplementary Figs. 22 and 23). As shown in Fig. 5b and Supplementary Fig. 24, hcp-Ru<sub>1</sub>Co exhibits superior performance with maximum NH<sub>3</sub> yield rate ( $Y_{\text{NH}_3}$ ) of  $1.33 \pm 0.06 \text{ mg h}^{-1} \text{ cm}^{-2}$  at -0.1 V and NH<sub>3</sub> Faradaic efficiency ( $FE_{\text{NH}_3}$ ) of  $96.78 \pm 1.97\%$  at 0 V, significantly outperforming hcp/fcc-Ru<sub>1</sub>Co ( $0.90 \pm 0.06 \text{ mg h}^{-1} \text{ cm}^{-2}$ ,  $84.41 \pm 3.70\%$ ) and fcc-Ru<sub>1</sub>Co ( $0.39 \pm 0.05 \text{ mg h}^{-1} \text{ cm}^{-2}$ ,  $56.94 \pm 2.60\%$ ). The minimal concentrations of by-products (i.e., NO<sub>2</sub><sup>-</sup>, N<sub>2</sub>H<sub>4</sub>, N<sub>2</sub>, and H<sub>2</sub>) confirm the high NH<sub>3</sub> selectivity of hcp-Ru<sub>1</sub>Co (Supplementary Figs. 25–31). At 0 V, hcp-Ru<sub>1</sub>Co demonstrates higher values of  $Y_{\text{NH}_3}$ ,  $FE_{\text{NH}_3}$ , NO<sub>3</sub><sup>-</sup> conversion ( $C_{\text{NO}_3^-}$ ), NH<sub>3</sub> selectivity ( $S_{\text{NH}_3}$ ), half-cell energy efficiencies of NH<sub>3</sub> ( $EE_{\text{NH}_3}$ ) and NH<sub>3</sub> partial current density ( $j_{\text{NH}_3}$ ) compared to hcp/fcc-Ru<sub>1</sub>Co and fcc-Ru<sub>1</sub>Co (Fig. 5c and Supplementary Figs. 32 and 33). Notably, under high-concentration conditions (1400 ppm NO<sub>3</sub><sup>-</sup>-N), hcp-Ru<sub>1</sub>Co delivers  $Y_{\text{NH}_3}$  of  $11.65 \pm 0.46 \text{ mg h}^{-1} \text{ cm}^{-2}$  at -0.1 V and  $FE_{\text{NH}_3}$  of 100% at 0 V (Supplementary Fig. 34). These metrics position it among the most active metal-based catalysts for NO<sub>3</sub>RR (Supplementary Table 4).

EC and NH<sub>3</sub> production cost analyses are explored only considering the price of renewable electricity (0.03 \$<sub>USD</sub> kWh<sup>-1</sup>, full leveled cost of electricity for utility solar power according to the announcement by the US Department of Energy for the 2030



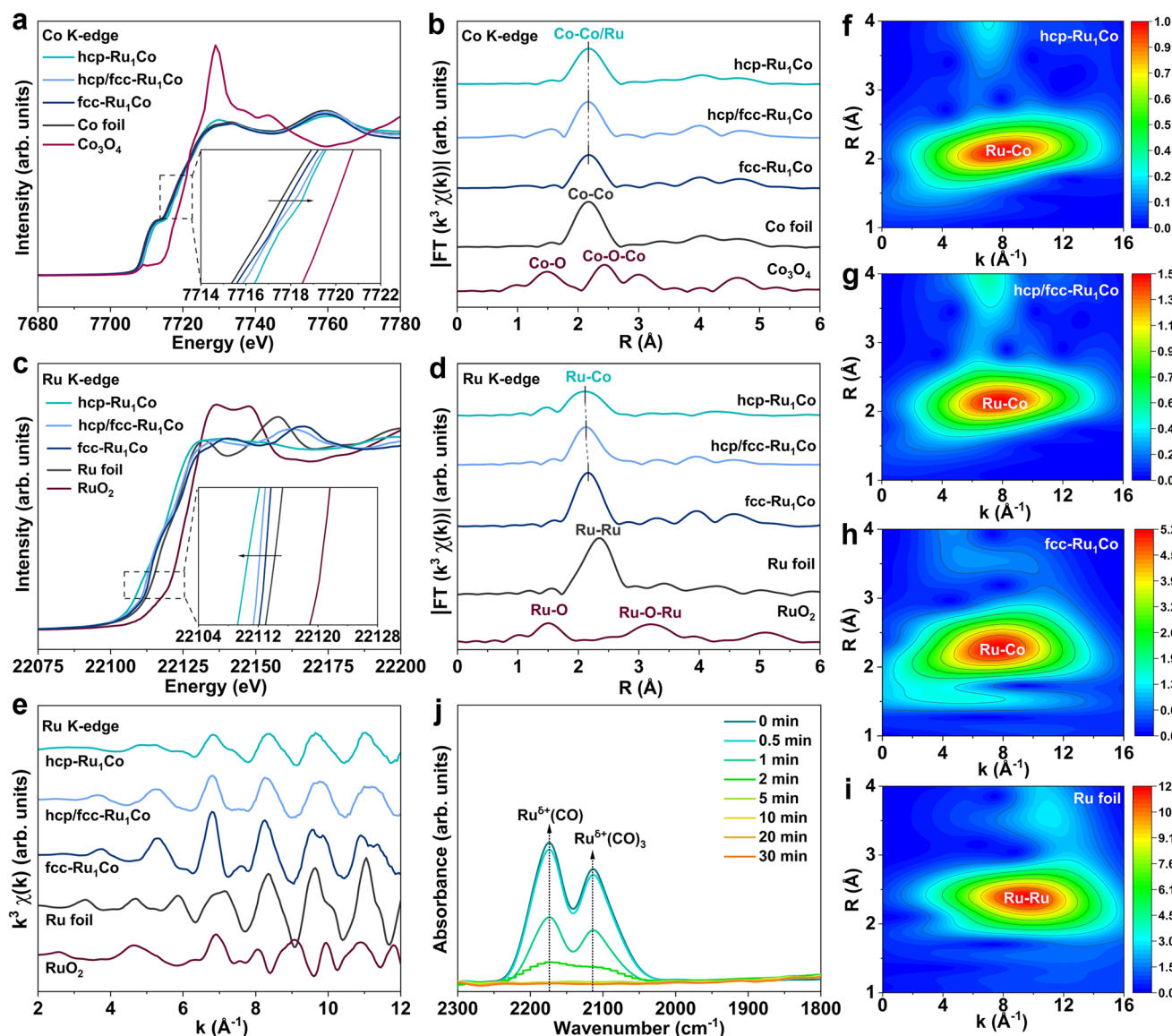


**Fig. 3 | Characterization of fcc-Ru<sub>1</sub>Co and hcp/fcc-Ru<sub>1</sub>Co.** **a** TEM image of fcc-Ru<sub>1</sub>Co. **b** AC-HAADF-STEM image of fcc-Ru<sub>1</sub>Co. **c** 3D surface plots converted from the purple square in **(b)**. **d** High-resolution AC-HAADF-STEM image of fcc-Ru<sub>1</sub>Co. **e** Enlarged HAADF-STEM image extracted from the purple square in **(d)**. **f** The corresponding FFT pattern. **g** and **h** The simulated atomic model **(g)** and the electron diffraction pattern **(h)** of fcc-Co oriented along the [110] zone axis. **i** and **j** Intensity profiles from the orange rectangles in **(d)**. **k** TEM image of hcp/fcc-Ru<sub>1</sub>Co.

**l** AC-HAADF-STEM image of hcp/fcc-Ru<sub>1</sub>Co. **m** 3D surface plots extracted from the blue square in **(h)**. **n** High-resolution AC-HAADF-STEM image of hcp/fcc-Ru<sub>1</sub>Co. **o** and **p** FFT patterns extracted from the squares in **(n)**. **q** and **r** The simulated electron diffraction patterns oriented along the [110]<sub>fcc</sub> and [111]<sub>hcp</sub> zone axes. **s** and **t** Intensity profiles from the rectangles in **(n)**. Source data for this figure are provided as a Source Data file.

target)<sup>23–25</sup>. As shown in Supplementary Fig. 35 and Fig. 5d, EC and NH<sub>3</sub> production cost of hcp-Ru<sub>1</sub>Co are calculated as  $19.04 \pm 1.10 \text{ kWh kg}^{-1}$  and  $0.57 \pm 0.03 \text{ USD kg}^{-1}$  at 0.1 V, respectively, significantly lower than those of hcp/fcc-Ru<sub>1</sub>Co ( $37.0 \pm 0.37 \text{ kWh kg}^{-1}$ ,  $1.11 \pm 0.01 \text{ USD kg}^{-1}$ ) and fcc-Ru<sub>1</sub>Co ( $288.78 \pm 0.50 \text{ kWh kg}^{-1}$ ,  $8.66 \pm 0.02 \text{ USD kg}^{-1}$ ). Notably, the EC values of hcp-Ru<sub>1</sub>Co at all potentials are significantly lower than commercial benchmarks ( $1\text{--}1.5 \text{ \$ kg}^{-1}$ )<sup>26</sup>, highlighting its industrial viability. Temperature-dependent  $Y_{\text{NH}_3}$  measurements reveal the apparent activation energy ( $E_a$ ) of  $3.49 \text{ kJ mol}^{-1}$  for hcp-Ru<sub>1</sub>Co, significantly lower than that of hcp/fcc-Ru<sub>1</sub>Co ( $14.22 \text{ kJ mol}^{-1}$ ) and fcc-Ru<sub>1</sub>Co ( $25.55 \text{ kJ mol}^{-1}$ ),

confirming the accelerated NO<sub>3</sub>RR kinetics (Fig. 5e and Supplementary Fig. 36). In addition, hcp-Ru<sub>1</sub>Co possesses a larger electrochemically active surface area (ECSA) compared to hcp/fcc-Ru<sub>1</sub>Co and fcc-Ru<sub>1</sub>Co (Supplementary Fig. 37, Table 5), consistent with the N<sub>2</sub> adsorption–desorption results (Supplementary Fig. 38).  $Y_{\text{NH}_3}$  values normalized to ECSA and Brunauer–Emmett–Teller (BET) surface area indicate the superior intrinsic activity of hcp-Ru<sub>1</sub>Co (Supplementary Figs. 39 and 40). Electrochemical impedance spectroscopy (EIS) reveals reduced charge transfer impedance for hcp-Ru<sub>1</sub>Co, attributed to its distinctive hcp structure and large ECSA (Supplementary Fig. 41).



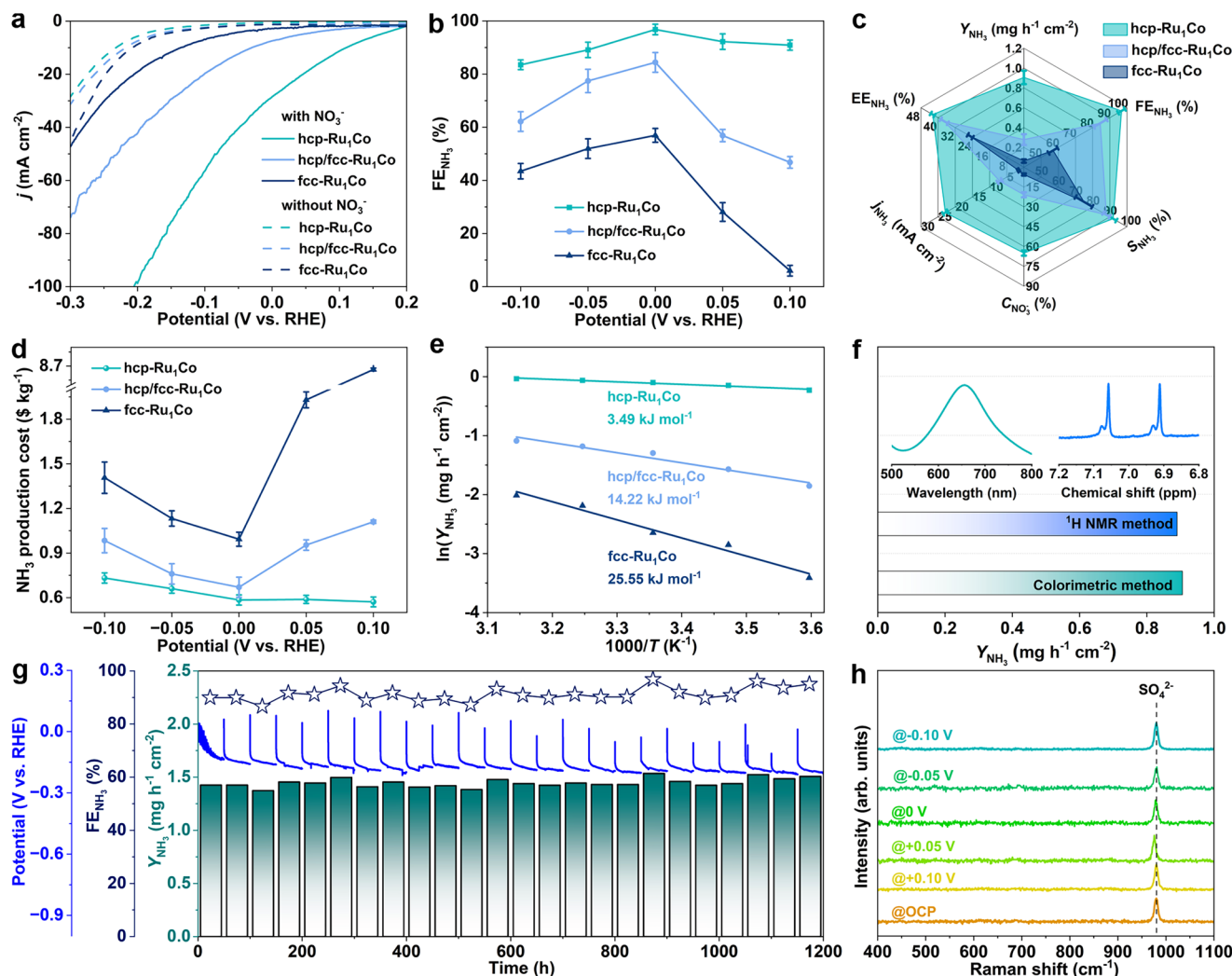
**Fig. 4 | Chemical state and coordination environment.** **a** The normalized Co K-edge XANES spectra of hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, fcc-Ru<sub>1</sub>Co, Co foil, and Co<sub>3</sub>O<sub>4</sub>. **b** The Co K-edge FT-EXAFS spectra of hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, fcc-Ru<sub>1</sub>Co, Co foil, and Co<sub>3</sub>O<sub>4</sub>. **c** The normalized Ru K-edge XANES spectra of hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, fcc-Ru<sub>1</sub>Co, Ru foil, and RuO<sub>2</sub>. **d** The Ru K-edge FT-EXAFS spectra of hcp-

Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, fcc-Ru<sub>1</sub>Co, Ru foil, and RuO<sub>2</sub>. **e** The Ru K-edge EXAFS spectra of hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, fcc-Ru<sub>1</sub>Co, Ru foil, and RuO<sub>2</sub>. **f-i** The WT-EXAFS contour plots of hcp-Ru<sub>1</sub>Co (**f**), hcp/fcc-Ru<sub>1</sub>Co (**g**), fcc-Ru<sub>1</sub>Co (**h**), and Ru foil (**i**) at Ru K-edge. **j** In situ CO-DRIFTS spectra of hcp-Ru<sub>1</sub>Co at room temperature. Source data for this figure are provided as a Source Data file.

To verify that the produced NH<sub>3</sub> originates from the NO<sub>3</sub>RR process catalyzed by hcp-Ru<sub>1</sub>Co, control experiments are carried out. Negligible NH<sub>3</sub> is detected in solutions of 0.5 M Na<sub>2</sub>SO<sub>4</sub> and 0.1 M NaOH at 0 V or in solutions of 0.5 M Na<sub>2</sub>SO<sub>4</sub> and 0.1 M NaOH with 200 ppm NO<sub>3</sub><sup>-</sup>-N at open circuit potential (OCP), and using pure NF substrate as the working electrode (Supplementary Fig. 42). <sup>15</sup>N isotope labeling experiments employing <sup>15</sup>NO<sub>3</sub><sup>-</sup> as nitrogen source yield characteristic <sup>15</sup>NH<sub>4</sub><sup>+</sup> peaks at  $\delta = 6.91$  and 7.06 ppm in <sup>1</sup>H nuclear magnetic resonance (NMR) spectrum (Supplementary Fig. 43), confirming NH<sub>3</sub> generation through NO<sub>3</sub>RR (Supplementary Fig. 44).  $Y_{\text{NH}_3}$  values obtained from <sup>1</sup>H NMR method match those from colorimetric analysis (Fig. 5f), validating both analytical methods.

Durability is a pivotal aspect in evaluating the performance of electrocatalysts. As depicted in Supplementary Fig. 45, negligible changes in  $Y_{\text{NH}_3}$  and  $FE_{\text{NH}_3}$  of hcp-Ru<sub>1</sub>Co during 12 consecutive recycling tests demonstrate its robust electrochemical stability.

Chronopotentiometric test under continuous electrolyte flow (2 mL min<sup>-1</sup>, Supplementary Fig. 46) maintains stable  $Y_{\text{NH}_3}$  and  $FE_{\text{NH}_3}$  over 1200 h of prolonged operation (Fig. 5g). Post-stability characterizations confirm the retention of nano-urchin morphology, atomic Ru dispersion (Supplementary Fig. 47), crystal structure (Supplementary Fig. 48), and chemical states (Supplementary Fig. 49). In situ Raman spectroscopy during NO<sub>3</sub>RR only detects the vibration mode of SO<sub>4</sub><sup>2-</sup> (981 cm<sup>-1</sup>) from electrolyte (Fig. 5h, Supplementary Fig. 50)<sup>27</sup>. No additional Raman peaks are observed at all applied potentials, suggesting that hcp-Ru<sub>1</sub>Co does not transform into oxide during NO<sub>3</sub>RR. Furthermore, hcp-Ru<sub>1</sub>Co exhibits competitive performance across a broad range of NO<sub>3</sub><sup>-</sup>-N concentrations (100–500 ppm), suggesting its wide applicability (Supplementary Fig. 51). As current density increases from 50 to 500 mA cm<sup>-2</sup>,  $Y_{\text{NH}_3}$  of hcp-Ru<sub>1</sub>Co progressively rises, attaining a maximum value of 25.52 mg h<sup>-1</sup> cm<sup>-2</sup> at 500 mA cm<sup>-2</sup> (Supplementary Fig. 52).



**Fig. 5 | Electrochemical  $\text{NO}_3\text{RR}$  performance.** **a** LSV curves of hcp- $\text{Ru}_1\text{Co}$ , hcp/fcc- $\text{Ru}_1\text{Co}$ , and fcc- $\text{Ru}_1\text{Co}$  at a scan rate of  $5 \text{ mV s}^{-1}$  in an electrolyte containing  $0.5 \text{ M Na}_2\text{SO}_4$  and  $0.1 \text{ M NaOH}$  with and without  $200 \text{ ppm NO}_3^- \text{N}$  at room temperature ( $25^\circ\text{C}$ ). **b**  $\text{FE}_{\text{NH}_3}$  of hcp- $\text{Ru}_1\text{Co}$ , hcp/fcc- $\text{Ru}_1\text{Co}$ , and fcc- $\text{Ru}_1\text{Co}$  at different potentials. **c** Comparison of  $Y_{\text{NH}_3}$ ,  $\text{FE}_{\text{NH}_3}$ ,  $C_{\text{NO}_3^-}$ ,  $S_{\text{NH}_3}$ ,  $j_{\text{NH}_3}$ , and  $\text{EE}_{\text{NH}_3}$  over hcp- $\text{Ru}_1\text{Co}$ , hcp/fcc- $\text{Ru}_1\text{Co}$ , and fcc- $\text{Ru}_1\text{Co}$  at  $0 \text{ V}$ . **d**  $\text{NH}_3$  production cost of hcp- $\text{Ru}_1\text{Co}$ , hcp/fcc- $\text{Ru}_1\text{Co}$ , and fcc- $\text{Ru}_1\text{Co}$  at different potentials. **e**  $E_a$  of hcp- $\text{Ru}_1\text{Co}$ , hcp/fcc- $\text{Ru}_1\text{Co}$ , and fcc- $\text{Ru}_1\text{Co}$  at  $0 \text{ V}$ . **f**  $Y_{\text{NH}_3}$  of hcp- $\text{Ru}_1\text{Co}$  at  $0 \text{ V}$  obtained by colorimetric and  $^1\text{H}$  NMR methods (the insets are UV-Vis absorption and  $^1\text{H}$  NMR spectra of post-

electrolyzed solution over hcp- $\text{Ru}_1\text{Co}$  at  $0 \text{ V}$ ). **g** Chronopotentiometry curve of hcp- $\text{Ru}_1\text{Co}$  in an H-type continuous-flow cell at  $20 \text{ mA cm}^{-2}$  with corresponding  $Y_{\text{NH}_3}$  and  $\text{FE}_{\text{NH}_3}$ . **h** In situ Raman spectra of hcp- $\text{Ru}_1\text{Co}$  during chronopotentiometry test at different potentials in an electrolyte containing  $0.5 \text{ M Na}_2\text{SO}_4$  and  $0.1 \text{ M NaOH}$  with  $200 \text{ ppm NO}_3^- \text{N}$ . All potentials are referenced to the RHE scale without IR compensation. Catalyst loading amount for all  $\text{NO}_3\text{RR}$  tests is  $3 \text{ mg cm}^{-2}$ . Error bars represent the standard deviations from three independent measurements. Source data for this figure are provided as a Source Data file.

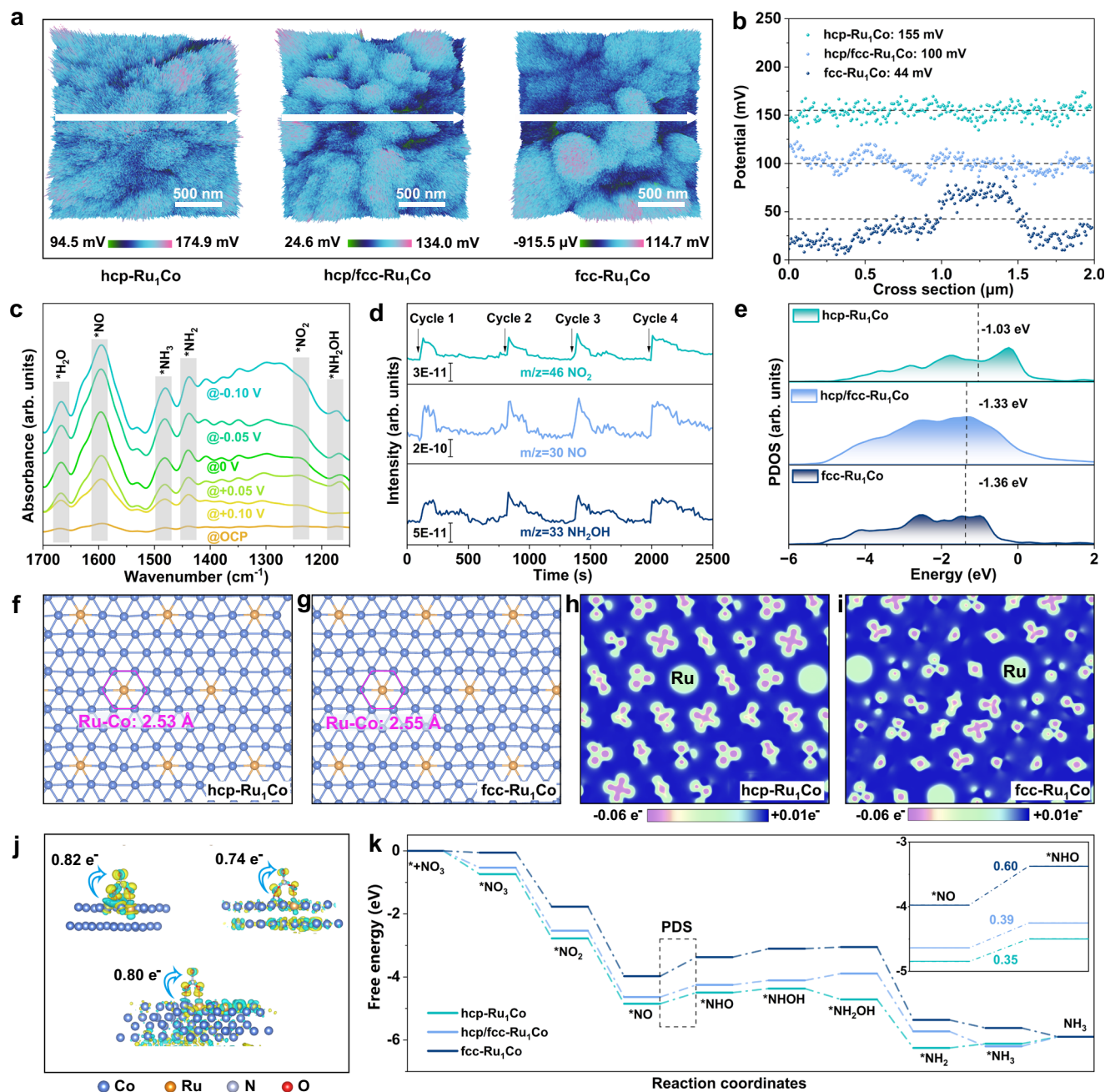
## Mechanistic studies

Recent studies have highlighted the critical role of catalyst surface potential in regulating  $\text{NO}_3^-$  adsorption, where elevated surface potentials significantly enhance  $\text{NO}_3^-$  adsorption and improve  $\text{NO}_3\text{RR}$  performance<sup>28–30</sup>. To explore the surface potential of  $\text{Ru}_1\text{Co}$  SAAs, Kelvin probe force microscopy (KPFM) is conducted (Fig. 6a). The average surface potential of hcp- $\text{Ru}_1\text{Co}$  achieved by contact potential difference is  $155 \text{ mV}$ , substantially exceeding that of hcp/fcc- $\text{Ru}_1\text{Co}$  ( $100 \text{ mV}$ ) and fcc- $\text{Ru}_1\text{Co}$  ( $44 \text{ mV}$ ) (Fig. 6b). This enhanced surface potential of hcp- $\text{Ru}_1\text{Co}$ , attributed to its unique hcp structure, facilitates  $\text{NO}_3^-$  adsorption and thereby accelerates the reaction kinetics. To quantitatively assess  $\text{NO}_3^-$  adsorption behavior,  $\text{Ru}_1\text{Co}$  SAAs are immersed in an electrolyte containing  $200 \text{ ppm NO}_3^- \text{N}$  and agitated for  $30 \text{ min}$ , the  $\text{NO}_3^-$  adsorption capacity ( $q_e$ ) is determined by measuring the concentration of  $\text{NO}_3^-$  in solution before and after agitation. As shown in Supplementary Fig. 53, hcp- $\text{Ru}_1\text{Co}$  achieves a  $q_e$  value of  $1.91 \pm 0.05 \mu\text{mol mg}_{\text{cat}}^{-1}$ , significantly surpassing hcp/fcc- $\text{Ru}_1\text{Co}$

( $1.20 \pm 0.03 \mu\text{mol mg}_{\text{cat}}^{-1}$ ) and fcc- $\text{Ru}_1\text{Co}$  ( $0.77 \pm 0.02 \mu\text{mol mg}_{\text{cat}}^{-1}$ ). Furthermore, Fourier transform infrared (FT-IR) analysis of  $\text{Ru}_1\text{Co}$  SAAs with adsorbed  $\text{NO}_3^-$  further confirms the enhanced  $\text{NO}_3^-$  adsorption on hcp- $\text{Ru}_1\text{Co}$ , evidenced by intensified absorption at  $1350 \text{ cm}^{-1}$  corresponding to anti-symmetric stretching vibrations of  $\text{NO}_3^-$  (Supplementary Fig. 54)<sup>31</sup>. These findings collectively demonstrate that hcp- $\text{Ru}_1\text{Co}$  possesses a stronger  $\text{NO}_3^-$  adsorption, contributing to its enhanced  $\text{NO}_3\text{RR}$  performance.

To probe into the intermediates formed during the  $\text{NO}_3\text{RR}$  process, in situ attenuated total reflection surface-enhanced infrared absorption spectroscopy (ATR-SEIRAS, Supplementary Fig. 55) and online differential electrochemical mass spectrometry (DEMS, Supplementary Fig. 56) are carried out. In situ ATR-SEIRAS spectra of hcp- $\text{Ru}_1\text{Co}$  (Fig. 6c) display characteristic peaks at  $1595$ ,  $1483$ ,  $1438$ ,  $1235$ , and  $1168 \text{ cm}^{-1}$ , attributed to the vibrations of  $^*\text{NO}$ ,  $^*\text{NH}_3$ ,  $^*\text{NH}_2$ ,  $^*\text{NO}_2$ , and  $^*\text{NH}_2\text{OH}$ , respectively<sup>32,33</sup>. The peak at  $1668 \text{ cm}^{-1}$  is assigned to the bending vibration of the adsorbed  $\text{H}_2\text{O}$ <sup>34</sup>. Online DEMS analysis during





**Fig. 6 | Mechanistic studies.** **a** Surface potential distribution of hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, and fcc-Ru<sub>1</sub>Co. **b** The corresponding surface potentials. **c** In situ ATR-SEIRAS spectra of hcp-Ru<sub>1</sub>Co at different potentials. **d** Online DEMS spectra of hcp-Ru<sub>1</sub>Co during the NO<sub>3</sub>RR process. **e** The PDOS profiles of hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, and fcc-Ru<sub>1</sub>Co. The vertical dashed lines indicate the position of the *d*-band center. **f** and **g** The optimized structure models of hcp-Ru<sub>1</sub>Co (**f**) and fcc-Ru<sub>1</sub>Co (**g**). **h** and **i** 2D deformation charge density difference maps of hcp-Ru<sub>1</sub>Co (**h**) and fcc-Ru<sub>1</sub>Co (**i**). **j** The charge density difference of \*NO<sub>3</sub> adsorbed on hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, and fcc-Ru<sub>1</sub>Co (electron accumulation and depletion are indicated by yellow and cyan regions, respectively). **k** The free energy diagrams of NO<sub>3</sub>RR over hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, and fcc-Ru<sub>1</sub>Co. Source data for this figure are provided as a Source Data file.

chronoamperometry test at 0 V reveals the mass signals of mass-to-charge ratios (*m/z*) of 46, 33, 32, 31, 30, and 17, attributed to \*NO<sub>2</sub>, \*NH<sub>2</sub>OH, \*NHOH, \*NHO, \*NO, and \*NH<sub>3</sub>, respectively (Fig. 6d and Supplementary Fig. 57). Based on these detected intermediates, the NO<sub>3</sub>RR pathway is deduced, involving the following key intermediates: \*NO<sub>3</sub> → \*NO<sub>2</sub> → \*NO → \*NHO → \*NHOH → \*NH<sub>2</sub>OH → \*NH<sub>2</sub> → \*NH<sub>3</sub>.

To gain preliminary insights into the enhanced NO<sub>3</sub>RR performance of hcp-Ru<sub>1</sub>Co, density functional theory (DFT) calculations are performed. The optimized structure models are provided in Supplementary Fig. 58 and Supplementary Data 1. Partial density of state

(PDOS) profiles reveal that hcp-Ru<sub>1</sub>Co exhibits a *d*-band center at −1.03 eV, positioned closer to the Fermi level compared to hcp/fcc-Ru<sub>1</sub>Co (−1.33 eV) and fcc-Ru<sub>1</sub>Co (−1.36 eV) (Fig. 6e). The upshift of the *d*-band center for hcp-Ru<sub>1</sub>Co could theoretically favor the adsorption of intermediates. Additionally, the effect of the crystal structure on Ru–Co interatomic interaction is explored. As shown in the structure models (Fig. 6f, g), hcp-Ru<sub>1</sub>Co possesses a relatively shorter Ru–Co bond length (2.53 Å) than fcc-Ru<sub>1</sub>Co (2.55 Å), consistent with XAS findings. 2D deformation charge density maps and Bader charge analysis demonstrate electrons transfer from Co to Ru (Fig. 6h, i), with

hcp-Ru<sub>1</sub>Co showing a slightly larger charge transfer, indicating an enhanced Ru–Co interatomic interaction in hcp-Ru<sub>1</sub>Co.

Gibbs free energy of NO<sub>3</sub><sup>−</sup> adsorption ( $\Delta G_{\text{NO}_3}$ ) reveals that hcp-Ru<sub>1</sub>Co exhibits a more negative  $\Delta G_{\text{NO}_3}$  of −0.74 eV compared to hcp/fcc-Ru<sub>1</sub>Co (−0.53 eV) and fcc-Ru<sub>1</sub>Co (−0.05 eV) (Supplementary Fig. 59, Supplementary Data 1). This suggests a stronger NO<sub>3</sub><sup>−</sup> adsorption on hcp-Ru<sub>1</sub>Co, which aligns with the results of NO<sub>3</sub><sup>−</sup> adsorption capacity and FT-IR experiments in Supplementary Figs. 53 and 54. Charge density difference maps and Bader charge analysis demonstrate that 0.82 electrons are transferred from hcp-Ru<sub>1</sub>Co to \*NO<sub>3</sub>, exceeding the amount transferred on hcp/fcc-Ru<sub>1</sub>Co (0.80 electrons) and fcc-Ru<sub>1</sub>Co (0.74 electrons) (Fig. 6j). Free energy diagrams identify the hydrogenation of \*NO (\*NO → \*NHO) as the potential-determining step (PDS) for Ru<sub>1</sub>Co SAAs (Fig. 6k, Supplementary Figs. 60–62, Supplementary Data 1). Notably, hcp-Ru<sub>1</sub>Co exhibits a lower energy barrier of PDS (0.35 eV) compared to hcp/fcc-Ru<sub>1</sub>Co (0.39 eV) and fcc-Ru<sub>1</sub>Co (0.60 eV). Considering that HER is a primary competitive reaction, the free energy of \*H adsorption is calculated (Supplementary Figs. 63, 64, Supplementary Data 1). The free energy required to generate by-product H<sub>2</sub> for hcp-Ru<sub>1</sub>Co is 0.91 eV, higher than that for hcp/fcc-Ru<sub>1</sub>Co (0.51 eV) and fcc-Ru<sub>1</sub>Co (0.09 eV). This suggests that hcp-Ru<sub>1</sub>Co could potentially suppress the competing HER.

### The performance of the Zn-NO<sub>3</sub><sup>−</sup> battery

The Zn-NO<sub>3</sub><sup>−</sup> battery offers dual functionality by generating electricity while converting NO<sub>3</sub><sup>−</sup> pollutants into valuable NH<sub>3</sub><sup>35</sup>. The Zn-NO<sub>3</sub><sup>−</sup> battery is constructed by anchoring hcp-Ru<sub>1</sub>Co on NF as the cathode, paired with a zinc plate anode (Supplementary Fig. 65). The hcp-Ru<sub>1</sub>Co assembled Zn-NO<sub>3</sub><sup>−</sup> battery exhibits a stable OCP of 1.405 V vs. Zn/Zn<sup>2+</sup> (Supplementary Fig. 66). Two such batteries connected in series can power a bulb of 1.5 V (Supplementary Fig. 67). Additionally, the hcp-Ru<sub>1</sub>Co assembled Zn-NO<sub>3</sub><sup>−</sup> battery delivers a high power-density of 6.55 mW cm<sup>−2</sup>, surpassing most recently reported Zn-NO<sub>3</sub><sup>−</sup> batteries (Supplementary Fig. 68 and Table 6). At current densities of 2, 4, and 6 mA cm<sup>−2</sup>, the specific capacities of this battery are 576.81, 616.84, and 668.51 mAh g<sup>−1</sup>, respectively (Supplementary Fig. 69). Consequently, the corresponding energy densities under these conditions are calculated as 470.03, 448.13, and 416.04 mWh g<sup>−1</sup>. The battery demonstrates high rate-capability and stable operation at current densities ranging from 1 to 20 mA cm<sup>−2</sup> (Supplementary Fig. 70). Continuous discharge–charge cycling at 2 mA cm<sup>−2</sup> suggests its robust stability (Supplementary Fig. 71). Additionally, it achieves an  $\gamma_{\text{NH}_3}$  of  $1.72 \pm 0.02 \text{ mg h}^{-1} \text{ cm}^{-2}$  at 50 mA cm<sup>−2</sup> and a  $\text{FE}_{\text{NH}_3}$  of  $90.93 \pm 0.80\%$  at 40 mA cm<sup>−2</sup> (Supplementary Fig. 72). Minimal fluctuations in both  $\gamma_{\text{NH}_3}$  and  $\text{FE}_{\text{NH}_3}$  during consecutive recycling test at 40 mA cm<sup>−2</sup> confirm robust long-term stability (Supplementary Fig. 73).

### Discussion

In summary, Ru<sub>1</sub>Co SAAs with distinct crystal phases, i.e., hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, and fcc-Ru<sub>1</sub>Co, are successfully synthesized through precise control of the phase transition process and exhibit crystal phase-dependent performance in NO<sub>3</sub>RR to NH<sub>3</sub>. Notably, hcp-Ru<sub>1</sub>Co demonstrates superior catalytic performance with  $\text{FE}_{\text{NH}_3}$  of  $96.78 \pm 1.97\%$  at 0 V, EC of  $19.04 \pm 1.10 \text{ kWh kg}^{-1}$ , NH<sub>3</sub> production cost of  $0.57 \pm 0.03 \text{ \$}_{\text{USD}} \text{ kg}^{-1}$ , and stable operation exceeding 1200 h, significantly outperforming hcp/fcc-Ru<sub>1</sub>Co and fcc-Ru<sub>1</sub>Co. Insightful experiments and theoretical calculations reveal that hcp-Ru<sub>1</sub>Co is featured with shorter Ru–Co interatomic distances, stronger Ru–Co interatomic interactions, and more positive surface potential, which enhance the adsorption capacity of NO<sub>3</sub><sup>−</sup>, reduces the free energy barrier of PDS, and suppresses the HER. Furthermore, hcp-Ru<sub>1</sub>Co, when integrated as the cathode electrocatalyst into Zn-NO<sub>3</sub><sup>−</sup> battery, demonstrates its significant potential for application in advanced

energy devices. This study not only achieves precise control over the crystal phase of SAAs but also provides comprehensive insights into the relationship between the crystal structure of SAAs and catalytic performance.

### Methods

#### Chemicals and reagents

Cobalt chloride hexahydrate (CoCl<sub>2</sub>·6H<sub>2</sub>O, 99.0 wt%), ruthenium(III) chloride hydrate (RuCl<sub>3</sub>·xH<sub>2</sub>O, 99.95 wt%), 1,4-butanediol (98 wt%), sodium sulfate anhydrous (Na<sub>2</sub>SO<sub>4</sub>, 99.0 wt%), deuterium oxide (D<sub>2</sub>O, 99.9 at% D), sodium hypochlorite solution (NaClO, available chlorine 5.5–6.5 wt%), ammonium chloride-<sup>15</sup>N (<sup>15</sup>NH<sub>4</sub>Cl, 98.5 wt%), sodium nitrate-<sup>15</sup>N (Na<sup>15</sup>NO<sub>3</sub>, 98.5 wt%), maleic acid (C<sub>4</sub>H<sub>4</sub>O<sub>4</sub>, 98.0 wt%), salicylic acid (C<sub>7</sub>H<sub>6</sub>O<sub>3</sub>, 99.5 wt%), sodium citrate dihydrate (C<sub>6</sub>H<sub>5</sub>Na<sub>3</sub>O<sub>7</sub>·2H<sub>2</sub>O, 99.0 wt%), N-(1-naphthyl) ethylenediamine dihydrochloride (C<sub>12</sub>H<sub>14</sub>N<sub>2</sub>·2HCl, 98 wt%), phosphoric acid (H<sub>3</sub>PO<sub>4</sub>, 85 wt%), sulfanilamide (C<sub>6</sub>H<sub>8</sub>N<sub>2</sub>O<sub>2</sub>S, 99.5 wt%), and nitroferricyanide (III) dihydrate (Na<sub>2</sub>Fe(CN)<sub>5</sub>NO·2H<sub>2</sub>O, 99.0 wt%) were obtained from Shanghai Macklin Biochemical Co., Ltd. Sodium hydroxide (NaOH, ≥96.0 wt%), sulfuric acid (H<sub>2</sub>SO<sub>4</sub>, 95.0–98.0 wt%), hydrogen chloride (HCl, 36.0–38.0 wt%), and ammonium chloride (NH<sub>4</sub>Cl, ≥99.5 wt%) were purchased from Sinopharm Chemical Reagent Co., Ltd. Ethanol (C<sub>2</sub>H<sub>5</sub>OH, ≥99.7 wt%) was purchased from Tianjin Fuyu Fine Chemical Co., Ltd. Acetone (C<sub>3</sub>H<sub>6</sub>O, ≥99 wt%) was purchased from Yantai Far East Fine Chemical Co., Ltd. Nickel foam (NF, thickness: 2 mm) was purchased from Tianjin EVS Chemical Technology Co., Ltd. Nafion solution (D520, 5 wt%, Dupont) was purchased from Suzhou Sinero Technology Co., Ltd. Nafion 211 membrane (diameter: 3 cm, thickness: 25.4 μm) was purchased from SCI Materials Hub. All reagents were utilized without further purification. Deionized water with a resistivity of 18.2 MΩ was employed throughout all experimental procedures.

#### Synthesis of Ru<sub>1</sub>Co SAAs

0.08 M CoCl<sub>2</sub>·6H<sub>2</sub>O and 0.15 M NaOH were dissolved in 40 mL of 1,4-butanediol to form solution A. 0.015 g RuCl<sub>3</sub>·xH<sub>2</sub>O were dissolved in 5 mL of 1,4-butanediol to form solution B. Subsequently, solution B was gradually introduced into solution A under vigorous stirring for 30 min. The mixed solution was then heated to 230 °C for 20 min. The resulting product was washed with ethanol and acetone several times, and dried under vacuum at 60 °C for 3 h. Finally, the precursor powder was annealed at 300, 500, and 700 °C for 30 min at N<sub>2</sub> atmosphere with a heating rate of 5 °C min<sup>−1</sup> to form hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co and fcc-Ru<sub>1</sub>Co, respectively.

#### Fabrication of the working electrode

The working electrode was fabricated by immobilizing Ru<sub>1</sub>Co SAAs onto the pretreated nickel foam (NF) substrate. In detail, NF was sequentially pretreated by sonication in HCl solution (3 M), followed by thorough rinsing with ethanol and deionized water to remove surface impurities. Subsequently, the synthesized sample (hcp-Ru<sub>1</sub>Co, hcp/fcc-Ru<sub>1</sub>Co, and fcc-Ru<sub>1</sub>Co; 20 mg each) was dispersed in a mixed solution consisting of 950 μL ethanol and 50 μL Nafion under sonication for 0.5 h to form a homogeneous ink. Finally, the ink (300 μL) was dropped onto the surface of the pretreated NF (1 × 1 cm<sup>2</sup>), and dried in air for 30 min to form the working electrode. The mass loading of the catalyst was calculated to be 3 mg cm<sup>−2</sup>.

#### Physicochemical characterizations

XRD patterns were acquired using a Rigaku SmartLab powder diffractometer with Cu Kα radiation ( $\lambda = 1.5418 \text{ \AA}$ ). TEM images were recorded using a HITACHI H-8100 electron microscope with an operation voltage of 200 kV. AC-HAADF-STEM was conducted on ThermoFisher Scientific Themis microscope (300 kV) equipped with image and probe correctors, using a beam current of 2 pA, a convergence angle of 25 mrad, and a collection angle range of 55–220 mrad.

conditions. ICP-OES was carried out on an Agilent 5110 system. XPS measurements were performed on an ESCALABMK II spectrometer equipped with Mg K $\alpha$  excitation. The Cls peak at 284.8 eV was utilized for calibration. X-ray absorption spectroscopy (XAS) was carried out at the 1W1B beamline of the Shanghai Synchrotron Radiation Facility. In situ CO-DRIFTS experiments were performed on a Bruker Tensor II infrared spectrometer. UV-Vis absorbance spectra were collected using a SHIMADZU UV-1900 spectrophotometer.  $^1\text{H}$  NMR spectra were recorded on a Bruker Avance 500 MHz spectrometer. DEMS measurements were conducted on a QAS 100 system (Linglu Instruments Co. Ltd). FT-IR spectroscopy was performed using a Perkin-Elmer spectrometer. In-situ ATR-SEIRAS spectra were collected using an INVENIO S FT-IR spectrometer equipped with a liquid nitrogen-cooled mercury cadmium telluride (MCT) detector. Raman spectra were obtained using a LabRAM HR Evolution (Horiba) with a 532 nm excitation laser. KPFM images were acquired on a BRUKER Dimension Icon with ScanAsyst system.  $\text{N}_2$  adsorption-desorption isotherms were measured on a Quantachrome NOVA-3000 instrument.

### Electrochemical measurements

Electrochemical experiments were conducted in a H-type cell with a three-electrode configuration by CHI 760E electrochemical workstation (CH Instruments Inc., China). The cathodic and anodic chambers are separated by a Nafion 211 membrane (diameter: 3 cm, thickness: 25.4  $\mu\text{m}$ , DuPont). Prior to use, Nafion membrane underwent sequential pretreatment. First, the membrane was immersed in a 5%  $\text{H}_2\text{O}_2$  solution and maintained at 80  $^\circ\text{C}$  for 1 h to eliminate organic contaminants. Subsequently, the membrane was repeatedly rinsed with deionized water and immersed in deionized water at 80  $^\circ\text{C}$  for 1 h to ensure the complete removal of any residual  $\text{H}_2\text{O}_2$ . After pretreatment, the membrane was stored in deionized water under ambient conditions.

A saturated Ag/AgCl electrode and a Pt wire served as the reference and counter electrode, while nickel foam anchored with the prepared  $\text{Ru}_1\text{Co}$  SAAs (mass loading: 3  $\text{mg cm}^{-2}$ ) was used as the working electrode. All potentials were referenced to the RHE scale without iR compensation using Eq. (1):

$$E_{\text{RHE}} = E_{\text{Ag/AgCl}} + 0.197 + 0.059 \times \text{pH} \quad (1)$$

where the pH of electrolyte was measured to be  $12.98 \pm 0.12$  using a pH meter (Mettler Toledo).

The electrolyte containing 0.5 M  $\text{Na}_2\text{SO}_4$ , 0.1 M NaOH and 200 ppm  $\text{NO}_3^-$ -N, was prepared prior to the  $\text{NO}_3\text{RR}$  tests by dissolving 71.02 g of  $\text{Na}_2\text{SO}_4$  (0.5 mol), 4.00 g of NaOH (0.1 mol), and 1.21 g of  $\text{NaNO}_3$  in 1 L of deionized water within a volumetric flask. The solution was stored at room temperature (25  $^\circ\text{C}$ ) for subsequent use. The electrolyte volume in cathodic and anodic chamber is 12.5 mL.

LSV test was performed at a scan rate of 5  $\text{mV s}^{-1}$  at a potential range from 0.2 to -0.3 V vs. RHE at room temperature (25  $^\circ\text{C}$ ). Potentiostatic tests were conducted at different potentials for 1 h, with a stirring rate of 1500 r.p.m. at room temperature (25  $^\circ\text{C}$ ). After electrolysis, the electrolyte was analyzed by UV-Vis spectrophotometry. Electrochemical double-layer capacitance ( $C_{\text{dl}}$ ) was assessed using cyclic voltammetry in a non-Faradaic region (-0.45 to -0.55 V vs. Ag/AgCl) at different scan rates of 10, 20, 30, 40, 50, and 60  $\text{mV s}^{-1}$ . Electrochemical impedance spectroscopy (EIS) tests were conducted in a frequency range of 0.01 Hz–100 kHz at open circuit potential (-0.036 V vs. RHE) in an electrolyte containing 0.5 M  $\text{Na}_2\text{SO}_4$ , 0.1 M NaOH, and 200 ppm of  $\text{NO}_3^-$ -N.

### Determination of $\text{NO}_3^-$ -N concentration

$\text{NO}_3^-$ -N concentration was determined using UV-Vis spectrophotometry. Initially, 100  $\mu\text{L}$  of cathodic electrolyte were extracted and diluted to a total volume of 10 mL. Then, 200  $\mu\text{L}$  of HCl (1 M) were

incorporated to the above solution. Using UV-Vis spectrophotometry, the absorption intensities at wavelengths of 220 nm ( $A_{220\text{nm}}$ ) and 275 nm ( $A_{275\text{nm}}$ ) were recorded. The absorbance value ( $A$ ) was determined employing the equation:  $A = A_{220\text{nm}} - 2 \times A_{275\text{nm}}$ . The UV-Vis absorbance spectra of standard  $\text{NO}_3^-$ -N solutions with known concentrations were measured for calibration, resulting in the calibration equation:  $y = 0.110x + 0.031$  with an  $R^2$  value of 0.999.

### Determination of $\text{NH}_4^+$ -N concentration

The indophenol blue method was employed to quantify  $\text{NH}_4^+$ -N concentration. Initially, 40  $\mu\text{L}$  of cathodic electrolyte were obtained and diluted to a total volume of 4 mL. Subsequently, 4 mL of chromogenic agent composed of 1.0 M NaOH, 0.36 M  $\text{C}_7\text{H}_6\text{O}_3$ , and 0.17 M  $\text{C}_6\text{H}_5\text{Na}_3\text{O}_7 \cdot 2\text{H}_2\text{O}$ , 2 mL of NaClO (0.05 M), and 0.4 mL of complexing agent (1 wt%  $\text{Na}_2[\text{Fe}(\text{NO})(\text{CN})_5] \cdot 2\text{H}_2\text{O}$ ) were sequentially introduced into the aforementioned solution. Following 1 h's incubation, UV-Vis absorbance spectra were acquired, and the absorbance at 655 nm was recorded. The UV-Vis spectra of standard  $\text{NH}_4^+$ -N solutions with known concentrations were measured for calibration, resulting in the calibration equation:  $y = 0.459x + 0.032$  with an  $R^2$  value of 0.998.

### Determination of $\text{NO}_2^-$ -N concentration

Initially, 50  $\mu\text{L}$  of cathodic electrolyte were extracted and diluted to a total volume of 5 mL. Subsequently, 0.1 mL of color reagent composed of 12.9 mM  $\text{C}_{12}\text{H}_{14}\text{N}_2 \cdot 2\text{HCl}$ , 0.38 M  $\text{C}_6\text{H}_8\text{N}_2\text{O}_2\text{S}$  and 2.87 M  $\text{H}_3\text{PO}_4$ , were added to the above solution. Following 10 min's incubation, UV-Vis absorbance spectra were acquired, and the absorbance at 510 nm was recorded. The UV-Vis spectra of standard  $\text{NO}_2^-$ -N solutions with known concentrations were measured for calibration, resulting in the calibration equation:  $y = 0.370x + 0.001$  with an  $R^2$  value of 0.998.

### Determination of $\text{N}_2\text{H}_4$ -N concentration

$\text{N}_2\text{H}_4$ -N concentration was determined by the Watt and Chrisp method. Initially, a colorimetric reagent was prepared by dissolving 5.99 g  $\text{C}_9\text{H}_{11}\text{NO}$  (0.01 mol) in a mixture of HCl (30 mL) and ethanol (300 mL). Subsequently, 5 mL of cathodic electrolyte were extracted and combined with 5 mL of the prepared color reagent. Following 10 min's incubation at room temperature, UV-Vis absorbance spectra were acquired, and the absorbance at 455 nm was recorded. The UV-Vis spectra of standard  $\text{N}_2\text{H}_4$ -N solutions with known concentrations were tested for calibration, resulting in the calibration equation:  $y = 0.773x + 0.026$  with an  $R^2$  value of 0.997.

### Performance evaluation

To calculate  $\text{NO}_3^-$  conversion ( $C_{\text{NO}_3^-}$ ), Eq. (2) is used as follows:

$$C_{\text{NO}_3^-} = \frac{\Delta c_{\text{NO}_3^--\text{N}}}{C_0} \times 100\% \quad (2)$$

where  $c_0$  represents the initial concentration of  $\text{NO}_3^-$ -N in electrolyte,  $\Delta c_{\text{NO}_3^--\text{N}}$  stands for the variation in the concentration of  $\text{NO}_3^-$ -N before and after electrolysis.

To calculate  $\text{NH}_3$  selectivity ( $S_{\text{NH}_3}$ ), Eq. (3) is used as follows:

$$S_{\text{NH}_3} = \frac{c_{\text{NH}_3-\text{N}}}{\Delta c_{\text{NO}_3^--\text{N}}} \times 100\% \quad (3)$$

where  $\Delta c_{\text{NO}_3^--\text{N}}$  is the variation in the concentration of  $\text{NO}_3^-$ -N before and after electrolysis,  $c_{\text{NH}_3-\text{N}}$  stands for the concentration of  $\text{NH}_3$  - N after electrolysis.

To calculate  $\text{NH}_3$  yield rate ( $Y_{\text{NH}_3}$ ), Eq. (4) is employed as below:

$$Y_{\text{NH}_3} = \frac{c_{\text{NH}_3} \times V}{t \times S} \quad (4)$$



where  $c_{\text{NH}_3}$  stands for the concentration of  $\text{NH}_3$  after electrolysis,  $V$  is the cathodic electrolyte volume,  $t$  represents the reduction time,  $S$  is the geometric area of the working electrode.

To calculate  $\text{NH}_3$  Faradaic efficiency ( $\text{FE}_{\text{NH}_3}$ ), Eq. (5) is used as follows:

$$\text{FE}_{\text{NH}_3} = \frac{8 \times F \times c_{\text{NH}_3} \times V}{17 \times Q} \times 100\% \quad (5)$$

where  $F$  stands for the Faradaic constant ( $96,485 \text{ C mol}^{-1}$ ),  $c_{\text{NH}_3}$  is the concentration of  $\text{NH}_3$  after electrolysis,  $V$  is the cathodic electrolyte volume, and  $Q$  is the total charge that has passed through the electrode.

To calculate  $\text{NO}_2^-$  yield rate ( $Y_{\text{NO}_2^-}$ ), Eq. (6) is employed as follows:

$$Y_{\text{NO}_2^-} = \frac{c_{\text{NO}_2^-} \times V}{t \times S} \quad (6)$$

where  $c_{\text{NO}_2^-}$  stands for the concentration of  $\text{NO}_2^-$  after electrolysis,  $V$  represents the cathodic electrolyte volume,  $t$  is the reduction time in h, and  $S$  is the geometric area of the working electrode.

To calculate  $\text{NO}_2^-$  selectivity ( $S_{\text{NO}_2^-}$ ), Eq. (7) is used as follows:

$$S_{\text{NO}_2^-} = \frac{c_{\text{NO}_2^-} - N}{\Delta c_{\text{NO}_3^- - N}} \times 100\% \quad (7)$$

where  $\Delta c_{\text{NO}_3^- - N}$  is the variation in the concentration of  $\text{NO}_3^- - \text{N}$  before and after electrolysis,  $c_{\text{NO}_2^- - N}$  is the concentration of  $\text{NO}_2^- - \text{N}$  after electrolysis.

To calculate  $\text{NO}_2^-$  Faradaic efficiency ( $\text{FE}_{\text{NO}_2^-}$ ), Eq. (8) is used as follows:

$$\text{FE}_{\text{NO}_2^-} = \frac{2 \times F \times c_{\text{NO}_2^-} \times V}{46 \times Q} \times 100\% \quad (8)$$

where  $F$  stands for the Faradaic constant,  $c_{\text{NO}_2^-}$  is the concentration of  $\text{NO}_2^-$  after electrolysis,  $V$  is the cathodic electrolyte volume,  $Q$  is the total charge that has passed through the electrode.

$\text{N}_2$  selectivity ( $S_{\text{N}_2}$ ) is obtained by the subtraction method (Eq. 9), as only the N-containing products of  $\text{NO}_2^-$ ,  $\text{N}_2$ , and  $\text{NH}_3$  can be detected during the  $\text{NO}_3\text{RR}$  process.

$$S_{\text{N}_2} = \frac{\Delta c_{\text{NO}_3^- - N} - c_{\text{NO}_2^- - N} - c_{\text{NH}_3 - N}}{\Delta c_{\text{NO}_3^- - N}} \quad (9)$$

where  $\Delta c_{\text{NO}_3^- - N}$  is the variation in the concentration of  $\text{NO}_3^- - \text{N}$  before and after electrolysis,  $c_{\text{NO}_2^- - N}$  is the concentration of  $\text{NO}_2^- - \text{N}$  after electrolysis,  $c_{\text{NH}_3 - N}$  is the concentration of  $\text{NH}_3 - \text{N}$  after electrolysis.

To calculate  $\text{N}_2$  Faradaic efficiency ( $\text{FE}_{\text{N}_2}$ ), Eq. (10) is used as follows:

$$\text{FE}_{\text{N}_2} = \frac{5 \times F \times S_{\text{N}_2} \times \Delta c_{\text{NO}_3^- - N} \times V}{14 \times Q} \times 100\% \quad (10)$$

where  $F$  is the Faradaic constant ( $96,485 \text{ C mol}^{-1}$ ),  $\Delta c_{\text{NO}_3^- - N}$  is the variation in the concentration of  $\text{NO}_3^- - \text{N}$  before and after electrolysis,  $V$  is the cathodic electrolyte volume,  $Q$  is the total charge that has passed through the electrode.

$\text{H}_2$  was detected by the gas chromatograph (GC, A91 Plus PANNA) equipped with a thermal conductivity detector (TCD). The gas effluent from the cathodic chamber was directly delivered into the gas sampling loop of GC.  $\text{H}_2$  Faradaic efficiency ( $\text{FE}_{\text{H}_2}$ ) is calculated using the

following Eq. (11)<sup>36</sup>:

$$\text{FE}_{\text{H}_2} = \frac{2 \times F \times V_{\text{H}_2} \times G \times t \times P_0}{R \times T \times Q \times 10^6} \times 100\% \quad (11)$$

where  $F$  is the Faradaic constant ( $96,485 \text{ C mol}^{-1}$ ),  $V_{\text{H}_2}$  is the volume concentration of  $\text{H}_2$  in the exhausted gas from cathodic chamber at a given sampling time (vol%),  $G$  is total gas flow rate at room temperature and ambient pressure ( $20 \text{ L min}^{-1}$ ),  $t$  is the electrolysis time,  $P_0$  is the gas pressure ( $1.013 \times 10^5 \text{ Pa}$ ),  $R$  is the ideal gas constant ( $8.314 \text{ J mol}^{-1} \text{ K}^{-1}$ ),  $T$  is the temperature ( $298 \text{ K}$ ), and  $Q$  is the total charge that has passed through the electrode during the  $\text{NO}_3\text{RR}$  process.

To calculate  $\text{NH}_3$  partial current density ( $j_{\text{NH}_3}$ ), Eq. (12) is employed as follows:

$$j_{\text{NH}_3} = \frac{\text{FE}_{\text{NH}_3} \times Q}{t \times S} \quad (12)$$

where  $Q$  is the total charge that has passed through the electrode,  $t$  is the reduction time, and  $S$  stands for the geometric area of the working electrode.

The half-cell energy efficiency ( $\text{EE}_{\text{NH}_3}$ ) determined by the ratio of fuel energy to the electrical power applied, is calculated using Eq. (13) as follows:

$$\text{EE}_{\text{NH}_3} = \frac{(1.23 - E_{\text{NH}_3}^0) \times \text{FE}_{\text{NH}_3}}{1.23 - E} \quad (13)$$

where  $E_{\text{NH}_3}^0$  is the equilibrium potential of the  $\text{NO}_3\text{RR}$  process ( $0.69 \text{ V}$ ),  $E$  stands for the applied potential.

To calculate energy consumption (EC), Eq. 14 is employed as follows:

$$\text{EC} = \frac{(1.23 - E) \times i \times t}{m} \quad (14)$$

where  $E$  stands for the applied potential,  $i$  represents the current,  $t$  is the reduction time,  $m$  is the mass of produced  $\text{NH}_3$  after electrolysis.

To calculate  $\text{NH}_3$  production cost, Eq. (15) is employed as below:

$$\text{NH}_3 \text{ production cost} = 0.03 \times \text{EC} \quad (15)$$

where EC stands for the energy consumption,  $0.03 (\text{\$}_{\text{USD}} \text{ kWh}^{-1})$  is the full levelized cost of electricity (LCOE) for utility solar power according to the recent announcement by the US Department of Energy (DOE) for the 2030 target<sup>23,37</sup>. Note that this is a simplified calculation method that solely considers the electrical price without taking into account the capital costs and Ohmic losses.

Calculation of ECSA and ECSA-normalized  $Y_{\text{NH}_3}$

To calculate ECSA, Eq. (16) is used as follows:

$$\text{ECSA} = \frac{C_{\text{dl}}}{C_s} \quad (16)$$

where  $C_s$  refers to the specific capacitance of a flat metallic surface<sup>38</sup>, with a value of  $40 \mu\text{F cm}^{-2}$ .  $C_{\text{dl}}$  is the double-layer capacitance, which can be derived from cyclic voltammetry (CV) performed within the non-Faradaic potential range at different scan rates ( $10\text{--}60 \text{ mV s}^{-1}$ ). The calculation of  $C_{\text{dl}}$  is based on Eq. (17) as follows:

$$C_{\text{dl}} = \frac{\Delta i}{2 \times v} = \frac{i_a - i_c}{2 \times v} \quad (17)$$

where  $i_a$  and  $i_c$  represent the anodic and cathodic current at a certain potential, respectively,  $v$  is the scan rate of CV.

ECSA-normalized  $Y_{\text{NH}_3}$  is calculated using Eq. (18) as follows:

$$\text{ECSA} - \text{normalized } Y_{\text{NH}_3} = \frac{c_{\text{NH}_3} \times V}{t \times \text{ECSA}} \quad (18)$$

where  $V$  stands for the cathodic electrolyte volume,  $t$  is the reduction time,  $c_{\text{NH}_3}$  is the concentration of  $\text{NH}_3$  after electrolysis.

Calculation of BET surface area-normalized  $Y_{\text{NH}_3}$   
 $Y_{\text{NH}_3}$  is normalized to BET surface area according to the following Eq. (19):

$$\text{BET surface area} - \text{normalized } Y_{\text{NH}_3} = \frac{c_{\text{NH}_3} \times V}{t \times \text{BET surface area}} \quad (19)$$

where  $V$  stands for the cathodic electrolyte volume,  $t$  represents the reduction time,  $c_{\text{NH}_3}$  is the concentration of  $\text{NH}_3$  after electrolysis. BET surface area is obtained by  $\text{N}_2$  adsorption-desorption method.

### In situ Raman measurement

Gamry Reference 3000 coupled with an iRaman instrument equipped with a 532 nm laser was employed for in situ Raman measurement. A self-made cell featuring a three-electrode configuration was employed. The electrolyte contained 0.5 M  $\text{Na}_2\text{SO}_4$ , 0.1 M NaOH, and 200 ppm  $\text{NO}_3^-$ -N. All Raman spectra were acquired during chronoamperometric experiments.

### In situ ATR-SEIRAS measurement

For in situ ATR-SEIRAS measurements, hcp-Ru<sub>1</sub>Co was supported on an Au-coated Si crystal substrate as the working electrode, Ag/AgCl and Pt foil functioned as the reference and counter electrodes, respectively. During chronoamperometry experiments at various potentials, spectral data were collected. The electrolyte contained 0.5 M  $\text{Na}_2\text{SO}_4$ , 0.1 M NaOH, and 200 ppm  $\text{NO}_3^-$ -N.

### Online DEMS measurement

For online DEMS measurements, a peristaltic pump was utilized to continuously flow the electrolyte (0.5 M  $\text{Na}_2\text{SO}_4$ , 0.1 M NaOH, and 200 ppm  $\text{NO}_3^-$ -N) into a custom-made electrochemical cell, in which hcp-Ru<sub>1</sub>Co loaded on glassy carbon electrode served as the working electrode, while Pt wire and Ag/AgCl were used as the counter and the reference electrodes, respectively. Ar gas was bubbled into the electrolyte constantly before and during the DEMS measurement. The gaseous products generated from the working electrode were brought into a mass spectrometer through a hydrophobic polytetrafluoroethylene (PTFE) membrane (porosity  $\geq 50\%$ , pore diameter  $\leq 20$  nm). Chronoamperometry test at 0 V was carried out for 150 s. Once the test was completed and mass signals recovered to their initial levels, the subsequent cycle was initiated under identical conditions. Following four cycles, the measurement was finished.

### Isotope labeling experiments

Isotopic labeling experiments utilized  $\text{Na}^{15}\text{NO}_3$  (98.5 wt%) as the nitrogen source. The post-electrolysis electrolyte was extracted and adjusted to pH 4 using  $\text{H}_2\text{SO}_4$ . For  $^1\text{H}$  NMR test, 1 mL of  $\text{D}_2\text{O}$  with 4.4 mg of  $\text{C}_4\text{H}_4\text{O}_4$  was incorporated into 10 mL of the above solution. The  $^1\text{H}$  NMR spectra of standard  $^{15}\text{NH}_4^+$  solution with known concentrations were measured for calibration, resulting in the calibration equation:  $y = 0.016x - 0.034$  with an  $R^2$  value of 0.997.

### $\text{NO}_3^-$ adsorption and FT-IR experiments

To ascertain the adsorption capacities of  $\text{NO}_3^-$ , Ru<sub>1</sub>Co SAAs (10 mg) were immersed in 10 mL of an electrolyte comprising 0.5 M  $\text{Na}_2\text{SO}_4$ , 0.1 M NaOH, and 200 ppm  $\text{NO}_3^-$ -N. After stirring for 30 min, the

adsorption capacity ( $q_e$ ) is determined using Eq. (20) as follows:

$$q_e = \frac{\Delta c_{\text{NO}_3^- - \text{N}} \times V}{14 \times m} \quad (20)$$

where  $q_e$  stands for the adsorption capacity,  $\Delta c_{\text{NO}_3^- - \text{N}}$  is the variation in the concentration of  $\text{NO}_3^-$ -N before and after stirring,  $V$  is the electrolyte volume,  $m$  is the mass loading amount of Ru<sub>1</sub>Co SAAs.

The Ru<sub>1</sub>Co SAAs with absorbed  $\text{NO}_3^-$  underwent sequential washing with deionized water, centrifugation, and drying. Finally, they were analyzed using FT-IR spectroscopy.

### Computational details

Density functional theory (DFT) calculations were carried out using the Vienna ab-initio Simulation Package software<sup>39,40</sup>. The generalized gradient approximation (GGA) with the Perdew–Burke–Ernzerhof (PBE) exchange-correlation function was used, and projector augmented wave (PAW) pseudo-potentials were used to model ion-electron interactions<sup>41–43</sup>. A plane-wave cutoff energy basis set with a cutoff energy of 450 eV was applied. To account for van der Waals forces, the DFT-D3 method was employed<sup>44,45</sup>. Structural relaxations utilized a Monkhoest–Pack  $k$ -point grid of  $2 \times 2 \times 1$ , with convergence thresholds set to an energy tolerance of  $10^{-5}$  eV and force below  $0.05 \text{ eV } \text{\AA}^{-1}$ . A  $15 \text{ \AA}$  vacuum region was introduced along the  $z$ -axis. The free energy change ( $\Delta G$ ) of the reaction pathway was determined using Eq. 21 as follows:

$$\Delta G = \Delta E + \Delta \text{ZPE} - T\Delta S \quad (21)$$

where  $\Delta E$ ,  $\Delta \text{ZPE}$ , and  $\Delta S$  are the variations in the reaction energy, zero-point energy change, and entropy change, respectively,  $T$  stands for the temperature.

### Rechargeable Zn- $\text{NO}_3^-$ battery measurements

For the rechargeable Zn- $\text{NO}_3^-$  battery tests, an H-cell setup with a Nafion 211 membrane as the separator was used. The anode compartment contained 2 M KOH as the electrolyte, while the cathode compartment utilized a solution of 0.5 M  $\text{Na}_2\text{SO}_4$ , 0.1 M NaOH, and 200 ppm  $\text{NO}_3^-$ -N. A polished Zn plate with a geometric area of  $0.5 \text{ cm}^2$  served as the anode, and the cathode employed NF anchored with hcp-Ru<sub>1</sub>Co.

### Reporting summary

Further information on research design is available in the Nature Portfolio Reporting Summary linked to this article.

### Data availability

The data supporting the findings of this study are available within the article and its Supplementary Information files. Source data are provided with this paper.

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## Author contributions

A.-L.W. and Q.L. proposed the overall research direction and guided the project. A.-L.W., Q.L., and X.Z. conceived and designed the experiments, synthesized the materials, performed the electrochemical measurements, and drafted the manuscript. Y.-C.W. conducted the aberration-corrected HAADF-STEM characterizations. K.Q. and S.Y. carried out the theoretical calculations. L.S., J.W., Y.G., X.L., and C.-F.L. provided valuable discussions and suggestions. All authors discussed and commented on the manuscript.

## Competing interests

The authors declare no competing interests.

## Additional information

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