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Received: 15 September 2025

Accepted: 23 February 2026

Cite this article as: Lou, Y., Han, Y., Li, T. *et al.* Metal-organic framework-confined  $\text{Co}_3\text{O}_4$  for humidity-immune ozone decomposition. *Nat Commun* (2026). <https://doi.org/10.1038/s41467-026-70324-3>

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# Metal-organic framework-confined $\text{Co}_3\text{O}_4$ for humidity-immune ozone decomposition

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## Abstract

Ground-level ozone ( $O_3$ ) is a major air pollutant, and catalytic decomposition represents a promising strategy for its removal. However, maintaining high catalytic efficiency under humid conditions remains a considerable challenge. In this study, we encapsulate ultrafine metal oxides (UMOs; e.g.,  $Co_3O_4$ , NiO) within the nanopores of an  $Fe_3O$ -cluster-based metal–organic framework, PCN-333(Fe), for catalytic  $O_3$  decomposition. The optimized 30%  $Co_3O_4@PCN-333(Fe)$  catalyst achieves sustained 100%  $O_3$  conversion for over 120 hours in a continuous airflow containing 40 ppm  $O_3$  under high space velocity ( $1.75 \times 10^5 \text{ h}^{-1}$ ) and a broad range of humidity (10-90% RH). Mechanistic investigations reveal that the exceptional performance originates from an interfacial hydrogen-atom transfer process between  $Co_3O_4$  and the  $Fe_3O$  clusters of PCN-333(Fe), as confirmed by in situ diffuse reflectance infrared Fourier-transform spectroscopy (DRIFTS) and in situ Raman spectroscopy. This work proposes a general principle for designing humidity-immune catalytic interfaces between metal oxides and porous materials, thereby providing a practical foundation for sustainable control of pollutant emissions in complex environments.

## Introduction

Ground-level ozone ( $O_3$ ) has emerged as a major global air pollutant, posing serious threats to both environmental quality and public health<sup>1, 2</sup>. Outdoor  $O_3$  is primarily generated through photochemical reactions between nitrogen oxides and volatile organic compounds under sunlight, while indoor  $O_3$  may accumulate from emissions produced by photocopiers, laser printers, ultraviolet lamps, and disinfection devices<sup>3, 4</sup>. As a potent oxidant,  $O_3$  remains relatively stable at typical ambient concentrations (ppb level)<sup>5</sup>; however, long-term exposure has been associated with respiratory disorders, cardiovascular diseases, and even premature mortality<sup>6, 7</sup>. The World Health Organization has recommended that the 8-h average  $O_3$  concentration exceeding  $100 \mu\text{g m}^{-3}$  ( $\approx 51$  ppb) poses health risks<sup>8</sup>. Alarmingly,  $O_3$  levels exceeding 150 ppb are frequently reported in many regions, reflecting severe pollution episodes. These observations underscore the urgent need for efficient, durable, and environmentally sustainable strategies for  $O_3$  removal.

Among various control measures, catalytic decomposition is regarded as the most promising strategy owing to its high efficiency and absence of harmful by-products<sup>9, 10</sup>. Conventional transition-metal oxides exhibit notable activity but suffer from rapid deactivation under humid conditions, where water molecules compete strongly for active sites<sup>11-13</sup>. Dispersing ultrafine metal oxides (UMOs) on carbonaceous or porous substrates can partially alleviate these issues<sup>14</sup>, yet such systems still face challenges of weak host–guest interfacial coupling, limited control over particle size, and heterogeneous distributions of active sites. In contrast, metal-organic frameworks (MOFs)

offer distinct advantages, including tunable organic linkers to balance hydrophilicity/hydrophobicity, robust inorganic nodes to act as active sites, and hierarchical porosity to facilitate mass transport<sup>15-19</sup>. Nevertheless, most reported UMO-MOF composites rely on external loading, which often leads to non-uniform particle distributions, pore blockage, and reduced accessibility of active sites<sup>20-22</sup>. Therefore, designing UMO-MOF catalysts with well-defined structures, strong interfacial interactions, and high stability is of paramount importance, offering new opportunities to overcome current limitations and realize highly efficient O<sub>3</sub> catalytic decomposition.

Herein, we report a series of UMOs@PCN-333(Fe) composites (UMOs = ultrafine Co<sub>3</sub>O<sub>4</sub> or NiO nanoparticles), in which the oxide nanoparticles are precisely encapsulated inside the nanopores of PCN-333(Fe) rather than simply deposited on the external surface. Among them, 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) achieves 100% O<sub>3</sub> conversion across a wide humidity (10-90% RH) at room temperature, and maintains long-term stability for over 120 h. DFT calculations combined with in situ spectroscopy reveal that the exceptional catalytic performance originates from interfacial hydrogen-atom transfer between Co<sub>3</sub>O<sub>4</sub> and Fe<sub>3</sub>O clusters of PCN-333(Fe), which facilitates stepwise O<sub>3</sub> activation, improves O<sub>2</sub> release efficiency, and accelerates active-site regeneration. Furthermore, the remarkable humidity immunity arises from the MOF-confined protection of active sites from water invasion, while water molecules actively participate in the reaction pathway rather than competing with O<sub>3</sub>. This work establishes a fundamental principle for engineering interfacial hydrogen-atom transfer within MOF-confined oxide catalysts, thereby providing a

practical foundation for achieving sustainable pollutant control under complex and variable environmental conditions.

## Results

### Syntheses and Structural Characterization of UMOs@PCN-333(Fe)

The synthetic route of UMOs@PCN-333(Fe) is depicted in Fig. 1. A sonication-microwave confinement strategy was developed to achieve the precise incorporation of ultrafine metal oxide nanoparticles within the nanopores of PCN-333(Fe). Initially, activated PCN-333(Fe) was dispersed homogeneously in a hydrophobic solvent (e.g. *n*-hexane) by ultrasonication, preventing aggregation and exposing the hierarchical pore system. Subsequently, controlled amounts of UMOs precursors were introduced under 0°C, enabling their gradual penetration into the nanopores of framework. After an aging process that facilitated precursor anchoring, the mixture was carefully filtered and underwent microwave treatment, which induced rapid in situ nucleation and growth of UMOs as highly dispersed clusters confined within the pores of PCN-333(Fe). This step ensured both uniform nanoparticle distribution and preservation of the host crystallinity. Finally, careful purification removed residual reactants without damaging the porous architecture. This synthetic strategy thus provides a versatile platform for embedding nanoscale metal oxides into MOFs, achieving strong interfacial coupling and well-defined hybrid architectures for catalytic applications.

To elucidate the structural characteristics of UMOs@PCN-333(Fe), we selected 30%

$\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  as a representative material. The MTN-type zeolitic topology of PCN-333 (Fig. 1) consists of a dual-mesopore network formed by supertetrahedral building units, with two types of mesocages (4.2 and 5.5 nm in diameter) interconnected by pore windows of  $\sim 2.6$  and 3.0 nm, thereby providing spatially well-defined compartments for nanoparticle encapsulation<sup>23, 24</sup>. Aberration-corrected high-angle annular dark-field scanning transmission electron microscopy (AC-HAADF-STEM) was employed to probe the structural integrity and encapsulation behavior<sup>25</sup>. The pristine PCN-333(Fe) framework displays periodically arranged mesopores on the (110) plane (Fig. 2a). Upon encapsulation, the 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  sample preserves the parent pore periodicity (Fig. 2b), yet exhibits locally elevated contrast, directly evidencing pore occupation by  $\text{Co}_3\text{O}_4$  nanoparticles (Fig. 2c). EDS elemental mapping further confirms homogeneous Co distribution across single MOF crystals (Fig. S1). The encapsulated  $\text{Co}_3\text{O}_4$  nanoparticles exhibit a uniform size of 3.4-3.9 nm (average  $3.6 \pm 0.1$  nm, Fig. S2), which matches the mesoporous cavity dimensions of PCN-333. Scanning Electron Microscope reveals well-retained octahedral morphology with smooth surfaces and absence of surface-deposited aggregates (Fig. S3), corroborating true intracrystalline encapsulation. These observations unambiguously confirm that  $\text{Co}_3\text{O}_4$  nanoparticles are formed in situ and precisely confined within the nanopores of PCN-333(Fe), without compromising the structural integrity of its framework.

To probe the chemical state of Co element in 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$ , Co K-edge X-ray absorption near-edge structure (XANES) and extended X-ray absorption fine structure (EXAFS) spectroscopy were performed, revealing an absorption edge between Co foil and bulk  $\text{Co}_3\text{O}_4$ ,

closer to  $\text{Co}_3\text{O}_4$ , indicating a slightly reduced oxidation state due to nanoconfinement-induced interface effects (Fig. 3a)<sup>26</sup>. Fourier-transformed EXAFS (FT-EXAFS, Fig. 3b) reveals a prominent Co-O coordination at  $\sim 1.42$  Å, marginally shorter than the 1.46 Å path in bulk  $\text{Co}_3\text{O}_4$ <sup>27</sup>,<sup>28</sup>, while subsequent Co-Co coordination shells are markedly attenuated, directly evidencing the highly dispersed and size-confined nature of the encapsulated clusters. Quantitative EXAFS fitting using crystallographic  $\text{Co}_3\text{O}_4$  parameters yields excellent agreement (Fig. 3c), unequivocally confirming  $\text{Co}_3\text{O}_4$  as the dominant crystalline phase while exhibiting subtle oxidation state reduction associated with elevated oxygen vacancy concentrations.

Powder XRD patterns, photograph, and FT-IR spectra (Fig. 3d and Figs. S4-S5) confirm the preservation of PCN-333(Fe)'s crystalline integrity following  $\text{Co}_3\text{O}_4$  incorporation across various loadings. The absence of distinct  $\text{Co}_3\text{O}_4$  diffraction peaks precludes large particle formation, instead indicating highly dispersed, ultra-small  $\text{Co}_3\text{O}_4$  nanoclusters<sup>29, 30</sup>. Raman spectroscopy identifies the characteristic  $\text{Co}_3\text{O}_4$  peak at  $682\text{ cm}^{-1}$  (Fig. 3e), confirming the encapsulated phase's identity as  $\text{Co}_3\text{O}_4$ <sup>31, 32</sup>.  $\text{N}_2$  adsorption isotherms (Fig. 3f) and pore size analysis (Fig. S6) reveal a systematic decrease in uptake capacity with increasing  $\text{Co}_3\text{O}_4$  loading, consistent with progressive pore filling. Notably, unlike previous reports where metal oxides (e.g.,  $\text{TiO}_2$ ) were confined solely to mesopores,  $\text{Co}_3\text{O}_4$  in this work also occupies micropores ( $\sim 11$  Å diameter), attributable to the smaller size of its precursors<sup>25</sup>. Inductively coupled plasma optical emission spectrometry (ICP-OES) quantitatively verifies  $\text{Co}_3\text{O}_4$  mass percentages of 9.4%, 18.6%, and 27.3% (Table S1), aligning with the designated loadings. Similarly, structure characterization of NiO (Figs. S7-S10)

confirms its successful encapsulation within the PCN-333(Fe) framework.

### **O<sub>3</sub> catalytic decomposition on UMOs@PCN-333(Fe)**

The O<sub>3</sub> catalytic decomposition performance of UMOs@PCN-333(Fe) was evaluated with a dynamic test at various humidity and temperature on a custom-built ozone analyzer at an inlet O<sub>3</sub> concentration of 40 ppm (Fig. S11). The effect of varying oxide loadings on catalyst under low (10% RH) and high humidity (90% RH) conditions was first optimized (Figs. S12-S13). Remarkably, 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) maintains complete O<sub>3</sub> conversion for more than 160 h at 40°C even under 10% RH (Fig. 4a), attesting to its outstanding durability in dry environments, with a performance level comparable to the best catalysts reported to date<sup>13, 33-36</sup>. In addition, the catalytic rate of O<sub>3</sub> decomposition over 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) was calculated to be 1.9 mmol·h<sup>-1</sup>·g<sub>cat.</sub><sup>-1</sup>. While performance exhibits humidity dependence, degrading to 120 hours at 90% RH, this still represents exceptional longevity under high moisture stress compared to benchmark materials. Furthermore, a pronounced positive temperature dependence of catalytic stability at fixed low humidity (10% RH): 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) sustains 100% O<sub>3</sub> conversion for 50 hours even at a low temperature of 10°C, underscoring its exceptional intrinsic activity and robustness in O<sub>3</sub> catalytic decomposition (Fig. 4b). Under 10% RH (Fig. 4c), the O<sub>3</sub> conversion of bulk Co<sub>3</sub>O<sub>4</sub> and pristine PCN-333(Fe) rapidly deactivate, reaching peak conversions of <10% and <30% within 3 h, far below the sustained 100% activity of the composite. Even at 90% RH, 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) preserves its pronounced advantage, underscoring its superior humidity

immunity (Fig. 4d). These results highlight the synergistic catalysis arising from the MOF-encapsulated UMOs structure.

The robustness of 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  to dynamic environmental fluctuations is shown in Figs 4e-f. When subjected to fluctuating humidity cycles between 30% and 90% RH, or temperature shifts between 10°C and 40°C, the material consistently maintains 100%  $\text{O}_3$  conversion for 50+ hours without performance decay. This robust adaptability underscores its capability to handle real-world atmospheric variability where humidity and temperature rarely remain static. Optimization of the active phase loading is critical for maximizing humidity immunity. Fig. 4g demonstrates that  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  with 10% loading sustains 100% conversion for only 20 hours at 90% RH, whereas increasing the loading to 30% extends this duration to more than 160 hours. This pronounced  $\text{Co}_3\text{O}_4$  loading dependence unequivocally demonstrates that achieving an optimal  $\text{Co}_3\text{O}_4$  density within the PCN-333(Fe) framework is indispensable for preserving abundant and accessible catalytic sites, particularly under wet environments.

Critically, 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  exhibits industry-relevant performance even under simulated extreme environments, underscoring its substantial potential for practical application. Challenging summertime conditions representative of the Yangtze River Delta region in China, where intense photochemical activity and high humidity converge to produce severe  $\text{O}_3$  pollution episodes, thereby underscoring the urgent necessity of effective removal strategies. Remarkably, under these accelerated degradation conditions, 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  sustains complete  $\text{O}_3$

decomposition for 120 hours (Fig. 4h). This superior stability highlights not only the high intrinsic activity of the encapsulated architecture but also its resilience against the simultaneous thermal and humidity stresses that typically deactivate conventional catalysts. Beyond the single  $\text{Co}_3\text{O}_4$  system, the encapsulation strategy proves broadly generalizable for enhancing the catalytic efficiency of diverse transition metal oxides. As demonstrated in Fig. 4i, PCN-333(Fe) incorporating NiO, or  $\text{Co}_3\text{O}_4$  nanoclusters achieves over 120 hours of continuous and complete  $\text{O}_3$  conversion under optimized conditions, markedly outperforming state-of-the-art benchmarks (Table S2). Furthermore, systematic evaluations of NiO@PCN-333(Fe) a (Figs. S14-S16) confirm its outstanding decomposition activity across a wide range of environmental conditions. Although all encapsulated composites deliver transformative stability enhancements relative to their bulk oxide counterparts, 30%  $\text{Co}_3\text{O}_4$ @PCN-333(Fe) consistently demonstrates the highest activity-to-stability balance, firmly establishing it as a leading candidate for scalable and durable industrial  $\text{O}_3$  removal.

### **$\text{O}_3$ Conversion Mechanism over 30% $\text{Co}_3\text{O}_4$ @PCN-333(Fe)**

To elucidate the underlying mechanisms contributing to the excellent  $\text{O}_3$  catalytic decomposition performance of 30%  $\text{Co}_3\text{O}_4$ @PCN-333(Fe), X-ray photoelectron spectroscopy (XPS), in situ diffuse reflectance infrared Fourier transform spectroscopy and in situ Raman spectroscopy was performed. The chemical states of both Fe and Co underwent significant changes after the encapsulation of  $\text{Co}_3\text{O}_4$  particles within the PCN-333(Fe) cages (Fig. 5a-b). Upon  $\text{Co}_3\text{O}_4$

encapsulation, the  $\text{Fe}^{2+}$  content on PCN-333(Fe) increases from 45.1% to 61.9%, while the  $\text{Co}^{2+}$  content of  $\text{Co}_3\text{O}_4$  rises from 45.7% to 63.4%. Such concurrent enrichment of reduced Fe and Co species underscores the emergence of an interfacial MOF-UMOs synergistic site, which is directly promoted by the confined architecture. During  $\text{O}_3$  decomposition, oxygen vacancies are generated to maintain electrostatic balance, and substantial evidence suggests that these vacancies act as the dominant active sites, accounting for the high catalytic efficiency<sup>12, 37, 38</sup>. This conclusion is corroborated by differential charge density calculation (Fig. S17), which reveals pronounced charge transfer from MOF ligands to Fe and Co centers.

Electron Paramagnetic Resonance (EPR) analysis reveals that  $\text{O}_3$  exposure induces  $\text{O}_2^{\cdot-}$  species in 30%  $\text{Co}_3\text{O}_4@\text{PCN-333(Fe)}$  when trapped by DMPO (Fig. S18). The in situ DRIFT spectrum (Fig. 5c) exhibited prominent absorption bands at approximately 3660, 2125, 1650, and 1380  $\text{cm}^{-1}$ . These bands are assigned to the O-H stretching vibration of doubly bridged hydroxyl groups (-OHO-)<sup>39</sup>, coordinated  $\text{O}_3$  complexes adsorbed on Co sites<sup>40</sup>, the O-H bending vibrations in adsorbed water and reaction intermediates<sup>41</sup>, and peroxide ( $\text{O}_2^{2-}$ ) species<sup>11</sup>, respectively. Meanwhile, new peaks were observed in the in situ Raman spectra (Fig. 5d), with the band at 526  $\text{cm}^{-1}$  assigned to the O-O stretching vibration in  $\text{Co-OOH}$ <sup>42-44</sup>, and the bands at 804 and 1097  $\text{cm}^{-1}$  attributed to  $\text{O}_2^{2-}$  and  $\text{O}_2^{\cdot-}$  species<sup>34</sup>, respectively, indicating the formation of new intermediates on the catalyst surface during  $\text{O}_3$  decomposition. This finding is consistent with the literature reports, suggesting that the peroxide intermediate is active for  $\text{O}_3$  catalytic decomposition. Following a 24-hour exposure to an  $\text{O}_3$  gas flow, the Raman spectrum of 30%  $\text{Co}_3\text{O}_4@\text{PCN-}$

333(Fe) showed no significant changes, which suggests that the structural integrity of the catalyst remained intact and undamaged throughout this duration. This observation serves to confirm the exceptional stability of the material. Furthermore, the accumulation of intermediate products was found to be minimal, and it is noteworthy that the release of these intermediates at the active sites constitutes the rate-limiting step in the  $O_3$  catalytic decomposition process, thereby providing further evidence of the catalyst's outstanding performance.

Density functional theory (DFT) calculations were performed to elucidate the mechanism of  $O_3$  decomposition over  $Co_3O_4@PCN-333(Fe)$  (Fig. 6). The model incorporates representative  $Fe_3O$  clusters from PCN-333(Fe) and  $Co_3O_4$  nanoclusters to simulate the catalytic interface (Fig. S19). The adsorption sites of  $H_2O$  and  $O_3$  in  $Co_3O_4@PCN-333(Fe)$  were calculated.  $H_2O$  was found to preferentially occupy an open Fe site adjacent to the  $Co_3O_4$ , with a distance of 2.223 Å, whereas  $O_3$  was located at a Co site in the vicinity of the  $Fe_3O$  cluster, with a distance of 1.825 Å, highlighting the distinct roles of Fe and Co nodes in activating the two adsorbates. Subsequently, the first  $O_3$  molecule preferentially adsorbs onto two adjacent open Co sites, with its two terminal O atoms coordinated to them. Then, the coordinated  $H_2O$  at the Fe site dissociates, releasing two free hydrogen atoms. One hydrogen atom reacts with the adsorbed  $O_3$  to generate a Co-OOOH intermediate, while the other is coordinated at the interfacial O atom. The Co-OOOH species then decomposes, releasing the first  $\cdot OOOH$  radical. The second  $O_3$  molecule subsequently adsorbs onto the Co sites, during which the interfacial hydrogen-atom transfer toward the Co center and reacts with the newly adsorbed  $O_3$  to form a second Co-OOOH intermediate. The decomposition of this Co-OOOH intermediate releases the second  $\cdot OOOH$  radical, which subsequently re-adsorbs onto Co centers to evolve the first  $O_2$  molecule, while leaving bridging O atoms shared by neighboring Co sites. In view of the complexity of this step and its pivotal role in the overall catalytic cycle, its kinetics were explicitly evaluated. The elementary step in which the  $\cdot OOOH$

intermediate forms the first O<sub>2</sub> molecule and \*OH (TS1), as well as the subsequent transfer of the resulting \*OH (TS2), was calculated. According to the DFT results, the Gibbs free energy barrier (TS1) for the formation of \*O<sub>2</sub> and \*OH intermediates from \*OOOH is 0.47 eV, and the barrier for the transfer of the generated \*OH to the O atom of Fe-O-Co (TS2) is 0.64 eV. These DFT-calculated energy barriers are moderate, indicating that the reaction process is kinetically feasible. Finally, the transient Co-OOH intermediate decomposes to release the third O<sub>2</sub> molecule, after which both hydrogen atoms return to the Fe site to reconstitute the coordinated water. Overall, the key driving force of the O<sub>3</sub> catalytic decomposition process on Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) is hydrogen-atom transfer mechanism (Tables S3-S4 and Fig. S20), in which hydrogen atoms was transferred among the Fe<sub>3</sub>O cluster, the interfacial oxygen and the Co sites, ensuring continuous regeneration of active centers. In addition, the O<sub>2</sub> desorption barrier on bare Co<sub>3</sub>O<sub>4</sub> was also calculated and found to be 1.84 eV (Fig. S21), which is much higher than the corresponding value of 0.62 eV on Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe), underscoring the advantage of the hydrogen-atom transfer nanoreactor. The above results indicated that the hydrogen-atom transfer between the interface between Co<sub>3</sub>O<sub>4</sub> and Fe<sub>3</sub>O cluster enable stepwise O<sub>3</sub> activation, efficient O<sub>2</sub> release, and accelerated active-site regeneration, thereby accounting for the high catalytic activity observed experimentally.

## Discussion

In conclusion, we have successfully constructed a hydrogen-atom transfer nanoreactor by encapsulating ultrafine metal oxides (UMOs) within the nanopores of an Fe-based metal-organic framework, PCN-333(Fe). Among the encapsulated architectures, 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) maintains high and stable O<sub>3</sub> decomposition activity across a broad range of humidity levels, demonstrating its strong potential for practical applications in real-world environments. The outstanding O<sub>3</sub> decomposition performance is attributed to a hydrogen-atom transfer mechanism

between the  $\text{Co}_3\text{O}_4$  and  $\text{Fe}_3\text{O}_4$  of PCN-333 interfaces, which facilitates stepwise activation of  $\text{O}_3$ , promotes efficient  $\text{O}_2$  release, and accelerates the regeneration of active sites. These findings underscore the significant potential of MOF-confined metal oxide materials in pollution control and may open new avenues for the development of advanced catalysts for  $\text{O}_3$  decomposition.

## Methods

### Materials and reagents

$\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ ,  $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ ,  $\text{MnSO}_4$ ,  $(\text{NH}_4)_2\text{S}_2\text{O}_8$ ,  $\text{CO}(\text{NH}_2)_2$ ,  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$ , and 2,4,6-Tris(carboxyphenyl)-1,3,5-triazine ( $\text{H}_3\text{TATB}$ ) were purchased from Shanghai Macklin Biochemical Technology Co., Ltd. DMF, EtOH, Acetone was purchased from Shenyang Xinhua Reagent Factory without further purification.

The ozone ( $\text{O}_3$ ) catalyst performance test system is self-made, and its main accessories are as follows: UV lamp and ballast were bought from Beijing Aerospace Hongda Optoelectronic Technology Co., Ltd. Ozone monitor (Model 202) was bought from 2B Technologies. Humidity generator was bought from Shanghai Penghe electronic technology Co., Ltd. Air pump (SPB-3) was bought from Beijing BHP Analytical Technology Institute. Gas mass flowmeter (PIPG-M102-01-2000) was bought from Shaanxi Yidu Intelligence Technology Co., Ltd.

### Synthesis of PCN-333(Fe)

PCN-333(Fe) was synthesized according to the previously reported literature<sup>24</sup>.  $\text{H}_3\text{TATB}$  (50 mg) and anhydrous  $\text{FeCl}_3$  (60 mg) were dissolved in 10 mL of DMF, followed by the addition of 0.5

mL trifluoroacetic acid. The resulting solution was transferred to a Teflon-lined autoclave and heated at 150 °C for 12 h, yielding a brown precipitate. After centrifugation, the product was repeatedly washed with fresh DMF and Acetone to remove any residual reactants.

### **Synthesis of UMOs@PCN-333(Fe)**

Co<sub>3</sub>O<sub>4</sub> precursor solution: dissolve 600 mg cobalt(II) nitrate hexahydrate (Co(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O) and 600 mg urea (CO(NH<sub>2</sub>)<sub>2</sub>) in 1 mL deionized water, then sonicate until completely dissolved.

NiO precursor solution: dissolve 600 mg nickel(II) nitrate hexahydrate (Ni(NO<sub>3</sub>)<sub>2</sub>·6H<sub>2</sub>O) and 600 mg urea (CO(NH<sub>2</sub>)<sub>2</sub>) in 1 mL deionized water, then sonicate until completely dissolved.

UMOs@PCN-333(Fe) hybrids were prepared by a sonication–microwave confinement strategy. Activated PCN-333(Fe) (50 mg) was ultrasonicated (15 min) in 20 mL anhydrous DMF to fully expose its hierarchical meso- and micro-pores. Separately, 1 mL UMOs precursor solution (Co<sub>3</sub>O<sub>4</sub> or NiO precursor solution) was added dropwise to the MOF dispersion under continuous stirring. The mixture was aged at 0°C for 2 h to allow precursor diffusion and anchoring within the cavities. Subsequent microwave irradiation induced rapid in-situ nucleation of ultrafine Co<sub>3</sub>O<sub>4</sub>, or NiO clusters without disrupting the framework. After cooling, the product was collected by filtration, washed repeatedly with DMF and ethanol, and vacuum-dried at 80°C to furnish the corresponding UMOs@PCN-333(Fe) composite.

### **Synthesis of Co<sub>3</sub>O<sub>4</sub>**

The Co<sub>3</sub>O<sub>4</sub> precursor solution was prepared by dissolving 30 mg of cobalt(II) nitrate hexahydrate

( $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ ) and 31 mg of urea ( $\text{CO}(\text{NH}_2)_2$ ) in 50  $\mu\text{L}$  of deionized water. The resulting mixture was subjected to microwave irradiation for a duration of 5 minutes to facilitate the reaction. After cooling to room temperature, the resulting powder was washed by  $\text{H}_2\text{O}$  and ethanol for 3 times, respectively. Finally, the product was dry at  $85^\circ\text{C}$  for 12 hrs.

### **Synthesis of NiO**

The NiO precursor solution was prepared by dissolving 30 mg of nickel(II) nitrate hexahydrate ( $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$ ) and 31 mg of urea ( $\text{CO}(\text{NH}_2)_2$ ) in 50  $\mu\text{L}$  of deionized water. The resulting mixture was subjected to microwave irradiation for a duration of 5 minutes to facilitate the reaction. After cooling to room temperature, the resulting powder was washed by  $\text{H}_2\text{O}$  and ethanol for 3 times, respectively. Finally, the product was dry at  $85^\circ\text{C}$  for 12 hrs.

### **Structure characterization**

The powder X-ray diffraction (PXRD) patterns were recorded on a Bruker Advanced D8 X-ray Powder Diffractometer ( $\lambda = 1.54056 \text{ \AA}$ ).  $\text{N}_2$  adsorption/desorption isotherms were measured by using a Beishide 3H-2000PS2 Surface Characterization Analyzer at 77 K. An Thermo Fisher 5700 Fourier transform infrared spectrometer was used for recording Fourier transform infrared (FT-IR) spectra. X-ray photoelectron spectroscopy (XPS) measurements were carried out using an ESCALAB 250 instrument. Metal oxides contents of all catalysts were determined by ICP-OES on an Agilent 5110(OES) atomic emission spectrometer. Raman spectra was recorded on Renishaw inVia™ InSpect Raman system. Synchrotron-based X-ray absorption spectroscopy (XAS)

measurements, including XANES and EXAFS, were carried out at the BL14W1 beamline of the Shanghai Synchrotron Radiation Facility (SSRF) operated at 3.5 GeV with a maximum current of 260 mA. Powdered samples were uniformly spread on Kapton tape and mounted in a liquid-nitrogen-cooled cryostat (80 K) to minimize radiation damage. Spectra were collected in transmission mode for the Co K-edge (7709 eV) and Fe K-edge (7112 eV), with energy calibration performed simultaneously using Co and Fe metal foils as references. Data reduction and analysis were performed with Athena and Artemis software packages following standard procedures. Aberration-corrected high-resolution transmission electron microscopy (AC-HRTEM) and high-angle annular dark-field scanning transmission electron microscopy (HAADF-STEM) were performed on a JEOL JEM-ARM300F Grand ARM double-Cs-corrected microscope operated at 300 kV (JEOL Ltd., Japan). Powder samples were ultrasonically dispersed in ethanol, drop-cast onto a holey carbon-coated copper grid, and dried under ambient conditions before imaging.

### **O<sub>3</sub> decomposition test**

The O<sub>3</sub> catalytic decomposition of UMOs@PCN-333(Fe) were evaluated through a homemade O<sub>3</sub> analysis system at room temperature. O<sub>3</sub> was generated from compressed air manufactured from a fully automatic air source (SPB-3, Beijing BCHP Analytical Technology Institute) by an ultraviolet lamp (10-08100, Beijing UVCN). Before the test, all samples were vacuum-dried at 120°C for 12 hours to remove guest molecules from the structure. Then, the mixture of the 50 mg catalysts and 450 mg of quartz sand were loaded into the quartz tube reactor. The total inlet gas flow was kept

at 1000 mL/min, and the inlet O<sub>3</sub> concentration was kept at 40 ± 1 ppm; the concentration of O<sub>3</sub> and RH were controlled by controlling the flow of blank air and O<sub>3</sub> while the total gas flow remained unchanged. The inlet and outlet O<sub>3</sub> concentration as well as RH were measured by an O<sub>3</sub> detector (model 202, 2B Technologies) and a humidity and temperature meter. The O<sub>3</sub> conversion rate was calculated via the following formula:

$$\text{O}_3 \text{ conversion (\%)} = (C_{\text{inlet}} - C_{\text{outlet}}) / C_{\text{inlet}} \times 100\% \quad (1)$$

where  $C_{\text{inlet}}$  and  $C_{\text{outlet}}$  are inlet and outlet concentrations of O<sub>3</sub>, respectively.

### Computational details

All DFT calculations were carried out using the CP2K code (V2024.1)<sup>45</sup>. The Gaussian-and-plane-wave (GPW) scheme was employed. Core electrons were described by norm-conserving Goedecker–Teter–Hutter (GTH) pseudopotentials<sup>46-48</sup>, and the valence electron wavefunctions were expanded in double- $\zeta$  Gaussian basis sets with polarization functions<sup>49</sup>, together with an auxiliary plane-wave basis set with a kinetic energy cutoff of 450 Ry. Exchange–correlation effects were treated within the generalized-gradient approximation using the Perdew-Burke-Ernzerhof (PBE) functional<sup>50</sup>. Geometry optimizations were performed with the Broyden-Fletcher-Goldfarb-Shanno (BFGS) algorithm until the self-consistent-field (SCF) energy converged to  $1.0 \times 10^{-6}$  a.u. Long-range van der Waals interactions between the adsorbates and the framework were accounted for using the DFT-D3 dispersion correction with an empirical damping function<sup>51</sup>. For Fe- and Co-containing models, the total spin multiplicities were set to 4 and 3, respectively. All calculations

were carried out in a cubic simulation cell of  $35 \times 35 \times 35 \text{ \AA}^3$ .

The Gibbs free energy change for each elementary step was calculated at 298.15 K, defining as follows:

$$\Delta G = \Delta E_{DFT} + \Delta E_{ZPE} - T\Delta S \quad (2)$$

where  $\Delta E$  is the difference of electronic energy calculated with CP2K,  $\Delta E_{ZPE}$  is the difference of zero-point energy (ZEP), and  $T\Delta S$  is the changed entropy value.  $E_{ZPE}$  and  $TS$  were calculated using the following equations for each reaction intermediates,

$$E_{ZPE} = \frac{1}{2} \sum_i h\nu_i \quad (3)$$

$$TS = \sum_i h\nu_i \left( \frac{1}{e^{h\nu_i/k_B T}} \right) - k_B T \sum_i \ln \left( 1 - e^{-h\nu_i/k_B T} \right) \quad (4)$$

where  $h$ ,  $\nu_i$ , and  $k_B$  are Planck's constant, vibrational frequencies, and Boltzmann constant, respectively. For vibrational frequency calculations, only the adsorbates were included with negligible contributions from the framework of the catalyst.

The Gibbs free energy of  $O_3$  or reaction species adsorbed on the substrates was obtained after the geometry optimization for the adsorption and reaction process. And then, the Gibbs free energy change ( $\Delta G$ ) was calculated between the free energy for each reaction step.

### Data Availability

All data supporting the findings of this study are available within the article and its Supplementary Information, or from the corresponding author upon reasonable request. Source Data are provided with the paper.

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### Acknowledgments

This work was supported by the National Natural Science Foundation of China (22171121), the Applied Basic Research Plan of Liaoning Province (2023JH2/101300007).

### Author contributions

Z.H conceived and designed this project. Y.L and T.L performed the experiments, Y.L and Y.H carried out the DFT calculation, Y.L analyzed the data, Y.L, Z.H and Z.-M.Z wrote and revised the manuscript.

### Competing interests statement

The authors declare no competing interests.

## Figure Captions

**Fig. 1. Synthetic methodology for UMOs@PCN-333(Fe) via a sonication-microwave confinement strategy.** Metal oxide precursor loading and immobilization inside PCN-333(Fe) are followed by confined conversion to ultrafine metal oxides, yielding robust hybrids.

**Fig. 2. AC-HAADF-STEM of 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) and pristine PCN-333(Fe).** (a) HAADF-STEM image of pristine PCN-333(Fe). (b) HAADF-STEM overview and (c) magnified view of 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe). Insets highlight the mesoporous arrangement of PCN-333 viewed along the (110) crystallographic plane.

**Fig. 3. Structural and textural characterization of Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) with varying Co<sub>3</sub>O<sub>4</sub> loadings.** (a) Co K-edge XANES spectra, (b) corresponding FT-EXAFS spectra, and (c) FT-EXAFS fitting curve of 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe). (d) PXRD patterns of Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) with various and Co<sub>3</sub>O<sub>4</sub> contents. (e) Raman spectra of 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe). (f) N<sub>2</sub> adsorption isotherm of Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) with various and Co<sub>3</sub>O<sub>4</sub> contents.

**Fig. 4. O<sub>3</sub> decomposition performance of various catalysts under different conditions.** (a) 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe) under 10-90% RH at 40°C. (b) Comparison among 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe), pure Co<sub>3</sub>O<sub>4</sub>, and PCN-333(Fe) under 10% RH at 40°C. (c) Comparison among 30% Co<sub>3</sub>O<sub>4</sub>@PCN-333(Fe), pure Co<sub>3</sub>O<sub>4</sub>, and PCN-333(Fe) under 90% RH at 40°C. (d) O<sub>3</sub> conversion

over  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  with different  $\text{Co}_3\text{O}_4$  loadings. **(e)** Performance of 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  under alternating humidity (30-90% RH) at 40°C. **(f)** Performance of 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  under alternating temperature (10-40°C). **(g)** Performance of 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  across 10-40 °C. **(h)**  $\text{O}_3$  conversion of 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  under simulated Yangtze River Delta region environmental conditions. **(i)** Comparison of  $\text{O}_3$  conversion among three different  $\text{UMOs}@\text{PCN-333}(\text{Fe})$  composites.

**Fig. 5. Surface chemical states and structural evolution of 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  under  $\text{O}_3$  exposure.** XPS spectra of **(a)** Co 2*p* and **(b)** Fe 2*p* of 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  and other reference materials. **(c)** in situ DRIFT spectra and **(d)** in situ Raman spectra of 30%  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$  with continuous  $\text{O}_3$  flow at room temperature.

**Fig. 6. Proposed catalytic mechanism of  $\text{O}_3$  decomposition on  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$ .** **(a)** the adsorption sites of  $\text{H}_2\text{O}$  and  $\text{O}_3$  on  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$ , **(b)** the reaction pathways and **(c)** stationary-point structures for  $\text{O}_3$  decomposition catalyzed by  $\text{Co}_3\text{O}_4@\text{PCN-333}(\text{Fe})$ . Fe atoms are light purple, Co atoms are light blue, O atoms are red, and H atoms are white.

#### Editorial summary:

Ground-level ozone is harmful, and efficient removal in humid air remains difficult. Ultrafine

cobalt oxide confined in a metal-organic framework delivers sustained complete conversion across wide humidity by enabling interfacial hydrogen transfer.

**Peer review information:** *Nature Communications* thanks Yongfa Zhu, and the other, anonymous, reviewer(s) for their contribution to the peer review of this work. A peer review file is available.

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