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## The role of promoters on NiO catalysts for methane decomposition and hydrogen production

Abdulrahman I. Alharthi<sup>1</sup>✉, Mshari A. Alotaibi<sup>1</sup>, Essam M. Abdel-Fattah<sup>2</sup>, Talal F. Qahtan<sup>2</sup> & Osama A. Alshreef<sup>2</sup>

In this study, the impact of Al, Co, and Cu as promoters for NiO to enhance its catalytic performance in methane decomposition has been investigated. The catalysts were synthesized via a co-precipitation route and comprehensively characterized using SEM, BET, XRD, XPS, Raman, TPR, and TGA techniques. Catalytic performance was evaluated in a fixed-bed reactor operated at 800 °C with a feed gas flow rate of 20 mL/min. Al<sup>3+</sup> and Cu<sup>2+</sup> incorporation into NiO reduced crystallite size and increased surface area, while Co<sup>2+</sup> had the opposite effect, indicating a distinct structural impact. Additionally, Al<sup>3+</sup> doping induced a charge imbalance in NiO, leading to an increase in Ni<sup>2+</sup> content and oxygen vacancies, as confirmed by XPS analysis. Catalytic activity tests revealed that Al<sup>3+</sup> was the most effective promoter for NiO, followed by Co<sup>2+</sup> and Cu<sup>2+</sup>, respectively. The highest CH<sub>4</sub> conversion rate and H<sub>2</sub> production rate, achieved with 10% Al-NiO at a time-on-stream (TOS) of 25 min, were 71% and  $216.2 \times 10^{-5}$  mol H<sub>2</sub> g<sup>-1</sup> min<sup>-1</sup>, respectively. The methane decomposition process exhibited stable operation with minimal CO and CO<sub>2</sub> emissions. The catalytic performance was correlated with the detailed physicochemical properties of both fresh and spent catalysts.

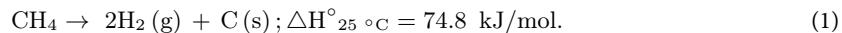
**Keywords** Al-NiO, Co-NiO, Cu-NiO, Carbon nanostructures, Hydrogen production, Methane decomposition

Presently, the world's major energy needs are met through the consumption of natural fossil fuels. The commercial use of fossil fuels creates two major issues for the modern world, (1): reducing fossil fuel reserves, and (2): increased emissions of greenhouse gases (GHG) into the environment<sup>1</sup>. To address these issues, emphasis has been placed on the use of renewable energy resources, which will be challenging, require new technological developments and investments in renewable energy, and may take decades or generations to implement<sup>2</sup>. Fuel cell technologies are considered one of the best ways to deal with current energy issues and environmental crises. Fuel cells are electrochemical equipment that convert hydrogen into electrical energy and heat<sup>3</sup>. Therefore, hydrogen energy has become one of the alternative sources that can play a role in reducing fossil fuel consumption and controlling environmental pollution. The use of fuel cell technology has led to a growing demand for hydrogen production in many industrial applications<sup>4</sup>. The technology of fuel cells is more appropriate and greener than present combustion fuels, such as gasoline and natural gas. Moreover, hydrogen can be used in many applications, such as rocket fuel, fuel for non-polluting vehicles, and clean fuel for aircraft, and water is the merely product resulting from the hydrogen combustion. The uses of hydrogen also extend beyond that, as it can be used in the petroleum industry, the production of ammonia, methanol, ethanol, dimethyl ether, and the hazardous waste hydrogenation<sup>5</sup>.

Several methods have been developed for hydrogen fuel production such as plasma assisted techniques<sup>6–8</sup>, water splitting<sup>9,10</sup>, photocatalysis<sup>11</sup>, hydrocarbon decomposition<sup>12</sup>, and steam reforming process<sup>13,14</sup>. Methane steam reforming (MSR) is presently the greatest economical pathway for hydrogen production<sup>14</sup>. Currently, about 97% of international hydrogen production is produced through MSR, accompanied by large emissions of carbon dioxide (CO<sub>2</sub>). Consequently, additional technologies are being used to capture CO<sub>2</sub>, separate and storage to produce clean hydrogen, which increases production costs. To correct defects in the MSR process, thermal catalytic decomposition of methane (CDM) is a suitable and desirable alternative path to produce clean hydrogen with small levels of harmful

<sup>1</sup>Department of Chemistry, College of Science and Humanities, Prince Sattam Bin Abdulaziz University, P.O. Box 173, 11942 Al-Kharj, Saudi Arabia. <sup>2</sup>Department of Physics, College of Science and Humanities, Prince Sattam Bin Abdulaziz University, P.O. Box 173, 11942 Al-Kharj, Saudi Arabia. ✉email: a.alharthi@psau.edu.sa

emissions and lower energy consumption. An additional advantage of this process is the production of high-quality carbon nanomaterials with unique properties as a by-product, which is valuable in the applications of nanotechnology and nanoscience<sup>15</sup>. The thermal catalytic decomposition of methane reaction occurs in one step, as shown in the following equation<sup>16</sup>:



Methane ( $\text{CH}_4$ ) is an excellent source of hydrogen because it is easily obtainable and has a high hydrogen-to-carbon ratio (H/C) compared to other hydrocarbons. However, due to the strong C-H bonds in the structure of the methane molecule, non-catalytic thermal decomposition of methane requires temperatures higher than  $1200\text{ }^\circ\text{C}$  to obtain an acceptable yield. Consequently, employing transition metal as catalysts is a suitable approach to lower the reaction temperature of methane decomposition<sup>16</sup>.

Various transition metals have been used as catalysts for the catalytic decomposition of methane. Pt, Pd, Ru, Rh, Mo, Ni, Fe and Co are examined as effective catalysts particularly when supported on inert metal oxides such as  $\text{Al}_2\text{O}_3$ ,  $\text{MgO}$ ,  $\text{TiO}_2$  and  $\text{SiO}_2$ . Fe, Co and Ni have been extensively studied due to their relative abundance and lower cost compared with noble metals. Irrespective of the noble metals, the catalytic activity of nickel (Ni) is the highest, followed by cobalt (Co), and then iron (Fe)<sup>5,15-19</sup>. From the literature, it was reported that nickel catalyst possesses high catalytic activity in CDM reaction, however, its activity is sensitive to reaction conditions and deactivates rapidly at high reaction temperature<sup>20,21</sup>. Sintering and agglomeration of nickel catalyst particles as well as their encapsulation with deposited carbon are considered as the main reasons for the deactivation of Ni-catalyst activity in CDM reactions<sup>22,23</sup>. Therefore, choosing the appropriate support for nickel catalyst, adding a second metal, and preparing the catalysts are the solutions to overcome the drawbacks of nickel-based catalysts<sup>23</sup>. It was reported that the alteration of nickel-based catalysts with second transition metals is a viable solution to avoid the deactivation of nickel catalysts. Ni impregnation with a second metal can lead to important changes in its stability and activity because of the effect of alloy formation<sup>24</sup>. Bayat et al.<sup>25</sup> studied the influence of Fe addition into  $\text{Ni}/\text{Al}_2\text{O}_3$  catalyst in methane decomposition reaction for hydrogen production. They observed that the addition of 10 wt% of Fe led to improving the stability and activity of  $\text{Ni}/\text{Al}_2\text{O}_3$  catalyst through obstruction the carbon encapsulating formation on the surface of catalyst, along with enhancing the carbon diffusion rate. Ali et al.<sup>26</sup> examined the influence of adding other metals, such as La, Ce, Cu, Co, and Fe, on the catalytic performance of  $\text{Ni}/\text{MgO}-\text{Al}_2\text{O}_3$  catalyst at different reaction temperatures. Among the added metals studied, it was found that adding 10 wt% Cu to the  $\text{Ni}/\text{MgO}-\text{Al}_2\text{O}_3$  catalyst led to an enhancement of its catalytic performance, methane conversion and hydrogen yield. Al-Fatesh et al.<sup>27,28</sup> investigated the impact of modifying  $\text{ZrO}_2$  supports with  $\text{La}_2\text{O}_3$  or  $\text{WO}_3$  on the performance of  $\text{Fe}-\text{Ni}/\text{x}-\text{ZrO}_2$  catalysts for methane decomposition. Their results showed that doping  $\text{ZrO}_2$  with  $\text{La}_2\text{O}_3$  or  $\text{WO}_3$  significantly enhanced hydrogen yield and catalyst stability. Further, they reported that incorporation of Ni further improved the activity and stability of all Fe-based catalysts. Awadallah et al.<sup>29</sup> studied the effect of Mo on the catalytic activity of  $\text{Ni}/\text{Al}_2\text{O}_3$  catalyst. Their results exhibited that the addition of Mo enhances methane conversions and carbon nanotube (CNT) production. They suggested that Ni component in the catalyst played a role in the decomposition of methane into hydrogen and carbon, while the Mo acts as a carbon diffusion center by facilitating the dissolution of carbon formed on the surface of the nickel particle onto the catalyst. Moreover, the presence of Mo as a promoter in the  $\text{Ni}/\text{Al}_2\text{O}_3$  catalyst provided appropriate metal-support interaction, which could reduce the sintering of catalyst metals and ultimately increase the catalytic activity and stability. Chatla et al.<sup>30</sup> investigated the effect of rare earth metals (La, Pr, Gd, Nd and Sm) adding to the Ni-Al catalyst activity for catalytic decomposition of methane. They observed that the promotion of Ni-Al catalyst with La metal has enhanced the Ni-Al catalyst activity and achieved the highest methane conversions rate compared to the parent catalyst. They attributed the improved activity of the nickel catalyst to the increase in its surface area as well as the strong interaction between nickel and rare metals.

In this study, the catalytic activity of  $\text{NiO}$  was enhanced by modifying it with secondary metals such as Al, Co, and Cu, aimed at improving its efficiency for the direct decomposition of methane into hydrogen and carbon nanostructures. This approach also seeks to avoid the need for catalyst support materials, which can sometimes cause strong metal-support interactions that reduce catalytic performance<sup>21,31,32</sup>. A key objective of this work is to develop cost-effective catalysts with well-defined properties by carefully selecting metal types and using a simple wet-chemical synthesis method, ultimately achieving high efficacy of methane decomposition.

## Experimental

### Synthesis of mixed oxides catalysts

Nickel nitrate hexahydrate  $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (99%), cobalt nitrate hexahydrate  $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  (98%), copper nitrate trihydrate  $\text{Cu}(\text{NO}_3)_2 \cdot 3\text{H}_2\text{O}$  (99.5%) were purchased from Loba Chemie Pvt. Ltd., while aluminum nitrates nonahydrate  $\text{Al}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  (98%) was supplied by alpha chemika. These chemicals have been used without additional purification. Nickel oxide,  $\text{NiO}$ , was prepared by direct calcination of nickel nitrate hexahydrate in air at temperature of  $500\text{ }^\circ\text{C}$ . The simple wet chemical method was adopted to synthesize mixed metal oxides. For 10 wt% Al-NiO metal oxide sample, in agate mortar 8.917 g of  $\text{Ni}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  was dissolved in a small amount of distilled water while stirring it by a pestle until completely dissolved. This was followed by adding 2.78 g of  $\text{Al}(\text{NO}_3)_3 \cdot 9\text{H}_2\text{O}$  to the solution and then continuing to stir with the pestle again. The solution was kept in the air and then dried in the oven overnight at  $80\text{ }^\circ\text{C}$ . Later, the resultant was crushed into powder and calcined in furnace for 4 h at  $500\text{ }^\circ\text{C}$ . The preparation of 10% Co-Ni and 10% Cu-Ni (wt./wt.) metal oxides, same procedures were used by taking 0.9877 and 0.98 g of cobalt nitrate hexahydrate and copper nitrate trihydrate, respectively.

## Characterization of materials

Characterization of fresh and spent materials (catalysts) was performed using different techniques. Texture properties of these materials, surface area and pore size, were measured utilizing Quantachrome autosorb IQ model ASIQA3V600000-6. For materials morphology, scanning electron microscope SEM (QUANTA 250 FEI; USA) was used. The identification of materials phases was confirmed using X-ray diffractometer XRD (Rigaku International) with Cu Ka radiation of  $=1.543\text{ \AA}$ . Raman spectra of the materials has been taken by a Micro Raman (SENTERRA II, Brucker) spectrometer at wavelength 532 nm and laser power of 2.25 mW, respectively. The reducibility of the synthesized materials was conducted using temperature programmed reduction (TPR) (Micromeritics AutoChem-II 2920). The surface chemical composition and oxidation states of materials were investigated by X-ray photoelectron spectroscopy, XPS. Thermo K Alpha spectrometer utilizing Al K alpha X-rays (1486.6 eV) with a spot size of 400  $\mu\text{m}$  utilizing flood gun for charge compensation. Moreover, the values of all binding energy were standardized to C 1s = 284.5 eV as an internal standard. Thermogravimetric measurements, TGA, (NETZSCH TG 209 F1 Libra) was utilized in the air environment in the temperature range from room temperature up to 1000  $^{\circ}\text{C}$ , with heating rate of 10  $^{\circ}\text{C}/\text{min}$  to estimate the weight of the carbon formed on spent materials by assistance of Netzsch proteus 70 software.

## Catalytic activity and product analysis

The activity of NiO, Al-Ni, Co-Ni, and Cu-Ni materials for direct methane decomposition was investigated in a fixed-bed reactor made of a quartz tube, 50 cm in length and 1.5 cm in internal diameter. A 0.5 g sample of the unreduced material was placed as a sandwich between ceramic fibers at the center of the quartz tube, which was in the middle of the heating zone at 800  $^{\circ}\text{C}$ . The materials were not subjected to reduction processes because methane itself is considered reductant. A gas mixture of 75%  $\text{CH}_4$  and 25%  $\text{N}_2$  (purity 99.99%, supplied by AHG) was used as the reactant. The flow rate of the gas mixture into the reactor was set to 20 mL/min using a mass flow controller (MKS PR4000B). Nitrogen was used as an internal standard during the analysis. The reaction products were analyzed by connecting the reactor outlet to an on-line gas chromatograph (Agilent GC Model 7890 B) equipped with a 19,043 Restek Micropacked GC Column, Shin carbon ST 80/100, 2 m, 0.53 mm i.d., Bellefonte, USA. The column was connected to a thermal conductivity detector (TCD) with helium as the carrier gas. During the analysis, the detected gas phases were unreacted to methane, nitrogen, and produced hydrogen. CO and  $\text{CO}_2$  traces were measured using Fourier transform infrared spectroscopy (FTIR) (Thermo Scientific OMNIC).

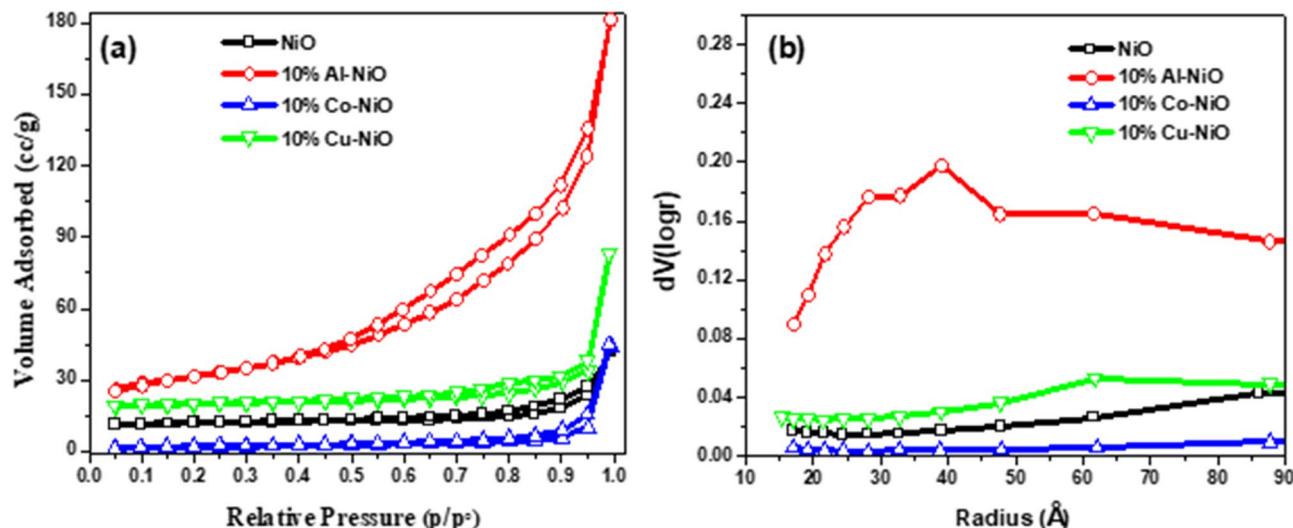
## Results and discussion

### Fresh catalysts characterization

#### Textural properties

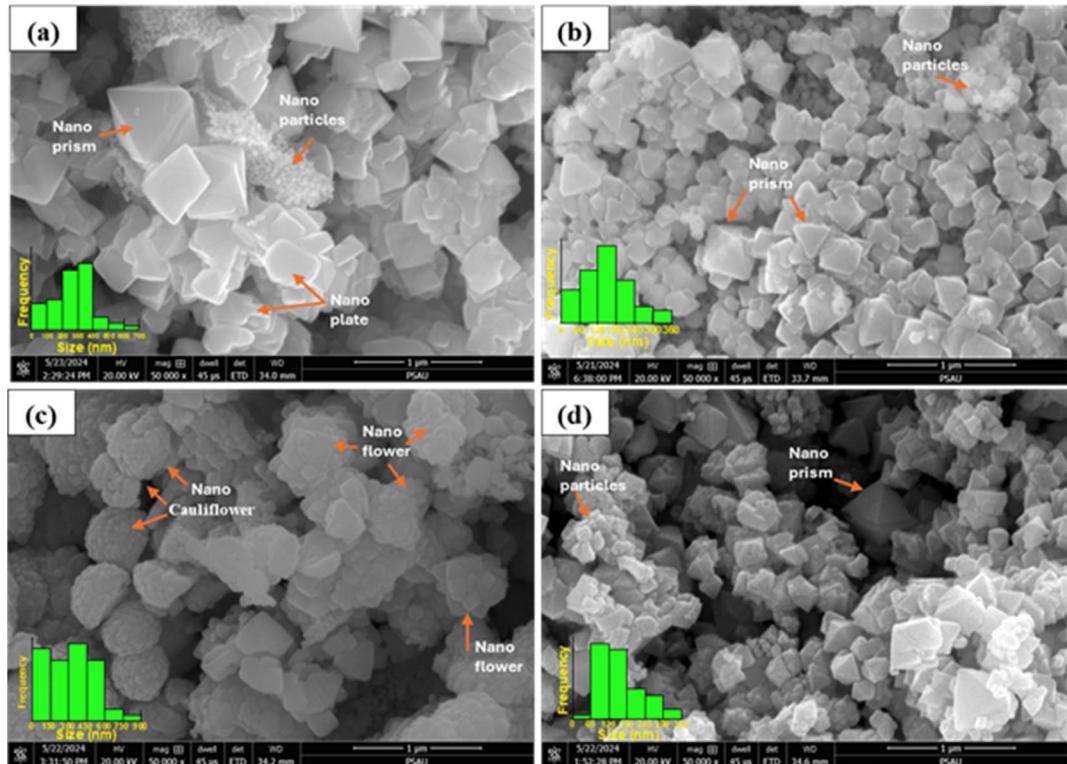
Figure 1(a, b) displays the  $\text{N}_2$  adsorption-desorption isotherms and the pore size distribution profiles of fresh NiO, 10%Al-NiO, 10%Co-NiO and 10%Cu-NiO materials at temperature of 77 K.

From Fig. 1 (a), the isotherm of pure NiO nanostructures exhibits a type IV hysteresis loops. According to the IUPAC classification, this result indicates that NiO has a mesoporous structure with non-rigid aggregates of plate-like particles<sup>33</sup>. The hysteresis is flattened and narrow hysteresis up to  $p/p^{\circ} \sim 0.75$  and slightly increases at higher  $p/p^{\circ} > 0.8$  due to capillary condensation. Similar BET isotherms for NiO nanowires have been reported in<sup>34</sup>. The isotherms of NiO promoted with  $\text{Al}^{3+}$ ,  $\text{Co}^{2+}$ , and  $\text{Cu}^{2+}$  ions also exhibit type IV with H3 hysteresis, but with varying nitrogen uptake values and steeper capillary condensation. Notably, the isotherm of 10%Al-NiO shows a wide mesoporous range from  $p/p^{\circ} \sim 0.45 - 0.9$ , with the highest  $\text{N}_2$  uptake,



**Fig. 1.** (a) Isotherm and (b) pore radius distribution of the fresh NiO, 10%Al-NiO, 10%Co-NiO and 10%Cu-NiO materials.

Materials	Surface area (m <sup>2</sup> /g)	Pore volume (cc/g)
NiO	5.12	0.05
10%Al-NiO	74.44	0.26
10%Co-NiO	4.13	0.07
10%Cu-NiO	8.50	0.10

**Table 1.** Texture parameters of NiO, 10%Al-NiO, 10%Co-NiO and 10%Cu-NiO materials.**Fig. 2.** FE-SEM images of fresh (a) pure NiO, (b) 10% Al-NiO, (c) 10% Co-NiO and (d) 10% Cu-NiO materials.

indicating a larger and wider pore distribution compared to NiO, 10%Co-NiO, and 10%Cu-NiO materials. In contrast, the isotherm of 10%Co-NiO is lower than that of NiO, suggesting a reduced mesoporous content. The pore size distribution of these materials was also studied using the Barrett-Joyner-Halenda (BJH) method, and the results are plotted in Fig. 1(b). As expected, 10%Al-NiO exhibits an asymmetric monomodal-wide distribution, with a maximum pore radius at  $\sim 39$  Å. The 10%Cu-NiO has a maximum pore radius at  $\sim 61$  Å. In contrast, NiO and 10%Co-NiO display a very narrow distribution, suggesting consistent pore radii. Moreover, the surface areas of these materials were measured by Brunauer-Emmett Teller (BET). Table 1 summarizes the textural parameters of the examined materials, clearly showing that the surface area follows the order 10%Al-NiO  $>>$  10%Cu-NiO  $>>$  NiO  $>>$  10%Co-NiO. From the literature, it is suggested that the catalytic performance of materials is closely related to their porous properties<sup>35</sup>.

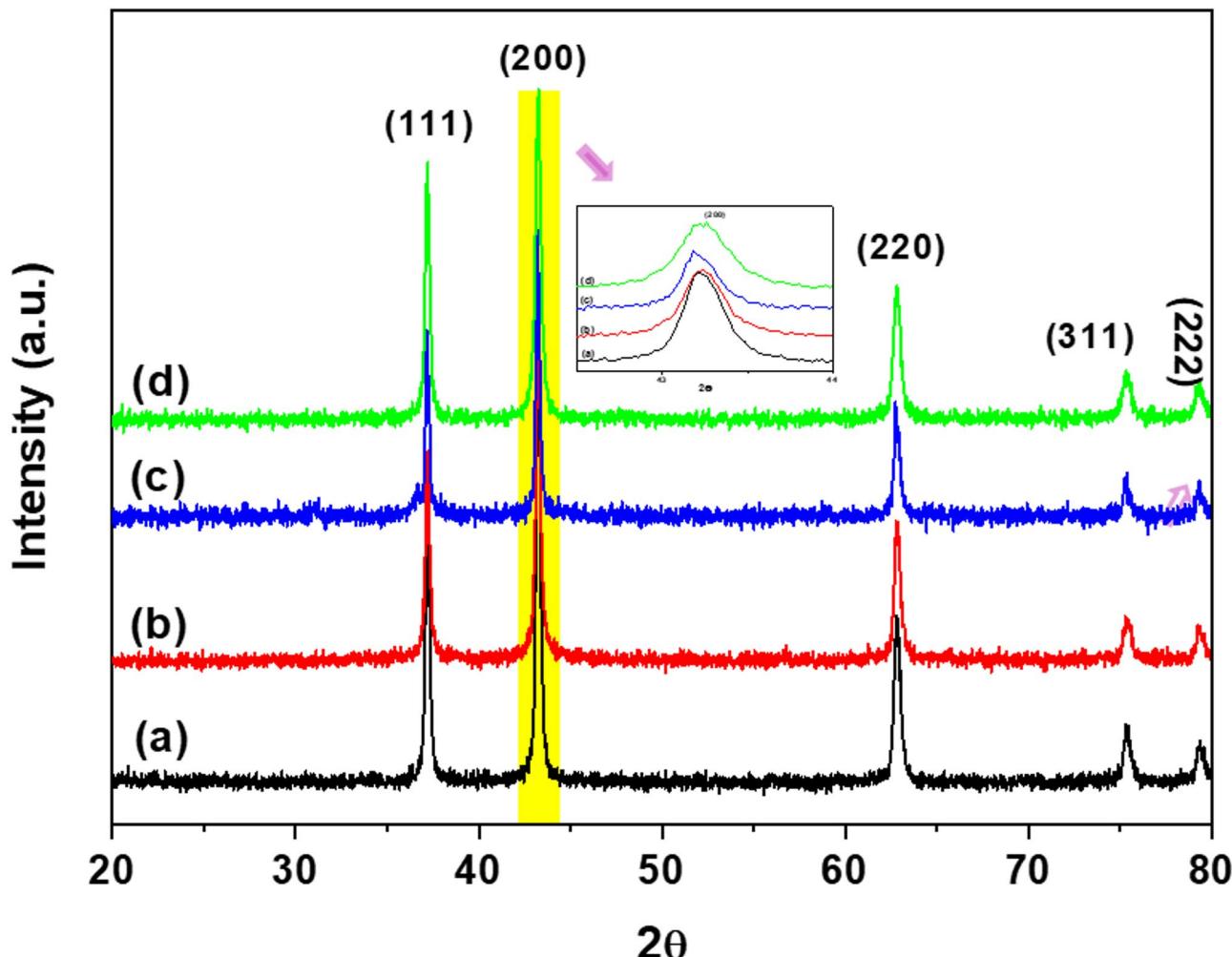
#### Morphology analysis

The surface morphology of fresh NiO and Al<sup>3+</sup>, Co<sup>2+</sup>, and Cu<sup>2+</sup>-doped NiO materials is shown in Fig. 2. ImageJ software was used to estimate the nanostructure size distributions for all examined samples, as seen in the inset of Fig. 2. The morphology of pure NiO nanostructures (Fig. 2 (a)) exhibits various morphologies nanostructure such as nano prism, nanoplates and nanoparticles tending to aggregate into larger grains. The NiO nanostructures have a wide size range with an average size of 300–400 nm as shown in the inset of Fig. 2(a). The incorporation of Al<sup>3+</sup> and Cu<sup>2+</sup> ions into NiO preserves the morphology, however, smaller size nano prism and nanoparticles with an average size of 150 nm and 120 nm for 10% Al-NiO and 10% Cu-NiO, as seen in Fig. 2 (b, d). In contrast, the incorporation of Co<sup>2+</sup> ions into NiO leads to the formation of relatively larger nanoflowers and nano cauliflower as shown in Fig. 2(c). The 10% Co-NiO nanoflowers composed of petals that growth radially, while the nano cauliflower composed of aggregated nanoparticles of size 130 nm. The average size of the 10% Co-NiO nanoflowers/ nano cauliflower is 300–450 nm. The pore size/volume, which is the gap

between the nanostructures, correlates with the nanostructure size. As a result, smaller nanostructures could lead to increased interparticle porosity. Therefore, the 10% Al–NiO and 10% Cu–NiO composites probably have higher porosity than pure NiO and 10% Co–NiO materials.

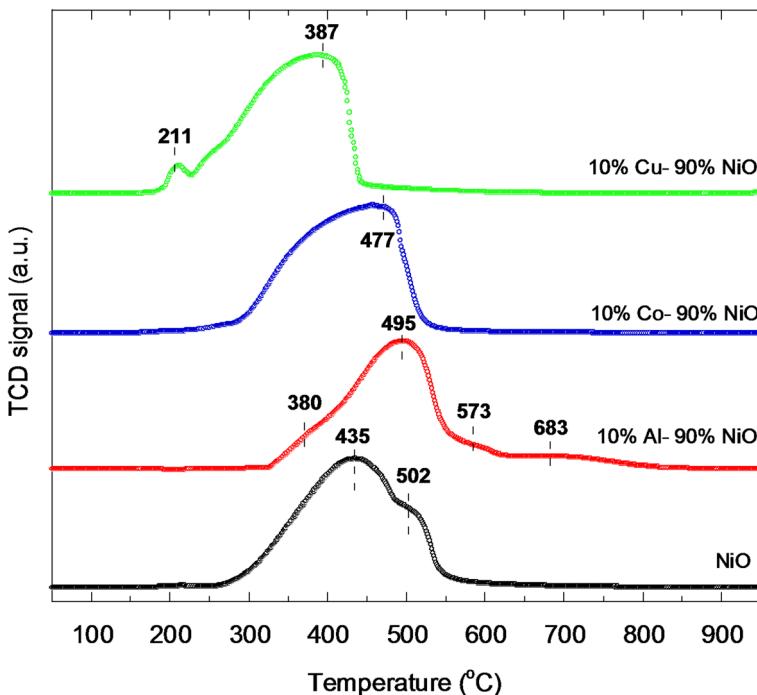
#### XRD studies

The phases and crystallinity of the examined materials have been investigated with XRD and results are depicted in Fig. 3. For the pure NiO sample, the diffraction peaks are sharp, implying a high degree of crystallinity. The peak positions at  $2\theta \sim 37.20^\circ$ ,  $43.20^\circ$ ,  $62.87^\circ$ ,  $75.20^\circ$ , and  $79.38^\circ$  correspond to the standard face-centered cubic (FCC) structure of NiO (JCPDS No. 04-0835). Hence, the observed peaks are indexed to the (111), (200), (220), (311), and (222) diffraction planes<sup>36</sup>. No other unknown peaks were observed suggesting the purity and mono-phase of the synthesized NiO material. The XRD patterns of NiO incorporated with  $\text{Al}^{3+}$ ,  $\text{Co}^{2+}$ , and  $\text{Cu}^{2+}$  promoter ions are also presented in Fig. 3. Clearly, the XRD patterns of 10%Al-NiO, 10%Co-NiO, and 10%Cu-NiO materials resemble that of pure NiO, indicating that the NiO phase dominates in the examined materials. The absence of distinct Al, Co, and Cu peaks in the XRD patterns of these NiO-based materials likely reflects the fine distribution of these ions within the NiO matrix. Alternatively, the concentration of Al, Co, and Cu in the composites may be below the detection limit of the XRD instrument. However, zooming in on the (200) peak, as shown in the inset of Fig. 3, reveals that the width and position of the (200) peak vary upon the incorporation of  $\text{Al}^{3+}$ ,  $\text{Co}^{2+}$ , and  $\text{Cu}^{2+}$  promoters' ions. This is likely attributed to the differences in ionic radii ( $r_{\text{Ni}^{3+}} = 0.69 \text{ \AA}$ ,  $r_{\text{Ni}^{4+}} = 0.56 \text{ \AA}$ ,  $r_{\text{Al}^{3+}} = 0.54 \text{ \AA}$ ,  $r_{\text{Co}^{2+}} = 0.74 \text{ \AA}$ ,  $r_{\text{Cu}^{2+}} = 0.73 \text{ \AA}$ ). A peak shift to a lower diffraction angle indicates an increase in the lattice spacing (d-spacing) of the crystal lattice, and vice versa. Meanwhile, the broadening of the diffraction peaks suggests a reduction in crystallite size. The crystallite size and lattice parameter  $a$  of the pure NiO and NiO-based materials were calculated from the (200) peak using the Scherrer equation  $G = \frac{0.9 \cdot \lambda}{\beta \cdot \cos\theta}$ , and the relation  $a = \sqrt{d^2(h^2 + k^2 + l^2)}$ , respectively. Here,  $\lambda = 1.54 \text{ \AA}$ ,  $\beta$  is the full width at half maximum (FWHM),  $hkl$  refers to the miller indices of the peak (200) at angle  $\theta$  and  $d$  is the inter-planar distance. Table 2 summarizes the XRD analysis data of the examined materials.



**Fig. 3.** The XRD patterns of (a) pure NiO, (b) 10% Al-NiO, (c) 10% Co-NiO and (d) 10% Cu-NiO materials.

Sample	$2\theta$ (deg)	$\beta$ (FWHM)	Crystal size (nm)	d spacing (Å)	a (Å)
NiO	43.22	0.28	30.5	2.091	4.182
10% Al-NiO	43.24	0.30	28.5	2.09	4.18
10% Co-NiO	43.18	0.24	35.6	2.093	4.185
10% Cu-NiO	43.26	0.34	25.1	2.089	4.178

**Table 2.** XRD parameters calculated for diffraction line “200”.**Fig. 4.**  $H_2$ -TPR profiles of pure NiO, 10%Al-NiO, 10%Co-NiO and 10%Cu-NiO materials.

As inferred from Table 2, the crystallite size of NiO decreases upon the incorporation of  $Al^{3+}$  and  $Cu^{2+}$ , from 30.5 nm to 28.5 nm and 25.11 nm, respectively. Meanwhile, the crystallite size increases to 35.6 nm with the incorporation of  $Co^{2+}$  ions. The crystallite size estimated from the XRD data of NiO-based materials shows somewhat the same trend as the nanostructure size estimated from SEM images. Furthermore, based on the lattice parameter  $a$  value, it can be suggested that the NiO lattice is slightly compressed with  $Al^{3+}$  and  $Cu^{2+}$ , while it expands with  $Co^{2+}$  incorporation. The observed slight lattice compression upon  $Cu^{2+}$  incorporation may not be explained by ionic size alone and probably due to Jahn-Teller compression<sup>37</sup>. Similar observations have been reported for NiO structures upon the incorporation of  $Al^{3+}$ ,  $Cu^{2+}$ , and  $Co^{2+}$  ions<sup>38–40</sup>. The compression of the lattice parameters likely induces structural defects, which play a crucial role in catalytic performance.

#### $H_2$ -TPR measurements

Figure 4 shows the  $H_2$ -TPR profiles of pure NiO and NiO promoted with 10 wt% of Al, Co and Cu separately. The  $H_2$ -TPR profile of pure NiO exhibits a broad peak centered at 435 °C, with a shoulder at a higher temperature of 502 °C. These peaks correspond to the reduction of NiO to metallic Ni ( $Ni^{2+} \rightarrow Ni^0$ )<sup>41</sup>. SEM images of the NiO nanoparticles indicate a wide distribution size ranging from 50 to 700 nm. Incorporating 10 wt% of Al, Co, or Cu as promoters into NiO results in distinct TPR profiles compared to pure NiO, with additional reduction peaks and shifts in peak positions. The  $H_2$ -TPR profile of 10% Al-NiO is dominated by a reduction peak at 495 °C, with additional shoulders observed at 385 and 573 °C. Ahmed et al.<sup>42</sup> characterized the 60%Ni/ $Al_2O_3$  catalyst by temperature-programmed reduction by  $H_2$  ( $H_2$ -TPR). They observed that there are three broad reduction peaks at temperatures of 200–400, 400–500 and 600–700 °C. They suggested that the reduction peak between 200 and 400 °C can be attributed to the facile reduction of pure NiO phases, whereas the second reduction peak between 400 and 500 °C can be related to the reduction of both NiO with small particles and NiO contact with the aluminum. Lastly, the third peak of reduction at higher temperature of 600–700 °C is corresponding to the reduction of some  $NiAl_2O_4$  species. Therefore, it can be suggested that the peaks at 385 °C and 495 °C are associated with the reduction of smaller NiO NPs and NiO contact with the Al, respectively, while the peak at 573 °C is likely attributed to reduction of possible formed  $NiAl_2O_4$  species.

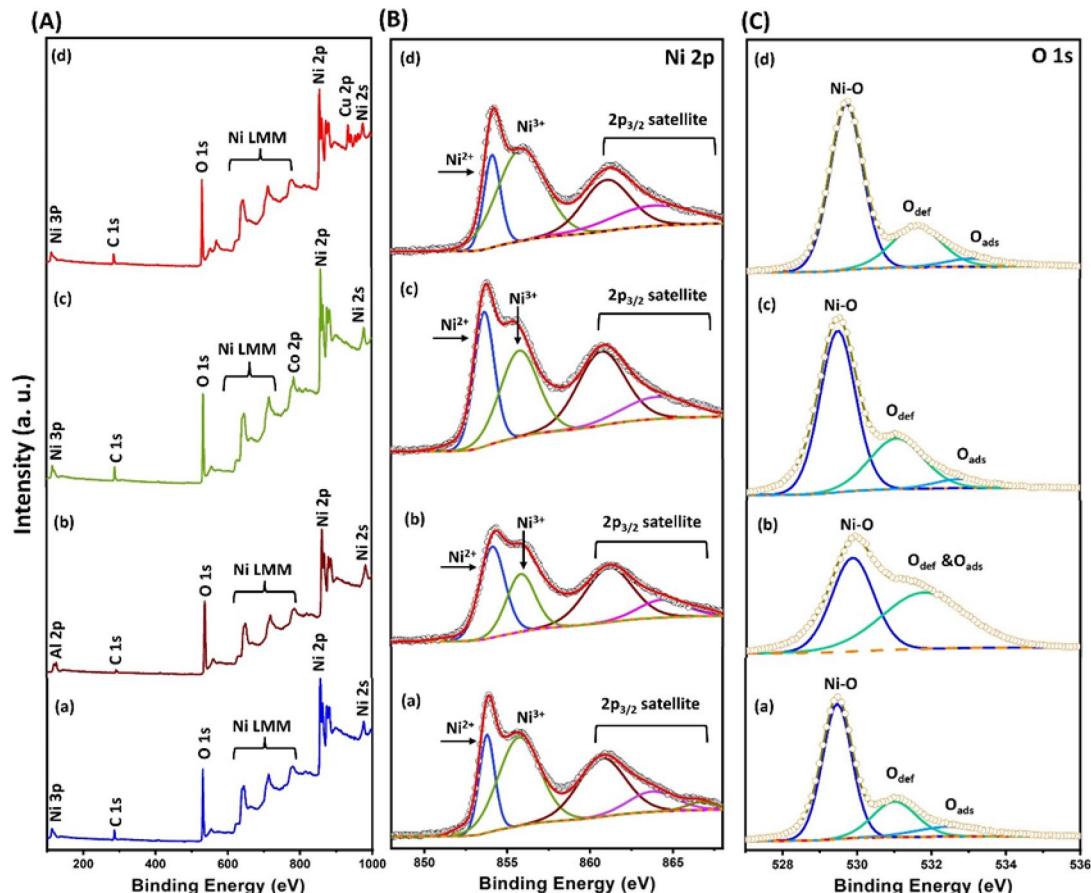
The  $\text{H}_2$ -TPR profile of 10% Co-NiO shows a broad reduction peak centered at 477 °C, attributed to the reduction of NiO nanoparticle. No distinct reduction peak for  $\text{Co}^\circ$  is observed, indicating that  $\text{Co}_3\text{O}_4$  reduces to  $\text{Co}^\circ$  ( $\text{Co}_3\text{O}_4 \rightarrow \text{CoO} \rightarrow \text{Co}^\circ$ ) within the temperature range of 200–600 °C<sup>43</sup>. This suggests an overlap in the reduction processes of Co and Ni, resulting in a broad peak rather than distinct peaks for Co and Ni, as seen in Fig. 4.

Finally, the  $\text{H}_2$ -TPR profile of 10% Cu-NiO shows two distinct reduction peaks around 208 °C and 385 °C, which are ascribed to the reduction of finely dispersed CuO NPs and NiO NPs, respectively<sup>44</sup>. It is evident that the reduction profile of NiO strongly dependent on the type of promoters.

#### XPS and Raman analysis

To identify the surface chemical composition of the examined materials, survey XPS spectra were acquired, and the results are shown in Fig. 5. The survey XPS spectrum of NiO (Fig. 5A (a)) is dominated by the characteristic peaks of Ni and oxygen<sup>45</sup>. For example, Ni 3p, Ni 3s, Ni LMM (Auger), Ni 2p, and Ni 2s peaks are observed, representing Ni metal. Additionally, one observes O 1s peak corresponds to oxygen and small peak at 285 eV assigned to carbon C 1s as a residual contamination during the material synthesis process. The survey spectra of NiO incorporated with 10 wt% of Al, Co, and Cu are also shown in Fig. 5A. Clearly, the spectra resemble that of pure NiO; however, traces of the incorporated Al, Co, and Cu ions can be observed. For example, the Al 2p peak at 72 eV overlaps with the Ni 3p peak at 66.5 eV, as seen in Fig. 5A(b); the Co 2p<sub>3/2</sub> peak appears at 778.5 eV (Fig. 5A(c)); and the Cu 2p<sub>3/2</sub> peak is at 923.5 eV (Fig. 5A(d)). The elemental analysis of the samples investigated is summarized in Table 3. It should be mentioned that XPS is a surface-sensitive technique, therefore, when confirming the presence of the incorporated ions, the quantitative elemental composition should be interpreted with caution.

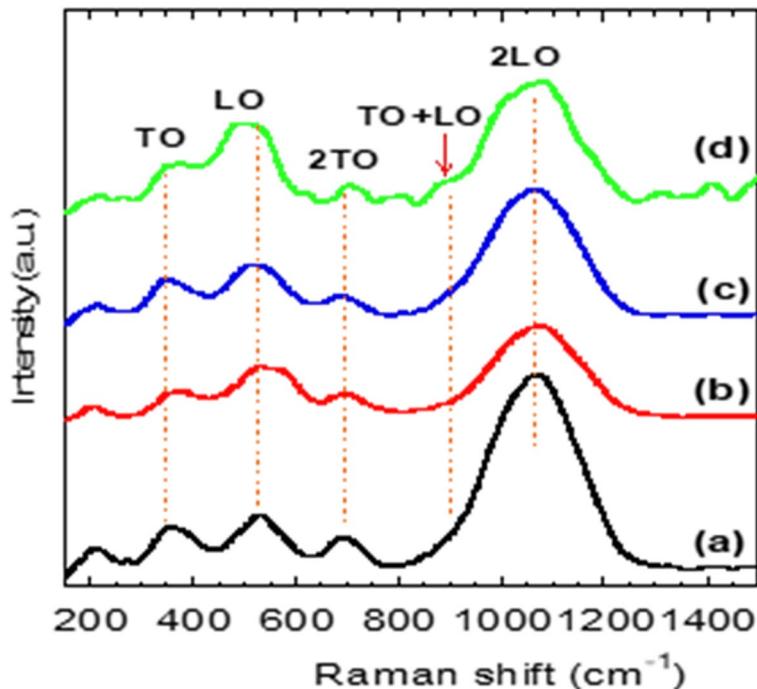
To resolve the oxidation states of NiO nanostructure upon the incorporation of  $\text{Al}^{3+}$ ,  $\text{Co}^{2+}$  and  $\text{Cu}^{2+}$  prompter ions, high-resolution spectra of Ni 2p and O 1s from the examined materials and results are depicted in Fig. 5 (B, C). The high-resolution Ni 2p spectrum of pure NiO exhibits a strong peak Ni 2p<sub>3/2</sub> at 856 eV and shake-up at the higher B.E of 862 eV as seen in Fig. 5B (a). The peak Ni 2p<sub>3/2</sub> can be deconvoluted into two sub-peaks; at 853.8 eV and 855.6 eV correspond to  $\text{Ni}^{2+}$  and  $\text{Ni}^{3+}$ , respectively<sup>46</sup>. The incorporation of  $\text{Al}^{3+}$ ,  $\text{Co}^{2+}$ , and  $\text{Cu}^{2+}$  ions exert distinct effects on the Ni 2p<sub>3/2</sub> spectrum. The incorporation of  $\text{Al}^{3+}$  and  $\text{Co}^{2+}$  results in an increase in the  $\text{Ni}^{2+}$  component in the Ni 2p<sub>3/2</sub> spectrum, as shown in Fig. 5B(b), whereas  $\text{Cu}^{2+}$  incorporation does not significantly alter the  $\text{Ni}^{2+}$  signal. The increase in  $\text{Ni}^{2+}$  upon  $\text{Al}^{3+}$  doping is likely due to the charge imbalance caused by substituting a trivalent  $\text{Al}^{3+}$  ion into a divalent  $\text{Ni}^{2+}$  site, which is compensated by the reduction of  $\text{Ni}^{3+}$ .



**Fig. 5.** (A) Survey XP spectra, High-resolution (B) Ni 2p spectra and (C) O 1s spectra for (a) pure NiO, (b) 10% Al-NiO, (c) 10% Co-NiO and (d) 10% Cu-NiO materials.

Sample	Ni 2p %	O 1s%	Al 2p%	Co 2p%	Cu 2p%	C 1s%
NiO	37.7	46.3	--	--	--	16
10% Al-NiO	30.2	54.1	8.9	--	--	6.8
10% Co-NiO	33.6	44.5	--	4.0	--	17
10% Cu-NiO	32.5	44.7	--	--	7.9	14.9

**Table 3.** Elemental analysis of pure NiO and NiO incorporated Al<sup>3+</sup>, Co<sup>2+</sup>, and Cu<sup>2+</sup>.



**Fig. 6.** Raman Spectra of (a) pure NiO, (b) 10% Al-NiO, (c) 10% Co-NiO and (d) 10% Cu-NiO materials.

to Ni<sup>2+</sup> or the formation of oxygen vacancies. In the case of Co<sup>2+</sup>, the similar ionic charge allows substitution without formal charge imbalance; however, its redox-active nature and potential for Co<sup>3+</sup>/Co<sup>2+</sup> transitions may influence local electron distribution, promoting partial reduction of Ni<sup>3+</sup> to Ni<sup>2+</sup>. On the other hand, Cu<sup>2+</sup> also a divalent ion, does not introduce charge imbalance and appears to have limited redox interaction under the tested conditions, resulting in minimal impact on the Ni oxidation state.

The O 1s spectrum for NiO material is shown in Fig. 5C(a), and it is fitted into three peaks: at 529.5 eV assigned to nickel atom bonded to oxygen (Ni—O); at 531.2 eV (O<sub>def</sub>) corresponding to oxygen defect/vacancy<sup>47</sup>; and at 532.6 eV (O<sub>ads</sub>), attributed to chemisorbed water on the surface<sup>48</sup>. The O 1s spectra of NiO incorporated with Al<sup>3+</sup>, Co<sup>2+</sup>, and Cu<sup>2+</sup> ions are also presented in Fig. 5C (b, c,d). The incorporation of Al<sup>3+</sup> induces an increase in the oxygen defect component (O<sub>def</sub>) compared to that in pure NiO and NiO incorporated Co<sup>2+</sup> and Cu<sup>2+</sup> ions. This change in the oxidation state of NiO due to Al<sup>3+</sup> incorporation may affect its performance as catalyst for methane decomposition.

Figure 6 shows the Raman spectra of pure NiO and NiO incorporated with 10% Al<sup>3+</sup>, Co<sup>2+</sup>, and Cu<sup>2+</sup> ions. The Raman spectrum of pure NiO nanostructures exhibits four peaks at 352 cm<sup>-1</sup>, 531 cm<sup>-1</sup>, 693 cm<sup>-1</sup>, and ~1067 cm<sup>-1</sup>, which are assigned to the TO (1st order transverse optical), LO (1st order longitudinal optical), 2TO (2nd order transverse optical), and 2LO (2nd order longitudinal optical) modes of face-centered cubic NiO nanostructures, respectively<sup>49</sup>. The LO and 2LO modes are associated with the vibrations of Ni—O bonds. Furthermore, the sharp LO emission peak indicates the presence of nickel defects and/or the coexistence of Ni<sup>3+</sup> and Ni<sup>2+</sup> ions. Similar Raman modes of intrinsic NiO nanostructures have been reported by<sup>50</sup>, confirming the phase purity of the synthesized NiO nanostructures.

The Raman modes of NiO incorporated with 10% Al<sup>3+</sup>, Co<sup>2+</sup>, and Cu<sup>2+</sup> ions resemble those of pure NiO and exhibit the characteristic TO, LO, 2TO, and 2LO Raman modes, as shown in Fig. 6 (b, c,d). However, variations in Raman band intensity, position, and width are observed when compared to the intrinsic NiO modes. For example, the intense LO mode in the spectra of 10% Cu-NiO suggests an increase in nickel defects<sup>48,49</sup>, which is consistent with the XRD and XPS results. The shift in band position and broadening is likely related to cation redistribution, as ions with different radii replace Ni<sup>2+</sup>, Ni<sup>3+</sup> ions, affecting the vibrational frequencies and

leading to mode broadening. Additionally, a new Raman mode at  $945\text{ cm}^{-1}$  is observed in the 10% Cu-NiO Raman spectra, which is assigned to a combination of TO and LO modes<sup>49</sup>.

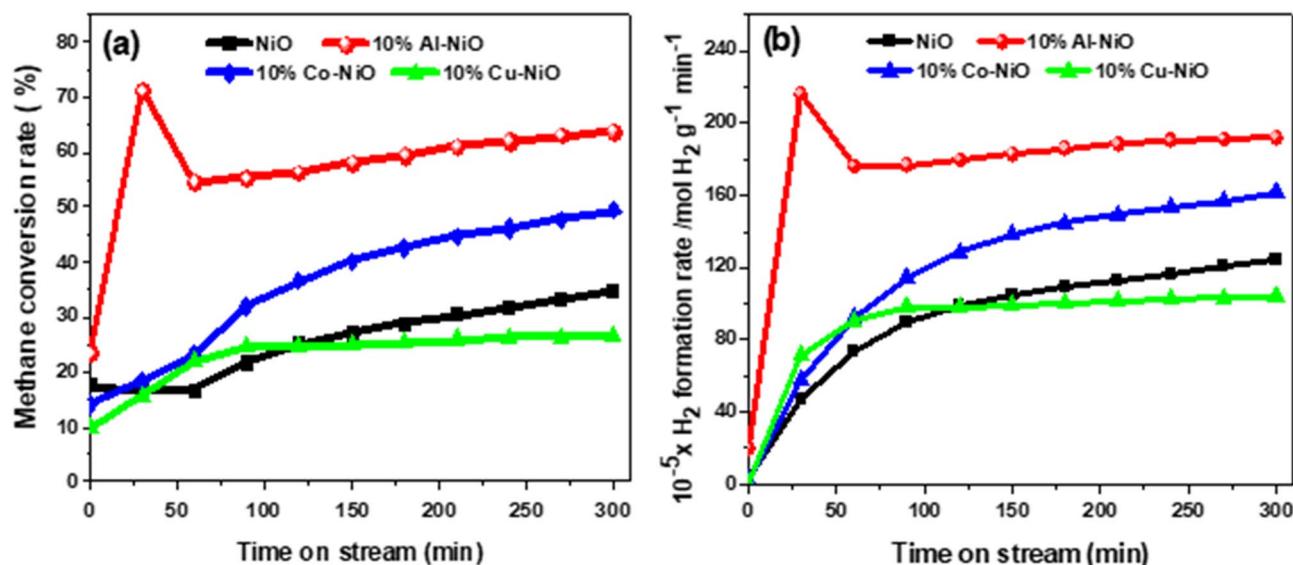
### Catalytic activity studies

Figure 7 (a, b) demonstrates the methane conversion rate percentage and the rate of hydrogen formation as a function of time on stream (TOS) for direct decomposition of methane over pure NiO, 10% Al-NiO, 10% Co-NiO and 10% Cu-NiO catalysts at temperature of  $800\text{ }^{\circ}\text{C}$  and gas flow rate of  $20\text{ mL/min}$ .

From Fig. 7 (a), it is obvious that there is variation in the activity of the catalysts used in terms of percentage of methane conversion rate. The catalysts activity was in order of 10% Al-NiO > 10% Co-NiO > NiO > 10% Cu-NiO, which have achieved the highest percentage of methane conversion rate of 71.0, 49.50, 34.80 and 26.90%, respectively. Figure 7 (b) shows the hydrogen formation rate, which is consistent with the percentage of methane conversion rate over these catalysts. Similarly, the highest rates of hydrogen formation were  $216.20$ ,  $161.70$ ,  $124.60$  and  $103.40 \times 10^{-5}\text{ mol H}_2\text{ g}^{-1}\text{ min}^{-1}$  for the catalysts of 10% Al-NiO > 10% Co-NiO > NiO > 10% Cu-NiO, respectively.

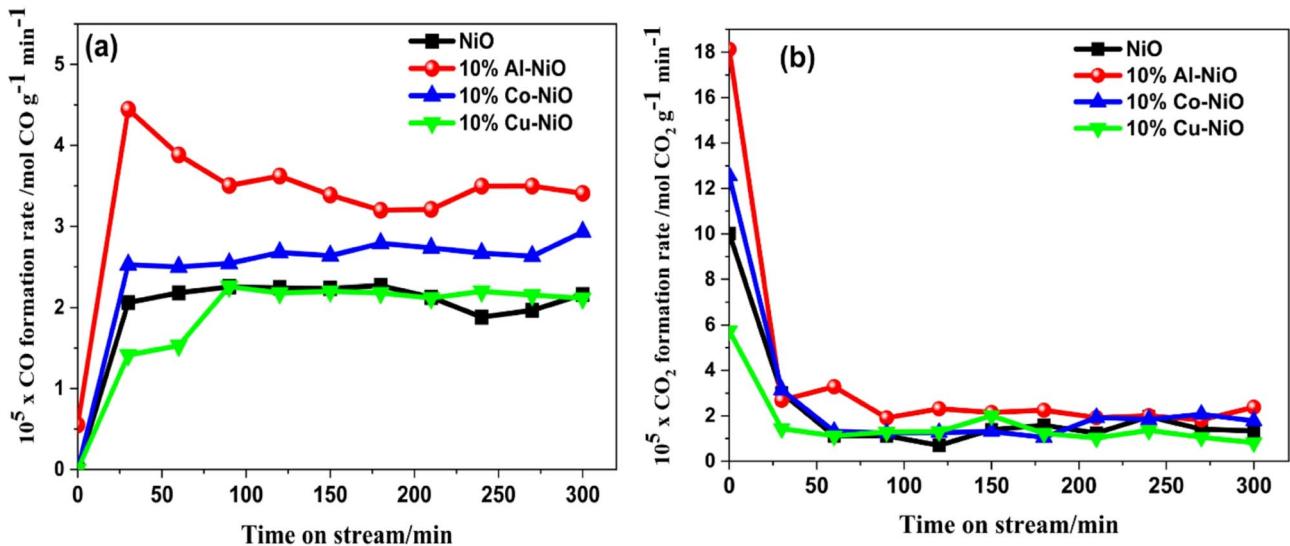
The superior catalytic performance of 10%Al-NiO compared to 10%Co-NiO and 10%Cu-NiO in methane conversion can be attributed to a synergistic combination of textural, structural, and electronic properties influenced by the incorporated promoter  $\text{Al}^{3+}$  ions. BET analysis reveals that  $\text{Al}^{3+}$  incorporation significantly enhances the surface area and mesoporosity of NiO, as evidenced by the highest nitrogen uptake and broad pore size distribution, providing more accessible active sites for methane adsorption and activation. Additionally, H<sub>2</sub>-TPR analysis indicates a multi-step reduction process for Al-NiO, with a major peak at  $495\text{ }^{\circ}\text{C}$  and additional peaks up to  $683\text{ }^{\circ}\text{C}$ , suggesting strong metal–support interaction and the formation of  $\text{NiAl}_2\text{O}_4$  spinel species, which are known to improve thermal stability and redox behavior. XPS analysis supports these findings by showing an increase in the  $\text{Ni}^{2+}$  state and oxygen vacancies in 10% Al-NiO, due to charge compensation from  $\text{Al}^{3+}$  substitution, which enhances the electron density around active sites and facilitates methane activation. Raman spectroscopy further confirms structural modifications through shifts and broadening of LO and 2LO modes, indicating cation substitution and defect formation. In contrast, 10% Co-NiO shows moderate performance, with a relatively lower surface area and overlapping reduction peaks, indicating weaker interaction and less-prominent redox behavior. Although the 10% Cu-NiO material exhibits somewhat enhanced porosity, it demonstrates the lowest catalytic performance among the tested catalysts. This can be attributed to the early reduction of CuO at  $211\text{ }^{\circ}\text{C}$ , compared to NiO at  $311\text{ }^{\circ}\text{C}$ , leading to the premature formation of metallic Cu. The presence of metallic Cu may block Ni active sites or reduce their dispersion, thereby impairing the catalyst's effectiveness in methane conversion. Furthermore, copper has a strong affinity for carbon, which can promote carbon deposition on the catalyst surface. As a result, the active Ni phase becomes encapsulated by carbon layers, further diminishing its catalytic activity<sup>51</sup>.

Table 4 presents a comparative summary of the catalytic performance of the synthesized catalysts for methane decomposition alongside relevant catalysts reported in the literature. As evident, the Ni-based catalysts promoted with 10% Al, Co, and Cu demonstrate significantly enhanced stability, with stable performance beyond 300 min, surpassing many of their supported counterparts. Notably, the 10% Al-NiO and 10% Co-NiO catalysts exhibit not only superior stability but also high methane conversion efficiencies, making them competitive with or superior to similar Ni-based catalysts reported previously. These findings highlight the potential of promoter-incorporated NiO nanostructures as effective and durable catalysts for methane decomposition. It should be



**Fig. 7.** (a) The percentage of methane conversion rate (%) and (b) the rate of hydrogen formation with time on stream (min) of NiO, 10% Al-NiO, 10% Co-NiO and 10% Cu-NiO catalysts, at fixed gas flow rate of  $20\text{ mL/min}$ , reaction temperature of  $800\text{ }^{\circ}\text{C}$ , and catalyst mass of  $0.5\text{ g}$ .

Catalysts	CMD condition	Max. $\text{CH}_4$ conversion %	Time on stream stability	Ref.
NiO	$\text{CH}_4$ , 800 °C	34.8%	Stable > 300 min	This work
10% Cu-NiO	$\text{CH}_4$ , 800 °C	26.9%	Moderate stability	This work
10% Co-NiO	$\text{CH}_4$ , 800 °C	49.5%	Stable > 300 min	This work
10% Al-NiO	$\text{CH}_4$ , 800 °C	71.0%	Stable > 300 min	This work
20% Ni-20% Co/AC	$\text{CH}_4$ , 850 °C	80%	Deactivated after 50 min	<sup>53</sup>
75% Ni-25% Co/ $\text{Al}_2\text{O}_3$	$\text{CH}_4$ , 873 °C	24%	Deactivated after 60 min	<sup>54</sup>
Ni-Co/Al	$\text{CH}_4$ , 650 °C	36%	Deactivated after 35 min	<sup>55</sup>
20% Ni-10% Co/ $\text{Al}_2\text{O}_3$	$\text{CH}_4$ , 500 °C	62.8%	Stable > 180 min	<sup>56</sup>
5% Ni/ $\text{Al}_2\text{O}_3$	$\text{CH}_4$ , 600-800 °C	5-40%	Deactivated after 10 min	<sup>57</sup>
30% Ni/ $\text{Al}_2\text{O}_3$	$\text{CH}_4$ , 700 °C	83%	Stable for over 240 min	<sup>58</sup>
Ni-Cu/ $\text{SiO}_2$	$\text{CH}_4$ , 750 °C	40%	Deactivated after 100 min	<sup>59</sup>
Ni-Cu/Al	$\text{CH}_4$ , 650 °C	38%	Deactivated after 60 min	<sup>55</sup>
Ni30Cu50	$\text{CH}_4$ , 600 °C	78%	Deactivated after 100 min	<sup>60</sup>

**Table 4.** Literature review on catalysts for CMD.**Fig. 8.** (a) CO formation rate and (b)  $\text{CO}_2$  formation rate associated with the hydrogen production, with time on stream (min) at same conditions of Fig. 7.

noted that the experimental parameters for the same catalyst type/composition affect the catalyst performance of methane decomposition<sup>51,52</sup>.

In the current experiment, the NiO, 10% Al-NiO, 10% Co-NiO and 10% Cu-NiO metal were used without reduction pr-treatment. During the methane decomposition reaction,  $\text{CH}_4$  reduces the oxide's component in these catalysts, producing CO and  $\text{CO}_2$ , which accompany hydrogen production. The production of CO and  $\text{CO}_2$  accompanying hydrogen production represents the reduction process of these catalysts<sup>61</sup>. Figure 8. (a, b) illustrates the CO and  $\text{CO}_2$  formation rate, associated with hydrogen production, against time on stream (TOS) at same condition of Fig. 7. From Fig. 8 (a, b), the CO and  $\text{CO}_2$  were formed throughout the reaction and obviously indicate that the reduction process of these catalysts is taking place. The highest formation rates of CO and  $\text{CO}_2$  were observed in the order of 10% Al-NiO > 10% Co-NiO > pure NiO > 10% Cu-NiO. This indicates that the highest reduction processes of these catalysts occurred in this order. As observed from the XPS and Raman analysis of the 10% Al-NiO catalyst, Figs. 5 and 6, it seems that the Al-doped NiO presumably highly facilitated the reduction process by forming more active metal sites compared to other catalysts. This result could be one of the reasons contributing to the high activity of the 10% Al-NiO catalyst.

### Spent catalysts characterization

#### XRD studies

Figure 9. displays the XRD patterns of the spent NiO, 10% Al-NiO, 10% Co-NiO and 10% Cu-NiO catalysts. The spaniel structure of these spent catalysts has completely changed compared to the fresh ones, Fig. 3. This is due

to the reduction process that occurred during the reaction. On the other hand, it is noticeable that these spent catalysts had similar patterns which indicate the formation of graphitic carbon and metallic Ni. The diffraction peak at  $2\theta = 26.2^\circ$  was appointed to the formation of crystalline graphitic carbon with (002) lattice plane, while there are three characteristic diffraction patterns attributed to metallic nickel which are evidently noted at ca.  $44.5^\circ$ ,  $52.1^\circ$ , and  $76.5^\circ$  corresponding to (111), (200) and (220) lattice planes (JCPDS file: No. 03-1051)<sup>62</sup>.

Moreover, the XRD patterns did not show any obvious phases related to the incorporated metals of Al, Co and Cu, but the dominant phases were related to metallic nickel and graphitic carbon. As previously mentioned, the absence of these phases may be due to their fine distribution within the nickel matrix and/or their quantities being very small and falling below the detection limit of the X-ray instrument.

From Fig. 9 (b), a magnified view of the nickel (111) peak at  $2\theta$  of  $44.5^\circ$  is presented for the spent NiO, 10% Al-NiO, 10% Co-NiO and 10% Cu-NiO catalysts. The position of this peak has been slightly shifted to higher  $2\theta$  values by incorporating Al, Co and Cu under the applied reaction conditions. From the literature, it has been reported that the formation of nickel alloys leads to a shift in the position of this peak to higher  $2\theta$  values<sup>54,63</sup>. Therefore, it can be suggested that the incorporation of Al, Co and Cu into nickel matrix resulted in the formation of alloys of Ni-Al, Ni-Co and Ni-Cu. Considering, the diffusion of carbon deposited throughout the lattice of these materials could be played a role in this shifting.

#### TGA studies

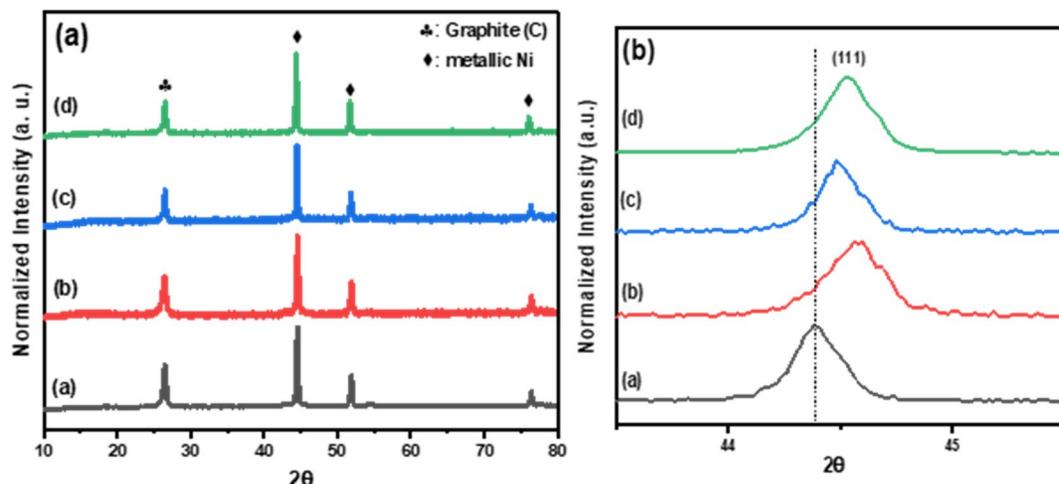
Figure 10 (a, b) shows the results of the TGA oxidation analysis, along with the corresponding first derivative thermogravimetric (DTG) profiles. Figure 10 (a) illustrates the weight loss of the spent NiO, 10% Al-NiO, 10% Co-NiO and 10% Cu-NiO catalysts when subjected to high temperatures in the existence of air. It can be observed that all samples exhibited significant mass loss in the region beyond  $500^\circ\text{C}$  which is due to the combustion of carbon deposited on the catalysts. From Fig. 10 (a), it is possible to estimate the amounts of carbon deposited on these catalysts. It was found that the weight percentages of carbon deposited were ca. 62.10, 72.60, 70.20 and 65.70 wt% spent NiO, 10% Al-NiO, 10% Co-NiO and 10% Cu-NiO catalysts, respectively. Since the products of methane decomposition are only hydrogen and carbon, the amounts of carbon deposited are related to the activity of these catalysts. Thus, there is an agreement between the activity results of these catalysts shown in Fig. 7 and the amounts of carbon formed, which are shown in the results of TGA in Fig. 10 (a).

Figure 10 (b) displays the profiles of derivative weight alterations for the spent catalysts. These profiles can track the differences between the spent catalysts more evidently. It can be observed that each catalyst exhibited a single peak in the coke combustion region in the range of  $500\text{--}770^\circ\text{C}$ , indicating the deposition of a single type of carbonaceous species in each catalyst.

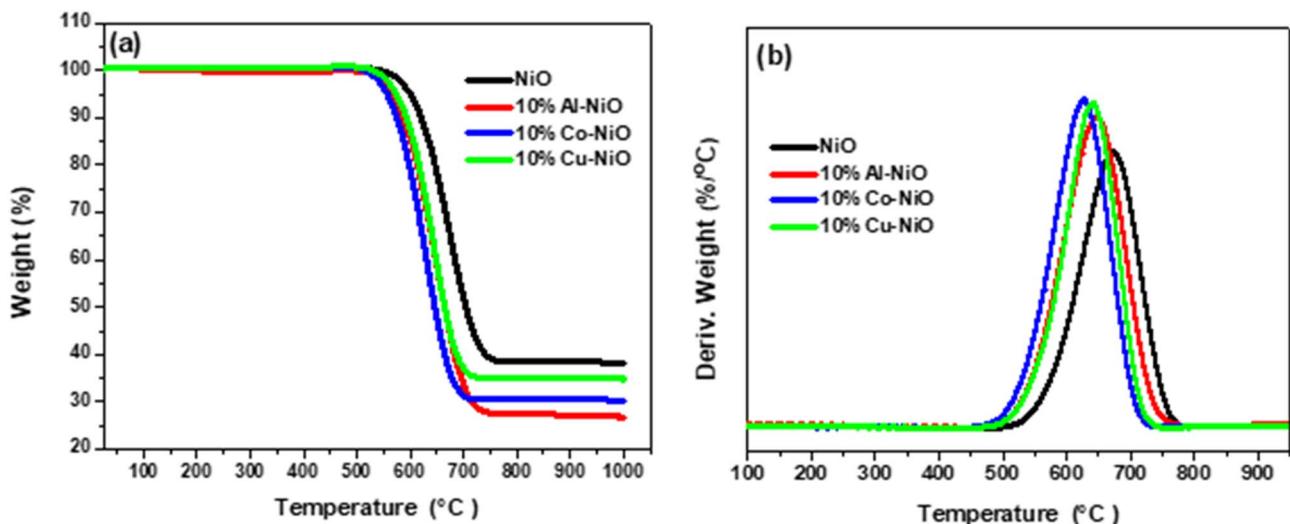
It has been stated that there are three main forms of carbon formed during the decomposition of hydrocarbons over metallic catalysts: amorphous, graphitic sheets and filamentous<sup>64,65</sup>. Filamentous carbon is one of graphitic carbon types. It was found that the combustion region of amorphous carbon is at a temperature of approximately  $330^\circ\text{C}$ , while the combustion region of graphitic carbon of all types is between  $500$  and  $750^\circ\text{C}$ <sup>5</sup>. Therefore, amorphous carbon did not form over the catalysts used, while graphitic carbon was formed. This is confirmed by the absence of oxidation temperature peak of the amorphous carbon in region at  $330^\circ\text{C}$ , and the appearance of combustion region peak of graphitic carbon in the range of  $500\text{--}770^\circ\text{C}$ , as it is shown in the TGA analysis result, Fig. 10 (b). In addition, the XRD analysis results showed the appearance of graphitic carbon peak at  $2\theta = 26.2^\circ$ , Fig. 9 (a).

#### Morphology analysis of spent catalysts

Figure 11 presents FE-SEM images of the spent NiO, 10% Al-NiO, 10% Co-NiO and 10% Cu-NiO catalysts. From these images, it is evident that carbon filaments did not form over these spent catalysts except for the spent



**Fig. 9.** (a) The XRD patterns of spent (a) NiO, (b) 10% Al-NiO, (c) 10% Co-NiO and (d) 10% Cu-NiO catalyst, (b) Zooming view of the nickel (111) peak at  $2\theta$  of  $44.5^\circ$ .



**Fig. 10.** (a) TGA oxidation profiles for the spent catalysts and (b) equivalent first derivative thermogravimetry (DTG) profiles.

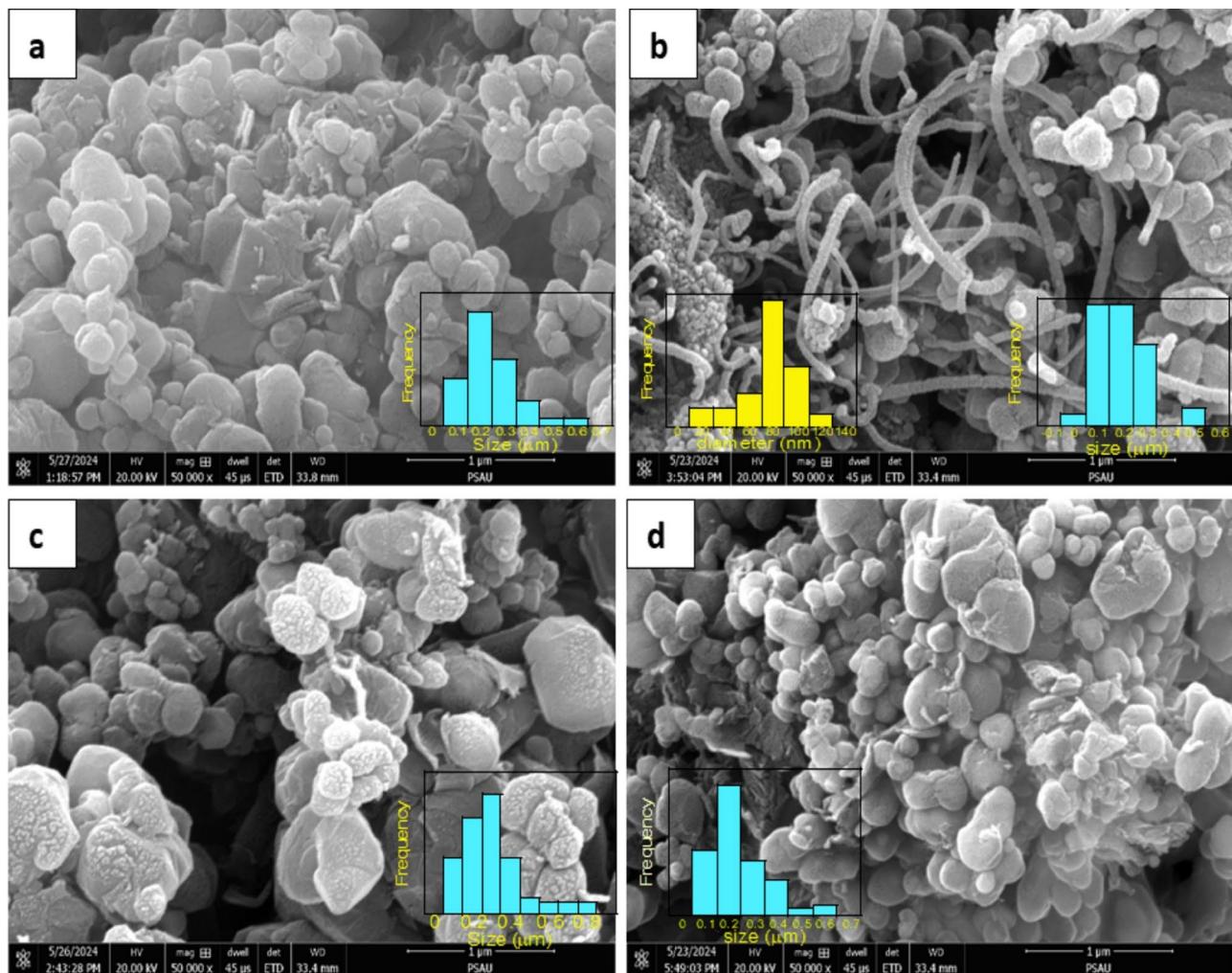
10% Al-NiO catalyst. It was reported that the particle size of catalysts is a significant factor in the growth of carbon nanotubes, one of the types of carbon filaments, and catalysts with large particle sizes have been assumed to be ineffective, and both experimentally and theoretically studies showed that the formation rate of carbon filament can be increased with decreasing particle size of catalysts<sup>66</sup>. Noda et al.<sup>67</sup> investigated the influence of reaction temperature on the formation of carbon nanotubes from the catalytic decomposition of methane over  $\text{Ni}/\text{SiO}_2$  catalyst. They observed that at a reaction temperature above 700 °C, Ni particles sinter to form large Ni particles, which reduce the formation of carbon filaments. Sun et al.<sup>68</sup> investigated the effect of nickel particle size in  $\text{Ni}/\text{Al}_2\text{O}_3$  catalyst on the growth of carbon filaments during the methane decomposition reaction. Their results revealed that the nickel catalyst with particle size of about 56 nm produced the highest yield of carbon filaments. Sakae et al.<sup>69</sup> studied the effectiveness of a  $\text{Ni}/\text{SiO}_2$  catalyst for methane decomposition into carbon nanofibers and hydrogen. They noted that nickel particle diameters in range of 60–100 nm resulted in longer lifetime of Ni catalyst and highest yield of carbon nanofibers.

The estimated particle sizes as inferred from Fig. 11, were 2, (80 nm and 2  $\mu\text{m}$ ), 3 and 2  $\mu\text{m}$  for NiO, 10% Al-NiO, 10% Co-NiO and 10% Cu-NiO, respectively. Obviously, the particle sizes of spent catalysts are much larger than their fresh one as shown in Fig. 2. This is probably due to agglomeration and/or sintering of the catalyst particles under the applied reaction conditions, especially the temperature of 800 °C. Thus, it appears that the increase in microscale particles size played a role in the failure of carbon filament growth. However, this does not fully apply to the 10% Al-NiO catalyst, which showed carbon filaments growth because it has a small particle size of about 80 nm. It has been stated that the size of the catalyst particle plays a role in the activity and stability of the catalyst. Kim et al.<sup>70</sup> investigated the activity of activated carbon as a catalyst for hydrogen production from methane decomposition. Their study included the effect of particle size of the activated carbon catalyst. They observed that as the particle size decreased, the catalyst activity increased. They suggested that this was because of mass transfer. That is, as the particle size increases, it will take more time for the methane molecules to reach the inner surface of the particle because of the limited rate of transport of the reactant, methane, and therefore, the overall reaction rate is lower. This suggestion was also supported by Abbas and co-worker<sup>71</sup>. Consequently, it can be suggested that the incorporation of  $\text{Al}^{3+}$  with NiO resulted in the formation of suitable particle size which improved the catalytic performance of NiO catalyst to produce hydrogen and carbon filaments.

In most of the cases studied, catalysts used in methane decomposition reactions are usually subject to deactivation, which is attributed to the formation of a carbon layer encapsulating the metal particles of the catalyst, which hinders the decomposition of methane<sup>72</sup>. Thus, the absence of carbon filaments on the surface of spent NiO, 10% Co-NiO and 10% Cu-NiO catalysts, Fig. 11 (a, c,d), and the presence of graphitic carbon in the composition of these catalysts as shown in the XRD and TGA results, Figs. 9 and 10, indicate that graphitic carbon may have been formed on these catalysts either by deposition of graphitic carbon on their surface and/or by encapsulating of the metal catalyst particles with graphitic carbon layers. From the above, it can be suggested that the formation of graphitic carbon layers around the metal particles of the catalyst played a role in the low activity of NiO, 10% Co-NiO and 10% Cu-NiO catalysts compared to the 10% Al-NiO catalyst.

#### Raman spectra

Figure 12 shows the Raman spectra of the spent NiO catalyst and NiO catalysts incorporated with 10% of  $\text{Al}^{3+}$ ,  $\text{Co}^{2+}$ , and  $\text{Cu}^{2+}$  ions. The Raman spectra of all spent catalysts are dominated by three sharp peaks at  $\sim 1336$ ,  $\sim 1570$ , and  $\sim 2679 \text{ cm}^{-1}$ , corresponding to the D, G, and 2D bands of graphitic carbon, respectively<sup>73</sup>. This observation confirms the deposition of graphitic carbon nanostructures on the surface of the spent catalysts as a by-product of the thermo-catalytic decomposition of methane. The D band is associated with defects in the

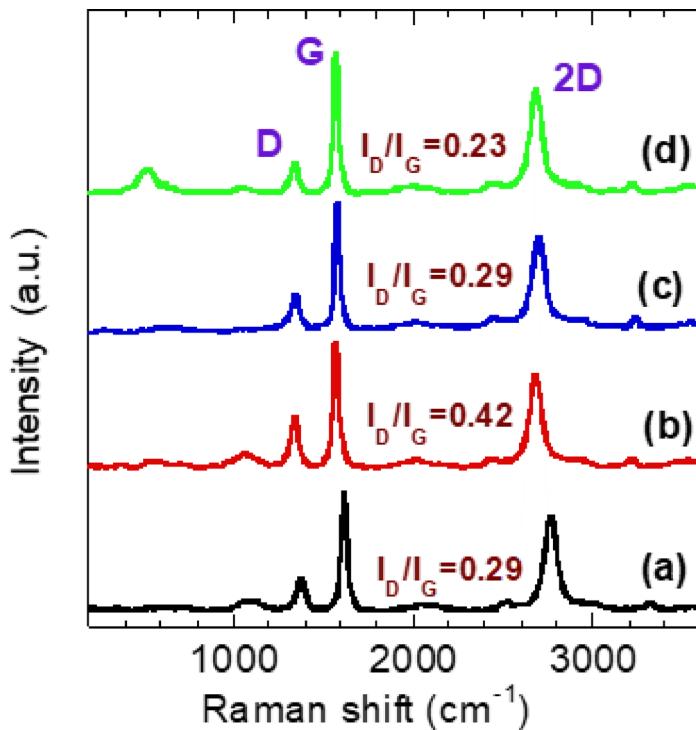


**Fig. 11.** FE-SEM images of the spent (a) NiO, (b) 10% Al-NiO, (c) 10% Co-NiO and (d) 10% Cu-NiO catalysts run at temperature of 800 °C, and fixed gas flow rate of 20 mL/min.

carbon structure, the G band corresponds to well-ordered carbon structures, and the 2D band represents the second-order overtone of the G band. The degree of disorder in the carbon structure is estimated from the  $I_D/I_G$  peak ratio<sup>74</sup>. A higher  $I_D/I_G$  ratio indicates a higher level of defects in the carbon structure and vice versa. The  $I_D/I_G$  ratio for the spent NiO catalyst is 0.29, which increases to 0.42 for carbon deposited on the spent 10%  $\text{Al}^{3+}$ -NiO catalyst. Meanwhile, it decreases to 0.23 for carbon deposited on the spent 10%  $\text{Cu}^{2+}$ -NiO catalyst. In other words, the use of  $\text{Cu}^{2+}$  ions as promoters in the NiO catalyst improves the quality of the deposited carbon during the thermo-catalytic decomposition of methane compared with pure NiO or NiO promoted with  $\text{Al}^{3+}$  and  $\text{Co}^{2+}$  ions.

### Conclusion

In this study, NiO catalysts promoted with 10 wt% of  $\text{Al}^{3+}$ ,  $\text{Co}^{2+}$ , and  $\text{Cu}^{2+}$  ions were successfully synthesized via a co-precipitation method and evaluated for methane decomposition. Among the three promoters,  $\text{Al}^{3+}$  showed the most significant enhancement in catalytic performance. The incorporation of  $\text{Al}^{3+}$  into the NiO lattice led to reduced crystallite size, increased surface area, higher oxygen vacancy concentration, and improved dispersion, all contributing to superior  $\text{CH}_4$  conversion (71%) and  $\text{H}_2$  production ( $216.2 \times 10^{-5}$  mol  $\text{H}_2$  g $^{-1}$  min $^{-1}$ ) at 800 °C. XPS confirmed the creation of charge imbalance and increased  $\text{Ni}^{2+}$  species, while Raman and SEM analyses revealed the formation of graphitic carbon nanostructures, especially on the Al-promoted catalyst. The findings demonstrate that  $\text{Al}^{3+}$  is an effective promoter for enhancing the physicochemical and catalytic properties of NiO in methane decomposition.



**Fig. 12.** Raman Spectra of spent (a) NiO, (b) 10% Al-NiO, (c) 10% Co-NiO and (d) 10% Cu-NiO catalysts.

## Data availability

Data is provided within the manuscript or supplementary information files.

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## Author contributions

Abdulrahman I. Alharthi: Funding acquisition, Conceptualization, Writing – review & editing, Writing – original draft, Mshari A. Alotaibi: Writing – original draft, Funding acquisition. Essam Abdel-Fattah: Writing – review & editing, Investigation, Formal analysis, Conceptualization. F. Qahtan: Methodology, Data curation. Osama A. Alshreef: Methodology, Data curation.

## Declarations

### Competing interests

The authors declare no competing interests.

### Additional information

**Correspondence** and requests for materials should be addressed to A.I.A.

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